

SOLUTION OF A GENERALIZED
AIR POLLUTION MODEL
BY ORTHOGONAL COLLOCATION

A Thesis
Presented to
the Faculty of the Department of
Chemical Engineering
The University of Houston

In Partial Fulfillment
of the Requirements for the Degree of
Master of Science in Chemical Engineering

by
Miguel T. Fleischer
December, 1975

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Finally, I am glad to dedicate this thesis to my wife, Jackie, and my son, David, whose patience and love have made all of this possible.

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ABSTRACT

Turbulent atmospheric diffusion from single or multiple point sources was simulated using the K-theory and solved by a new numerical technique, orthogonal collocation. The physical and chemical behavior of pollutant species in the atmosphere was described by the 3-dimensional, unsteady-state diffusion equation including chemical reactions. Orthogonal collocation was used to reduce the partial differential equation governing the mean concentration of contaminants to first-order ordinary differential equations. This system of equations was then solved in a digital computer.

Mean wind velocities and turbulent diffusivities were represented by empirical equations. Several meteorological parameters were included in these equations so that a variety of atmospheric conditions can be simulated. These parameters and other information required to solve an air pollution problem must be specified as input data by the user.

The present method was evaluated by comparing the results to existing experimental atmospheric concentration profiles. Good agreement was found in all cases. In addition, the sensitivity of the present model to variations in atmospheric conditions was analyzed by means of a parametric study. Proper responses were observed in all cases.

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CHAPTER I

INTRODUCTION

There has been increasing interest in bringing the air pollution problem under control. This problem can be represented as a system consisting of three basic components: emission sources, the atmosphere, and receptors. Once the pollutants are emitted from sources, they are transported, dispersed, and transformed according to the laws of physics and chemistry throughout the entire atmosphere. Finally, these air pollutants are detected by receptors, such as human beings, animals, plants, and materials, producing in some cases undesirable effects.

In order to understand the cause-effect relationship of pollutant emission and dispersion on the air quality, a study of the three components previously discussed should be carried out. Understanding of the physical and chemical behavior of pollutant species in the atmosphere plays then an important role in the relation of source emissions to air quality standards.

The objective of an air pollution model is to describe mathematically the spatial and temporal history of contaminants released into the atmosphere.

Several air pollution models have been developed so far, but they have had only limited success. An improved dispersion model based on the K-theory and solved using a new numerical technique is presented in this thesis. The atmospheric processes involving air pollutants are described by the 3-dimensional, unsteady-state diffusion equation including chemical reactions. Orthogonal collocation, a weighted residual method, reduces the partial differential equations governing the mean concentration of pollutant species to first-order ordinary differential equations. This system of equations is solved then in a digital computer.

The present work is validated with existing experimental data. In addition, its sensitivity to variations in atmospheric conditions is analyzed by means of a parametric study.

Chapter II

THEORETICAL BACKGROUND

There are two fundamental ways of describing the physical and chemical behavior of pollutant species in the turbulent atmosphere. The first is the so-called Eulerian approach, where the behavior of species is described relative to fixed coordinates. The second is the statistical approach, where concentration changes are described from a statistical point of view by considering the paths of individual elements of fluid, and is thus Lagrangian in nature.

The objective of any air pollution model is to predict pollutant concentrations at given points. These concentrations are caused by emissions from sources, and therefore a source-oriented point of view is the natural one in this case.

Eulerian Approach

Consider s species in a fluid. The concentration of each must, at each instant, satisfy a material balance taken over a volume element. Therefore, the concentration of each species must satisfy the continuity equation usually known as the instantaneous diffusion equation,

$$\frac{\partial C_i}{\partial t} + \frac{\partial}{\partial x_j} u_j C_i = \frac{\partial}{\partial x_j} \{D_i \frac{\partial C_i}{\partial x_j}\} + R_i(C_1, \dots, C_s) \quad (2.1)$$

$$i = 1, 2, \dots, s$$

where the subscript j represents the three coordinate directions: x (axial), y (lateral), and z (vertical); and

C_i = the instantaneous concentration of species i

u_j = the j th component of the fluid velocity

D_i = the molecular diffusivity of species i in the carrier fluid, and

R_i = the rate of generation of species i .

Since atmospheric flows are turbulent, it is conventional to divide the instantaneous quantities into mean and fluctuating facts,

$$\begin{aligned} C_i &= \langle C_i \rangle + C'_i \\ u_j &= \bar{u}_j + u'_j \end{aligned} \quad (2.2)$$

It should be noted that the mean fluid velocities are usually determined by temporal averaging and the mean concentrations always represent ensemble averages. This is the reason why a different notation has been used for the mean values of the velocities and the concentrations.

Substitution of equation (2.2) into equation (2.1) gives

$$\begin{aligned}
\frac{\partial}{\partial t}(\langle C_i \rangle + C_i') + \frac{\partial}{\partial x_j} \{ (\bar{u}_j + u_j') (\langle C_i \rangle + C_i') \} = \\
\frac{\partial}{\partial x_j} \{ D_i \frac{\partial}{\partial x_j} (\langle C_i \rangle + C_i') \} + \\
R_i(\langle C_1 \rangle + C_1', \dots, \langle C_s \rangle + C_s') \quad (2.3)
\end{aligned}$$

Taking an average of equation (2.3) over a large ensemble of realizations of the turbulence, one obtains the following equation governing $\langle C_i \rangle$

$$\begin{aligned}
\frac{\partial \langle C_i \rangle}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_j \langle C_i \rangle) = \frac{\partial}{\partial x_j} \{ D_i \frac{\partial \langle C_i \rangle}{\partial x_j} - \langle u_j' C_i' \rangle \} + \\
+ \langle R_i(\langle C_1 \rangle + C_1', \dots, \langle C_s \rangle + C_s') \rangle \quad (2.4)
\end{aligned}$$

The most common means of representing the turbulent fluxes $\langle u_j' C_i' \rangle$ is by the so-called K-theory, in which a turbulent diffusivity is defined by

$$-\langle u_j' C_i' \rangle = K_{jj} \frac{\partial \langle C_i \rangle}{\partial x_j} \quad (2.5)$$

Ignoring the molecular diffusion when compared with the turbulent diffusion, and assuming the atmosphere to be incompressible, the final expression for the diffusion equation becomes

$$\begin{aligned}
\frac{\partial \langle C_i \rangle}{\partial t} + \bar{u}_j \frac{\partial \langle C_i \rangle}{\partial x_j} = \frac{\partial}{\partial x_j} \{ K_{jj} \frac{\partial \langle C_i \rangle}{\partial x_j} \} + \\
+ \langle R_i(\langle C_1 \rangle, \dots, \langle C_s \rangle) \rangle \quad (2.6)
\end{aligned}$$

It should be pointed out that the effect of concentration fluctuations on the rate of reaction, i.e., terms such as $\langle C_i' C_j' \rangle$ that arise from cases where R_i is a nonlinear function of

the C_i , were neglected in the development of equation (2.6). The conditions for this approximation to be valid will be discussed in Chapter IV.

Lagrangian Approach

The Lagrangian approach to turbulent diffusion is concerned with the behavior of representative fluid particles. The development of a general equation for the mean concentration $\langle C(x,t) \rangle$ follows that of Seinfeld [22].

$$\begin{aligned} \langle C(x,t) \rangle = & \int_{-\infty}^{\infty} \int_{-\infty}^{\infty} \int_{-\infty}^{\infty} Q(x,t/x_0,t_0) \langle C(x_0,t_0) \rangle dx_0 + \\ & + \int_{-\infty}^{\infty} \int_{-\infty}^{\infty} \int_{-\infty}^{\infty} \int_{t_0}^t Q(x,t/x',t') S(x',t') dt' dx' \quad (2.7) \end{aligned}$$

where $Q(x,t/x^*,t^*)$ is the transition probability density for the particle, that is, the probability density that if the particle is at a position x^* at time t^* will undergo a displacement to x at t , and $S(x,t)$ is the spatial-temporal distribution of particle sources.

Therefore, the first term on the right-hand side of equation (2.7) represents those particles present at t_0 , and the second term on the right-hand side accounts for particles added from sources between t' and t .

As can be observed from equation (2.7), the applicability of the Lagrangian approach rests on the ability to

evaluate the transition probability Q . This is a difficult task because complete knowledge of the turbulence properties required to determine Q is generally not available. This problem has been usually overcome by assuming that Q obeys a multidimensional Gaussian distribution, but it is known that this assumption is valid only if the turbulence is stationary and homogeneous. By using that assumption then, one is limited to apply the Lagrangian approach only to some atmospheric cases.

Moreover, the development of equation (2.7) was done for cases where the particles were not undergoing chemical reactions. First-order reactions can be included rather easily in the development of a similar equation, but there is no convenient way of incorporating nonlinear chemical reactions in the Lagrangian approach to turbulent diffusion.

The Eulerian method is very useful in air pollution modeling because the Eulerian statistics are easy to measure and as it will be seen later, possible to represent in an analytical form suitable for computer programs. In addition, the mathematical expressions can be directly applied to situations where chemical reactions take place.

Unfortunately, the Eulerian approach can be solved only by approximate solutions, e.g., the K-theory, and this leads to the problem of accurately predict the eddy diffusivities.

The main objective of the present work is to obtain a model which can be applied to any atmospheric dispersion problem with chemical reactions. Because of the previous analysis of the two approaches that can be used to describe atmospheric diffusion, it was decided to use the Eulerian method as the basis of the present model. As will be seen later, this is the most common approach used although it leads to limited success. The reason being the numerical techniques with which the equations have been solved. Another objective of the present work is to investigate the possibility of a better numerical method for solving the general diffusion equation.

Chapter III

REVIEW OF PREVIOUS WORK

Eulerian Models

The basic mathematical statement for description of the temporal and spatial distribution of chemical species by this approach is the mass balance or continuity equation. This expression, equation (2.6) in this study, plus the appropriate initial and boundary conditions complete the general description.

Exact solutions to this set of equations have not been published. However, it is possible to obtain approximate solutions using numerical techniques.

During the past years, several models have been presented in the literature, ranging from very simple ones like the box model to general cases solved by finite-difference techniques.

Box Model

The simplest air pollution model, though not the first, is the box model, which has been discussed by Sklarew [25]. This model consists of an imaginary box which bounds the atmosphere over a city with the top of the box being at a constant mixing height, the height at which there is no further vertical diffusion. The concentration in the box

is calculated from a simple material balance on the air flow and pollutant emissions, thus, it is not sufficient for anything more than gross estimates, by offering a quick result for long-term concentrations.

Grid Model

Sklarew [25] proposed a different approach on urban air pollution modeling, the grid model. In this model, the region of interest is divided into a three dimensional grid of cells where the diffusion equation of the Eulerian approach is solved. The time-dependent solution is obtained numerically from difference equations.

Lagrangian particles representing a definite amount of pollutant are advected and diffused through the Eulerian grid. In order to do this, a pseudo-velocity $\tilde{v}^*$ is defined as

$$\tilde{v}^* = \tilde{u} - D' \nabla C / C \quad (3.1)$$

where D' is a diffusivity tensor and $\tilde{u}$ is the wind velocity averaged throughout the cell surrounding each grid point. The defined $\tilde{v}^*$ then is just the sum of the wind velocity and the velocity corresponding to the diffusion flux. Therefore, the diffusion equation is reduced to

$$\frac{\partial C_i}{\partial t} = - \nabla \cdot (\tilde{v}^* C_i) + R_i + \text{sources} \quad (3.2)$$

This equation is solved in time-steps in the following sequence: the pollutant concentration in each cell of the grid is given by the particles in the cell. The cell average concentration is updated by advancing the chemical reactions for a time-step and by adding (and/or subtracting) pollutant from sources (and/or sinks) within the cell. Finally, the Lagrangian particles are advected and diffused using the pseudo-velocity, and thus transported at the boundary of each cell for a specific period of time.

As it can be observed, this model is a mixture of the Eulerian and Lagrangian approaches. In spite of being a more general model as compared to the previous one, it has the disadvantage that the grid size necessary for a desired accuracy can result in prohibitive computing time.

Two Dimensional Unsteady State Models

Much of the recent work on air pollution modeling centers on solving a simplified diffusion equation, a two dimensional unsteady state case, which includes only the x-component of the wind velocity and the vertical turbulent diffusion coefficient. In almost all these models, the solutions are obtained by using a finite-difference technique.

For these cases, equation (2.6) for a single species becomes

$$\frac{\partial \langle C \rangle}{\partial t} + \bar{u} \frac{\partial \langle C \rangle}{\partial x} = \frac{\partial}{\partial z} \left\{ K_z \frac{\partial \langle C \rangle}{\partial z} \right\} \quad (3.3)$$

Runca and Sardei [21] solved equation (3.3) using a mixed Lagrangian-Eulerian finite difference scheme. In this model, the emission rate of the source is taken as a boundary condition. The wind velocity and diffusion coefficient are considered to be only functions of z .

Equation (3.3) is solved with the method of fractional steps: the concentration field at time $t+\Delta t$ is obtained from that at time t by separating the contributions due to the advection and diffusion terms of equation (3.3).

In the first step, the following advection equation is solved by a Lagrangian technique over the time interval Δt with the concentration field at time t as initial condition:

$$\frac{\partial C}{\partial t} + u(z) \frac{\partial C}{\partial x} = 0 \quad (3.4)$$

The diffusion equation,

$$\frac{\partial C}{\partial t} - \frac{\partial}{\partial z} \left\{ K_z(z) \frac{\partial C}{\partial z} \right\} = 0 \quad (3.5)$$

the second step, is solved with a conventional Eulerian finite-difference scheme over the same time interval. The initial condition is provided by the concentration field obtained from the first step, and the solution of the second step is an approximation of the concentration field at time $t+\Delta t$.

A different model was presented by Egan and Mahoney [6], where equation (3.3) was also solved, but the source emission rate Q , was included in the same governing equation:

$$\frac{\partial C}{\partial t} + \bar{u} \frac{\partial C}{\partial x} = \frac{\partial}{\partial z} \left\{ K_z \frac{\partial C}{\partial z} \right\} + Q \quad (3.6)$$

To simulate transport through an urban area, the region was divided into a number of grid elements, and the partial derivatives in equation (3.6) were approximated by finite differences corresponding to the dimensions of the urban grid elements. Equation (3.6) was solved by an unconventional scheme using moments of concentration distribution.

A slightly more difficult diffusion equation was solved by Eschenroeder and Martinez [7]. A simplified chemical kinetic scheme was included in the governing equation,

$$\frac{\partial C_i}{\partial t} + \bar{u} \frac{\partial C_i}{\partial x} = \frac{\partial}{\partial z} \left\{ K_z \frac{\partial C_i}{\partial z} \right\} + R_i \quad (3.7)$$

$$i = 1, 2, \dots, s$$

where R_i is the production rate for the i th species and s is the number of species.

The numerical solution of equation (3.7) followed a Crank-Nicholson type implicit finite difference scheme. Since fields for $\bar{u}$ and K_z were prescribed by meteorology inputs, the nonlinearity was confined only to some members of the R_i terms. In a later paper, Eschenroeder and

Martinez [8] reported that a number of difficulties were encountered in using the Crank-Nicholson method and the approach was abandoned.

General Solutions

Some recent work has been done to solve the general expression of the diffusion equation. One of these models was developed by Roth et al [20]. The governing equation solved was the following:

$$\begin{aligned} \frac{\partial \langle C_i \rangle}{\partial t} + \bar{u} \frac{\partial \langle C_i \rangle}{\partial x} + \bar{v} \frac{\partial \langle C_i \rangle}{\partial y} + \bar{w} \frac{\partial \langle C_i \rangle}{\partial z} = \frac{\partial}{\partial z} \left\{ K_z \frac{\partial \langle C_i \rangle}{\partial z} \right\} + \\ + R_i(\langle C_1 \rangle, \dots, \langle C_s \rangle) + Q_i(x, y, z, t) \end{aligned} \quad (3.8)$$

$$i = 1, 2, \dots, s$$

where K_z is the vertical eddy diffusivity, R_i is the rate of formation of species i by chemical reaction, and Q_i is the rate of emission of species i from sources.

Equation (3.8), plus initial and boundary conditions, was applied for the prediction of pollutant concentrations over a fifty mile square area. This region was divided into a grid of 625, 2x2 mile squares, where 198 grid squares were source-free. The grid actually used in the solution of equation (3.8) was a three-dimensional array of ten layers of cells occupying the space between the ground and the inversion base. Therefore, each cell had a two mile square base and a height of $(H-h)/10$, being H and h the elevations

of the inversion base and ground above sea level, respectively.

To represent the surface winds, Roth et al. constructed maps of wind speed and wind direction for hourly time intervals, using data gathered at the network of ground-based monitoring stations. In the absence of wind field aloft data, the surface values were used as the basis to calculate wind velocities to all levels between the ground and the inversion base.

A model for the vertical turbulent diffusivity was developed based on the work done by Eschenroeder and Martinez [7].

Finally, the model was completed by a simplified kinetic mechanism involving 12 species and 14 reaction steps. The mathematical representation included four coupled nonlinear differential equations (five other species were expressed by steady-state relations, and the remaining three species were products that could have also been represented by differential equations, but it was not done) that were solved by a modified Gear's method.

A fractional step finite-difference method was selected to be the numerical technique for the model. In this type of solution, a multidimensional problem is replaced by a succession of simpler lower dimensional problems. Therefore, the four-dimensional partial differential equation (3.8) in

(x,y,z,t) was split into three two-dimensional equations in (x,t) , (y,t) , and (z,t) , with the inclusion of the reaction and elevated source terms in the (z,t) fragment. The solution in (z,t) is implicit, while the solution in (x,t) and (y,t) is explicit. Each of these two-dimensional equations was then integrated in succession over one time step, and the terms in each of the three partial differential equations was approximated by finite-difference expressions.

It should be pointed out that this model cannot handle point or line sources, the emissions therefore averaged over relatively large distances.

Another recent model in which a solution to the general expression of the diffusion equation was obtained, was developed by Shir and Shieh [24]. This model was used to study SO_2 distributions in the St. Louis metropolitan area during 25 consecutive days. The region of interest was divided into a three-dimensional grid system of $30 \times 40 \times 14 = 16,800$ grid points. The horizontal grid sizes Δx and Δy were of 1524m and the vertical size 20m, 25m, or $(H-200)/4$ m, values depending on the heights of the vertical grids (H represents the mixing height). The horizontal grid sizes were chosen according to the grid size of the emission source inventory.

The equation solved in this model was the diffusion equation for a single species,

$$\frac{\partial C}{\partial t} + \nabla \cdot VC = K_H \nabla_H^2 C + \frac{\partial}{\partial z} \left\{ K_V \frac{\partial C}{\partial z} \right\} + Q + R \quad (3.9)$$

where C is the mean concentration of SO_2 , $V = (u, v, w)$ is the mean wind vector, Q is the source strength rate, R is the chemical reaction rate, K_H is the horizontal eddy diffusivity, and K_V is the vertical eddy diffusivity.

The hourly averaged surface wind field for the total region was obtained by using a weighted interpolation scheme. Data collected at some stations were interpolated to a square grid, which had a size of five area source dimensions. From this wind field, a linear interpolation was used to obtain a wind vector at each grid point.

Since upper layer wind data were not available, the vertical wind profiles at each grid location was assumed to be of power law from

$$V = V_s \left(\frac{z}{z_s} \right)^p \quad (3.10)$$

where V and V_s are the upper and surface wind at the height z and z_s , respectively. The power constant p was determined by using equation (3.10) and data gathered at heights of 140m and 39m. The vertical component of the wind vector was calculated from the horizontal winds through the continuity equation. Finally, a constant wind direction with height was assumed in the model.

A turbulence transport model developed by Shir [23] was used to calculate the eddy diffusivities. Under neutral conditions, the vertical component of the eddy diffusivity vector is expressed as

$$K_v = u_* \ell, \quad \ell = k_o z \exp\left(-\frac{4z}{H}\right) \quad (3.11)$$

where u_* , k_o and H are the friction velocity, the von Kármán constant, and the height of the boundary layer, respectively.

Under non-neutral conditions, an eddy diffusivity, K_s , at the surface layer ($z=10\text{m}$) is calculated using another model, and then extrapolated to higher altitudes by the assumption that

$$K_v = K_s \frac{\ell}{\ell_s} \quad (3.12)$$

In this model, the horizontal eddy diffusivity was assumed to be constant.

Finally, the time-dependent source emission rate was averaged over a 2-hour period for each source, and the chemical reaction rate of SO_2 expressed by

$$R = -kC \quad (3.13)$$

where k is the reaction rate constant with a given value of 10^{-4} sec^{-1} .

A second-order, central finite-difference scheme was used to integrate the advection and horizontal terms, and

the Crank-Nicholson method was used for the vertical diffusion term.

In this model, 2-hour and 24-hour averaged variations of SO_2 concentrations for the 25-day period were obtained, and compared with experimental measurements for the same term average concentrations, at 10 monitoring stations. In their analysis of the results, Shir and Shieh concluded that the 2-hour data were consistently larger than the 24-hour data.

Statistical Models

As it was previously discussed, one of the problems in the Lagrangian approach is the evaluation of the transition probability density function. The most common way that has been used to overcome this problem has been to assume that the transition probability density function, $Q(x, t/x^*, t^*)$ obeys a Gaussian distribution. This assumption has given rise to several models, which will be discussed next.

Gaussian Plume Models

The best known of the practical models based on statistical theory is the Gaussian Plume model. This model was the first recognized continuous point source air pollution model. Most of the existing urban air pollution models are Gaussian Plume models. The concentration of

gas or aerosols at a point (x,y,z) due to a continuous source with an effective emission height L , is given by

$$\langle C(x,y,z) \rangle = \frac{Q}{2\pi\sigma_y\sigma_z u} \exp \left[-\frac{1}{2} \left(\frac{y}{\sigma_y} \right)^2 \right] \times \left(\exp \left[-\frac{1}{2} \left(\frac{z-L}{\sigma_z} \right)^2 \right] + \exp \left[-\frac{1}{2} \left(\frac{z+L}{\sigma_z} \right)^2 \right] \right) \quad (3.14)$$

The following assumptions are made:

- 1) The dispersion process is at steady state conditions.
- 2) The plume spread has a Gaussian distribution in both the horizontal and vertical planes, with standard deviations of plume concentration distribution σ_y and σ_z , respectively, which are function of only the atmospheric stability and distance x from the source.
- 3) The mean wind speed affecting the plume, u , is oriented in the x -axis and is a constant value for any height.
- 4) A constant emission rate of pollutants, Q .
- 5) A total reflection at the earth's surface.
- 6) No wind shear; and
- 7) The pollutants are chemically non-interacting.

Typically then, in these models the rate of dispersion is a function of the atmospheric stability class and the travel time or distance from the source. The lateral and vertical distributions are assumed to be Gaussian around the plume centerline. The relation between the horizontal and vertical dispersion coefficients, σ_y and

σ_z , and the Pasquill-Gifford stability categories and downwind distance from the source can be found in Turner [30].

It can be observed then that the Gaussian Plume formula is not flexible enough to include all possible variations that the air motion experiences under urban atmospheric conditions.

Gaussian Puff Models

To describe more accurately the general unsteady state atmospheric diffusion case, some Puff models have been developed by Roberts et al [19] and others. In a Puff model, source emissions are broken into a series of instantaneous puffs instead of a continuous plume. The distribution within a puff is assumed Gaussian in the three directions.

In the Puff model, the entire cloud or puff is assumed to be simultaneously transported along a trajectory given by the mean flow. It is also assumed that the constant standard deviations (or diffusivities) are independent of height, up to an inversion height, that there is no wind shear, and that the pollutants are chemically non-interacting.

Monte Carlo Methods

In a Monte Carlo method, averages of a desired quantity, in this case concentration, are obtained by repeating the process many times using the same initial conditions. Each repetition is called a realization and is controlled by the random forces acting during its particular flight.

A recent model using a Monte Carlo method was developed by Bullin [4]. In this model, the turbulent diffusion process was simulated by allowing a large number of particles representing a definite amount of pollutant to diffuse through the flow field according to the following stochastic Markovian equation

$$\frac{dx_j}{dt} = u_j(x_j, t) + \left[\frac{2D}{P_j} \right]^{1/2} N_j(t) \quad (3.15)$$

where u_j is the instantaneous velocity in the j th direction, D is the molecular diffusivity, N_j is the j th independent Gaussian white noise with zero mean, P_j is the power spectral density of the j th white noise, and the subscript j denotes the three coordinate directions in the Cartesian space.

After a specified time, the location of each particle was recorded and the concentration distribution was calculated by counting the number of particles within cells of specified size and dividing by the cell volume.

This model was solved on a hybrid computer, where equation (3.15) was programmed for repeated solutions on an analog computer with stochastic variables u_j and N_j being provided as inputs.

As it can be observed, the Gaussian distribution assumption was again incorporated in the model, and no reactions were involved in the simulation of turbulent diffusion in the atmosphere.

Chapter IV

ORTHOGONAL COLLOCATION

In view of all air pollution problems and the need for air quality improvement, air pollution modeling has great practical importance. This is the reason why much consideration has been given to this subject during recent years.

Several air pollution models have been developed so far, but since this subject is very complex, most of those models have been simplified. It is evident that the more simplifications included the less applicable a model is and the poorer the results can be.

It is well known that a major factor that characterizes diffusion processes in the atmosphere is the state of atmospheric turbulence. A general model which includes temporal and spatial variations of meteorological parameters can provide a good description of atmospheric diffusion processes.

As it was discussed in Chapter II, the Eulerian approach will be used for solving the atmospheric diffusion problem in the present work.

A finite-difference scheme has been the most widely used numerical technique for solving the partial differential equations resulting from a model based on the

Eulerian approach. The application of this technique to a general problem gives rise to a very complex model, usually with a large number of grids and in most of the cases then requires much computer time to obtain accurate results. In addition, most of those models cannot handle point sources, and artificial diffusion errors are usually present in the results.

There is a need then to keep working with the diffusion equation in its more general form as a tool for solving air pollution problems, and to investigate the feasibility of using another type of numerical technique which could have better properties than the finite-difference method. This new technique, orthogonal collocation, is discussed next.

Theory

The orthogonal collocation method belongs to the class of weighted residual methods. It was presented by Villadsen and Stewart [31], Finlayson [11], and Villadsen [32], who give details about its theory, some of which will be presented next. They also discuss several applications, mainly one or two-dimensional problems.

The method of weighted residuals is a general method of obtaining solutions to differential equations. The unknown solution is expanded in a set of trial functions, which are specified, but with adjustable constants (or

functions), which are chosen to give the best solution to the differential equation.

The trial function is chosen in such a way that will satisfy the boundary conditions for all selections of the adjustable constants. This trial function then is substituted into the differential equation forming a residual. If the trial function were the exact solution, the residual would be zero. In the weighted residual method, the adjustable constants are chosen so that the residual is forced to be zero in an average sense.

Let us begin considering a boundary-value problem in one independent variable, x . A general type of differential equation can be written as

$$\begin{aligned} L^V(y) &= 0 & \text{in } V \\ L^S(y) &= 0 & \text{in } S \end{aligned} \tag{4.1}$$

where x is the position vector and S the surface or boundary. In the collocation method, the dependent variable y is approximated by a series expansion containing N undetermined parameters. These parameters are then calculated by applying equation (4.1) at N pre-selected points.

In the orthogonal collocation method, the series expansion consists of a set of orthogonal polynomials and the collocation points are chosen as the zeroes of the

polynomials, which make the weighted residuals to be zero in an average sense.

Therefore, for the system given by equation (4.1), the solution is approximated by

$$y(x) = y_0(x) + \sum_{i=1}^N a_i P_i(x) \quad (4.2)$$

$$\text{where } P_i(x) = \sum_{j=0}^i c_j x^j \quad (4.3)$$

is a polynomial such that successive polynomials are orthogonal to all polynomials of order less than i , with respect to some weighting function $w(x) \geq 0$:

$$\int_a^b w(x) P_n(x) P_i(x) dx = 0, \quad n=0,1,\dots,i-1 \quad (4.4)$$

Depending on the weighting function $w(x)$ and the interval $a \leq x \leq b$, several types of polynomials can be obtained. Choosing $w(x) = 1$, $a = -1$, $b = 1$, and the first polynomial $P_0(x) = 1$, the resulting polynomials, $P_i(x)$, are called Legendre polynomials.

If the weighting function is defined as

$$w(x) = (1-x)^\alpha (1+x)^\beta \quad (4.5)$$

and the same previous interval is used, the Jacobi polynomials, $P_i^{(\alpha, \beta)}(x)$, are obtained [1]. It follows then that

$$P_i(x) = P_i^{(0,0)}(x) \quad (4.6)$$

The polynomial $P_i(x)$, as defined by equation (4.3), has i roots in the interval $a \leq x \leq b$, which serve as collocation

points. From now on, let N equal the number of those interior collocation points.

Let us now consider polynomials which have additional convenient properties: the solution of a problem is sought in the domain $0 \leq x \leq 1$ and is required to be symmetric about $x=0$. Then, it can be expanded in terms of powers of x^2 .

A suitable trial function is

$$y(x) = y(1) + (1-x^2) \sum_{i=0}^{N-1} a_i P_i(x^2) \quad (4.7)$$

where the a_i are undetermined constants and the $P_i(x^2)$, polynomials of degree i in x^2 that can be constructed using an orthogonality condition like equation (4.4):

$$\int_0^1 (1-x^2) x^{a-1} P_n(x^2) P_i(x^2) dx = G_i \delta_{in} \quad (4.8)$$

$$n = 1, 2, \dots, i-1$$

where $a = 1, 2, 3$, for planar, cylindrical, or spherical geometry.

The polynomials defined by equation (4.8) are Jacobi polynomials [20], and the constant G_i is given by

$$G_i = \frac{[\Gamma(\frac{a}{2})]^2 \Gamma(i+1) \Gamma(i+2)}{(4i+a+2) \Gamma(i+\frac{a}{2}) \Gamma(i+\frac{a}{2}+1)} \quad (4.9)$$

The coefficients of orthogonal polynomials in a new interval $0 \leq x \leq 1$ can also be computed from the old interval polynomials, $-1 \leq x \leq 1$, by the following relation [23]:

$$\text{If } f_i(x) = \sum_{j=0}^i c_j x^j, \quad f_i^*(x) = f_i(2x-1) \quad (4.10)$$

$$= \sum_{j=0}^i c_j^* x^j$$

where $f_i^*(x)$ stands for the shifted polynomial. It should be pointed out that if the interval of orthogonality is changed, the weighting function $w(x)$ changes for the Jacobi polynomials, and remains the same ($=1$) for the Legendre polynomials.

A set of N equations is needed in order to determine the N coefficients a_i , and therefore completely define the solution in the form of the trial function. This can be obtained by substituting equation (4.7) into the differential equation (4.1) and setting the residual formed equal to zero at the N collocation points x_j . These points are the roots to the N th polynomial, $P_N(x^2) = 0$ at x_j .

The application of the method as described above becomes more confused as N increases (and also if the dimension of the differential equation increases). As a simpler and more attractive alternative to this method, as it will be seen later, the collocation equations can be obtained in terms of the solution at the collocation points, $y(x_j)$. In this method, if the solution at a different point than a collocation point needs to be obtained, it has to be interpolated by using all the known values of $y(x_j)$ at the collocation points.

For this purpose, equation (4.7) can be rewritten as

$$y(x) = \sum_{i=1}^{N+1} d_i x^{2i-2} \quad (4.11)$$

where the d_i are undetermined coefficients and the $(N+1)$ collocation point is at $x=1$. If equation (4.11) is evaluated at the collocation points, the following expression is obtained:

$$y(x_j) = \sum_{i=1}^{N+1} x_j^{2i-2} d_i \quad (4.12)$$

The same procedure can be done for the first derivative and the Laplacian,

$$\left. \frac{dy}{dx} \right|_{x_j} = \sum_{i=1}^{N+1} \left. \frac{dx^{2i-2}}{dx} \right|_{x_j} d_i \quad (4.13)$$

$$\left. \nabla^2 y \right|_{x_j} = \sum_{i=1}^{N+1} \left. \nabla^2 (x^{2i-2}) \right|_{x_j} d_i \quad (4.14)$$

These equations can be rewritten in matrix notation as follows (the square matrices have $(N+1) \times (N+1)$ elements):

$$\tilde{y} = \tilde{Q} \tilde{d} \quad (4.15)$$

$$\tilde{\nabla y} = \tilde{R} \tilde{d} \quad (4.16)$$

$$\tilde{\nabla^2 y} = \tilde{T} \tilde{d} \quad (4.17)$$

where

$$Q_{ji} = x_j^{2i-2}, \quad R_{ji} = \left. \frac{dx^{2i-2}}{dx} \right|_{x_j},$$

$$T_{ji} = \left. \nabla^2 (x^{2i-2}) \right|_{x_j} \quad (4.18)$$

The first derivative and Laplacian can be written in terms of the solution $y(x_j)$ by solving $\tilde{d}$ from equation (4.15) and substituting it into equations (4.16) and (4.17):

$$\nabla_{\tilde{y}} = \bar{R} \bar{Q}^{-1} \tilde{y} \equiv \bar{A} \tilde{y} \quad (4.19)$$

$$\nabla_{\tilde{y}}^2 = \bar{T} \bar{Q}^{-1} \tilde{y} \equiv \bar{B} \tilde{y} \quad (4.20)$$

Finally then, the derivatives can be expressed as

$$\nabla y = \left. \frac{dy}{dx} \right|_{x_j} = \sum_{i=1}^{N+1} A_{ji} y_i \quad \text{for } j=1, \dots, N+1 \quad (4.21)$$

$$\nabla^2 y = \left[\frac{d^2 y}{dx^2} + \frac{a}{x} \frac{dy}{dx} \right]_{x_j} = \sum_{i=1}^{N+1} B_{ji} y_i \quad \text{for } j=1, \dots, N+1 \quad (4.22)$$

where $a=0,1$, or 2 for plane parallel, cylindrical, or spherical symmetry, respectively, and

$$[A_{ji}] = \begin{bmatrix} \left(\frac{dx^0}{dx} \right)_{x_1} & \dots & \left(\frac{dx^{2N}}{dx} \right)_{x_1} \\ \vdots & & \vdots \\ \left(\frac{dx^0}{dx} \right)_{x_{N+1}} & \dots & \left(\frac{dx^{2N}}{dx} \right)_{x_{N+1}} \end{bmatrix} \begin{bmatrix} \\ \\ Q \end{bmatrix}^{-1} \quad (4.23)$$

$$[B_{ji}] = \begin{bmatrix} \nabla^2(x^0) \Big|_{x_1} & \dots & \nabla^2(x^{2N}) \Big|_{x_1} \\ \vdots & & \vdots \\ \nabla^2(x^0) \Big|_{x_{N+1}} & \dots & \nabla^2(x^{2N}) \Big|_{x_{N+1}} \end{bmatrix} \begin{bmatrix} Q \\ \vdots \\ Q \end{bmatrix}^{-1} \quad (4.24)$$

$$[Q] = \begin{bmatrix} 1 & x_1^2 & \dots & x_1^{2N} \\ \vdots & \vdots & & \vdots \\ \vdots & \vdots & & \vdots \\ \vdots & \vdots & & \vdots \\ \vdots & \vdots & & \vdots \\ 1 & x_{N+1}^2 & \dots & x_{N+1}^{2N} \end{bmatrix} \quad (4.25)$$

Integrals of the solution over the volume V can be calculated with high accuracy via the summation formula

$$\int_0^1 f(x) x^{a-1} dx = \sum_{j=1}^{N+1} W_j f(x_j) \quad (4.26)$$

where the quadrature weights are given by

$$[W_j] = \left[\int_0^1 x^{0+a-1} dx, \int_0^1 x^{2+a-1} dx, \dots, \int_0^1 x^{2N+a-1} dx \right] [Q]^{-1} \quad (4.27)$$

Examination of equations (4.23), (4.24), and (4.25) reveals that only the collocation points are needed in order to compute matrices A and B. Once the weighting function $w(x)$, the interval of integration $a \leq x \leq b$, and the number of interior points are specified, these collocation points can be easily calculated.

Let us now consider a more general problem, such as the problem being studied in the present work, in which the symmetry property is removed. In this case then, both even and odd powers of x are included in the orthogonal polynomials in the interval 0 to 1.

In first order differential equations, where only one initial condition needs to be satisfied, a suitable trial function can be of the form

$$y(x) = y(0) + x \sum_{i=0}^N a_i P_i(x) \quad (4.28)$$

In this case, y is a polynomial of degree $(N+1)$ in x , and $(N+1)$ equations are needed in order to compute the undetermined constants a_i . These equations can be obtained by substituting equation (4.28) into the first order differential equation at the N interior collocation points, and at the end of the interval $x=1$.

For second-order differential equations, a general expression for the trial function can be of the form

$$y(x) = b + cx + x(1-x) \sum_{i=1}^N a_i P_{i-1}(x) \quad (4.29)$$

This expression contains $(N+2)$ constants that can be determined by N conditions provided by the residuals evaluated at the N interior collocation points, the N roots to $P_N(x)=0$, and two conditions provided by boundary conditions at $x=0$ and $x=1$.

If those two boundary conditions were given as $y(0)$ and $y(1)$, equation (4.29) would remain as

$$y(x) = y(0)[1-x] + y(1)x + x(1-x) \sum_{i=1}^N a_i P_{i-1}(x) \quad (4.30)$$

and therefore only N equations, at the N collocation points, are needed to specify the solution, $y(x)$.

In equation (4.28) as well as in equation (4.30), the polynomials are defined by equation (4.4) with $a=0$ and $b=1$. A general expression for the weighting function $w(x)$ can be obtained from equation (4.8) in the following way:

$$\int_0^1 (1-u^2)^{\alpha} u^{a-1} P_i(u^2) P_j(u^2) du = G_i \delta_{ij} \quad (4.31)$$

Substitute $x=u^2$, $dx=2u du$:

$$\int_0^1 (1-x)^{\alpha} x^{\frac{a}{2}-1} P_i(x) P_j(x) dx = 2G_i \delta_{ij} \quad (4.32)$$

$$\text{or} \quad \int_0^1 (1-x)^{\alpha} x^{\beta} P_i(x) P_j(x) dx = G_i^* \delta_{ij} \quad (4.33)$$

Therefore, for a non-symmetric problem, the weighting function is

$$w(x) = (1-x)^\alpha x^\beta \quad (4.34)$$

This weighting function, as it was discussed before, corresponds to shifted Jacobi polynomials, and it follows then that if $\alpha=\beta=0$, i.e., $w(x)=1$, the polynomials obtained are shifted Legendre polynomials.

In this case, it is also convenient to express the collocation equations in terms of the solution at the collocation points, $y(x_j)$, rather than in terms of the undetermined parameters, a_i . The matrices representing the first and second derivatives, and the approximate expression representing integrals, are given by the same formula as equations (4.19), (4.20), and (4.26), but with different definitions for the elements of the matrices, which now have $(N+2) \times (N+2)$ elements:

$$Q_{ji} = x_j^{i-1} \quad (4.35)$$

$$R_{ji} = (i-1)x_j^{i-2} \quad (4.36)$$

$$T_{ji} = (i-1)(i-2)x_j^{i-3} \quad (4.37)$$

In this case, the quadrature weights are

$$[W_j] = \left[\int_0^1 x^0 dx, \int_0^1 x dx, \dots, \int_0^1 x^{2N+1} dx \right] [Q]^{-1} \quad (4.38)$$

Finally, the derivatives can be expressed in terms of the solution, $y(x_j)$, at the collocation points, following the same procedure as for the symmetrical case, but with different values for matrices A and B:

$$\nabla y = \sum_{i=1}^{N+2} A_{ji} y_i \quad \text{for } j=1, \dots, N+2 \quad (4.39)$$

$$\nabla^2 y = \sum_{i=1}^{N+2} B_{ji} y_i \quad \text{for } j=1, \dots, N+2 \quad (4.40)$$

The procedure to solve a one-dimensional differential equation using this alternative orthogonal collocation method (with matrices A and B) is similar for both, the symmetrical and the non-symmetrical cases. Equations (4.21) and (4.22) for the first case, and equations (4.39) and (4.40) for the non-symmetrical case can be used to express the first and second derivatives in the ordinary differential equation. This equation is then reduced to coupled algebraic equations, with the unknowns being the solutions at the collocation points.

The boundary conditions at $x=0$ and $x=1$ can be substituted into those equations so that only N unknowns, at the interior collocation points, and N equations remain to be solved.

As was discussed before, once the interval and the problem are specified (i.e., symmetric or non-symmetric), matrices A and B depend only on the number of collocation

points. If the same number of points is always used in the solution of a problem, these matrices have to be computed only once. Therefore, it might be enough to just include them as input data rather than having a subroutine to calculate them every time the program is run again.

Several tables and some algorithms for the interval $0 \leq x \leq 1$ and different weighting functions and number of collocation points are presented in [1], [11], [31], and [32]. These tables give values of the orthogonal points, matrices A and B, and the quadrature weights W_j for the symmetric case in different geometries, and also for the non-symmetric case.

In order to have more flexibility with respect to the number of points and the weighting function to be used, two subroutines (JCBI and DFOPR presented in Appendix A) were included in the computer program in this study. These algorithms were developed by Michelsen [16].

"JCBI" computes the roots of an Nth degree Jacobi polynomial and the derivatives at these points of the polynomial or the polynomial multiplied by x, by (x-1), or by both (including one or both interval end points $x=0$ and $x=1$). In this algorithm, the weighting function is given by equation (4.34).

From the quantities calculated in "JCBI", subroutine DFOPR computes the matrices for the first and second derivatives, and also the quadrature weights.

Let us now consider a more complicated problem, the solution to a two-dimensional differential equation, where the solution ϕ is a function of the independent variables x and y .

The trial function for the symmetrical case (about $x=0$ and $y=0$) can be obtained as an extension of equation (4.7). A suitable polynomial expression for $\phi(x,y)$ and subject to the symmetry conditions, and also to the boundary conditions $\phi(x,1) = \phi(1,y) = 0$, is

$$\phi(x,y) = (1-x^2)(1-y^2) \sum_{i=0}^{N-1} \sum_{j=0}^{M-1} a_{ij} P_i(x^2) P_j(y^2) \quad (4.41)$$

Here, $P_i(x^2)$ and $P_j(y^2)$ are defined in the same way as it was done before, with the use of equation (4.8) for planar geometry.

As has been discussed before, this is not the best way of solving differential equations by orthogonal collocation. It is evident that the confusion becomes worse for two-dimensional problems. Therefore, let us discuss the alternative method where matrices A and B are used. Furthermore, let us analyze non-symmetric cases for being more general cases.

The trial function can be rewritten then as

$$\phi(x,y) = \sum_{i=1}^{N+2} \sum_{j=1}^{M+2} d_{ij} x^{i-1} y^{j-1} \quad (4.42)$$

where N and M are the number of interior collocation points in the x and y directions, respectively.

Let us analyze the x -direction first. Knowing that the partial derivatives with respect to x are at constant y , the following substitution can be made into equation (4.42):

$$e_i = \sum_{j=1}^{M+2} d_{ij} y^{j-1} \quad (4.43)$$

Substituting equation (4.43) into equation (4.42) and evaluating it at the collocation points, x_k , one obtains

$$\phi \Big|_{x_k} = \sum_{i=1}^{N+2} x_k^{i-1} e_i \quad (4.44)$$

The first and second derivatives of equation (4.42) evaluated at the collocation points are

$$\frac{\partial \phi}{\partial x} \Big|_{x_k} = \sum_{i=1}^{N+2} (i-1) x_k^{i-2} e_i \quad (4.45)$$

$$\frac{\partial^2 \phi}{\partial x^2} \Big|_{x_k} = \sum_{i=1}^{N+2} (i-1)(i-2) x_k^{i-3} e_i \quad (4.46)$$

Using matrix notation, and solving for e for the first and second derivatives, the previous expressions can be rewritten as

$$\underset{\sim}{\phi} = \underset{\sim}{\bar{Q}} \underset{\sim}{e} \quad (4.47)$$

$$\underset{\sim}{\frac{\partial \phi}{\partial x}} = \underset{\sim}{\bar{RQ}^{-1}} \underset{\sim}{\phi} = \underset{\sim}{\bar{A}} \underset{\sim}{\phi} \quad (4.48)$$

$$\underset{\sim}{\frac{\partial^2 \phi}{\partial x^2}} = \underset{\sim}{\bar{TQ}^{-1}} \underset{\sim}{\phi} = \underset{\sim}{\bar{B}} \underset{\sim}{\phi} \quad (4.49)$$

where matrices Q , R , and T are defined by equations (4.35) through (4.37).

The same procedure can be used in analyzing the y -direction. One arrives at the same equations (4.47) through (4.49), but changing x_k by y_ℓ , the collocation points in the y -direction, the derivatives now with respect to y , and performing a similar substitution as before,

$$f_j = \sum_{i=1}^{N+2} d_{ij} x^{i-1} \quad (4.50)$$

It follows then that the same A and B matrices can be used for problems in one or two dimensions.

It should be pointed out that in the latter case, after the first and second derivatives and the boundary conditions are substituted into the differential equation, a system of $(N \times M)$ algebraic equations remains to be solved.

Partial differential equations can also be reduced to coupled ordinary differential equations, if it is not desired to go further and reduce them to algebraic equations. When both dimensions are collocated, and the differential equation is reduced to algebraic equations, the notation

used (indices) is very important and can give rise to confusion.

Let us illustrate everything that has been said before by setting the collocation equations for an example presented by Villadsen and Stewart [31].

The differential equation and the boundary conditions are:

$$\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} = -1 \quad (4.51)$$

$v=0$ at $x=\pm 1$ and at $y=\pm 1$

This problem is symmetric about $x=0$ and $y=0$. Using the matrix B to represent the second derivative, and collocating the same number of points, N , in either direction, the collocation equations are

$$\sum_{i=1}^N B_{ji} v_{ik} + \sum_{i=1}^N B_{ki} v_{ji} = -1 \quad (4.52)$$

for $j=1, \dots, N$

$k=1, \dots, N$

where the index j represents the x -direction, and k the y -direction. The boundary points $v_{N+1,k} = v_{j,N+1} = 0$ have already been substituted into equation (4.52). Equation (4.51) then has been reduced to a system of $(N \times N)$ algebraic equations, i.e., equation (4.52).

A similar analysis as done previously can be made for problems in more than two dimensions. It follows that,

as derived before, the same matrices and procedure can be used to reduce partial differential equations to coupled ordinary differential equations or algebraic equations by using the orthogonal collocation method.

Comparison to Finite Difference Techniques

Examination of the orthogonal collocation method, as presented previously, where a problem is solved for the solution at the collocation points rather than for the arbitrary coefficients in the expansion, leads to the conclusion that the equations which must finally be solved are more compact and easier to formulate, than those associated with conventional finite difference techniques.

Once a problem is converted into partial differential equations with the initial and boundary conditions known, and each term in these equations expressed as a function of the independent variables, the development of the collocation equations presents no difficulty.

The orthogonal collocation method is therefore a simple numerical technique most suitable for machine computation and with proven fast conversion.

Most of the previous models for solving air pollution problems neglect some of the terms in the general diffusion equation, so that the resulting equation is less complicated to solve. The use of the orthogonal collocation method,

as discussed before, will not introduce extra complications in the formulation of the final equations and their solution if those terms are not assumed to be negligible. Therefore, it will not be more difficult if a general case (four independent variables, the three directions and time) is solved, even with a non-linear reaction term.

Another advantage of the collocation method is that a much smaller number of points may be used since the solution at each point is influenced directly by the value at all the collocation points, as is the case for the exact solution, instead of depending directly on only neighboring grid points as is the case in finite difference schemes. In this respect then, the collocation method requires less computation time than a finite difference solution of comparable accuracy. This has been proved in several applications, some of them discussed next.

Ferguson and Finlayson [9] applied orthogonal collocation to a linear unsteady-state diffusion problem in a slab. They reported that the collocation solution is more accurate than finite difference solutions which use three to twelve times as many spatial grid points (they only collocated in the spatial coordinate and solved the resulting ordinary differential equations).

Ferguson and Finlayson also solved the diffusion of mass and energy in a spherical catalyst pellet with an

exothermic first-order irreversible reaction. Here, they again collocated only in the x-direction and these equations were integrated using Hamming's method. In this case, Ferguson and Finlayson demonstrated that the number of collocation points can be about ten times less than the number of finite difference grid points for equivalent accuracy. In terms of time, the best collocation solution was about twenty times (or more) as fast as a finite difference solution of about the same accuracy.

Finlayson [10] used orthogonal collocation to solve a two-dimensional (axial and radial directions) packed bed reactor under the assumptions of constant physical properties, plug flow, and a reaction governed by the conversion and temperature. Collocation was applied in the radial axis, and the resulting differential equations integrated using the Runge-Kutta method and the Euler method.

Comparison between collocation solutions and finite difference calculations using a Crank-Nicholson implicit method were reported to be in some cases from two to four times faster for equivalent accuracy. In some other cases, the collocation method was twice as fast and ten times as accurate or four times as fast and five times as accurate.

Finlayson [11] also applied collocation in the axial direction in place of the Runge-Kutta method used before, and solved the resulting set of algebraic equations by an iterative procedure proposed by Villadsen [32]. The solution obtained by this way was about three times faster than the one using the Runge-Kutta method for equivalent accuracy.

Finlayson [11] also solved the problem of tubular reactors with only axial dispersion (concentration and temperature). For this case, when orthogonal collocation was applied, the governing equations were reduced to a set of nonlinear algebraic equations for the concentration and temperature at the collocation points. He used the Newton-Raphson method to solve them, and compared this solution to those given in the literature using finite difference schemes.

Finlayson used six collocation points in order to obtain the same accuracy as reported for both a 100-grid point finite difference solution for the isothermal case and 481 grid points for the non-isothermal case.

Application to Turbulent Diffusion in the Atmosphere

As was discussed before, only finite-difference has been used previously to solve for the concentration distribution in atmospheric diffusion processes. The analysis

made in the preceding section leads to the conclusion that air pollution modeling could be improved by the use of the orthogonal collocation method as the numerical technique for solving the general diffusion equation. This equation, for a single species which will be the case studied in the present work⁽¹⁾, is repeated here for convenience.

$$\begin{aligned} \frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} + w \frac{\partial C}{\partial z} = & \frac{\partial}{\partial x} \left(K_x \frac{\partial C}{\partial x} \right) + \frac{\partial}{\partial y} \left(K_y \frac{\partial C}{\partial y} \right) + \\ & + \frac{\partial}{\partial z} \left(K_z \frac{\partial C}{\partial z} \right) + R \end{aligned} \quad (4.53)$$

Some of the attractive properties that orthogonal collocation has are its flexibility and easy handling of any variable or component in the diffusion equation, as compared to other numerical methods used in previous works. The model does not increase in difficulty if all the terms involved in equation (4.53) are incorporated in it. That is, a similar amount of work in formulating the collocation equations, but not computer time in solving them, has to be done if three instead of two dimensions are considered in the model. The same reasoning applies for all the components of the wind velocity and turbulent diffusivity, and the chemical reactions. Therefore, it is

(1) Symbols indicating averaged quantities will be omitted henceforth. All velocities and concentrations, however, continue to be time averaged quantities.

not necessary to assume that some terms are negligible in order to be able to obtain results, which in such a case would be applicable only for some particular situations.

With the present approach then, it is possible to simulate many types of atmospheric conditions. But to do so, it is necessary to express all the properties in equation (4.53) in an analytical form. This has been done in a flexible way by introducing several parameters in the expressions representing those properties, so that different input data can be supplied if different atmospheric conditions are to be tested.

Before applying orthogonal collocation to the present model, let us obtain those expressions for the initial and boundary conditions, turbulent diffusivities, velocity profiles, and chemical reaction.

Initial and Boundary Conditions

The initial conditions necessary for an unsteady state model can be expressed as follows,

$$C = C_B \quad \text{at } t=0 \quad \text{and any } (x,y,z) \quad (4.54)$$

where C_B is a constant and in general can be a function of x , y , and z .

These conditions are required to start the calculations performed by the integrating subroutine, and therefore are generated in the MAIN of the computer program. For all the cases studied in the present work, there was no background concentration and thus C_B was equated to zero.

The boundary conditions at the ground, $z=0$, and at the inversion base, $z=H$, are obtained by assuming that both completely reflect the diffusing pollutant, i.e.,

$$\frac{\partial C}{\partial z} = 0 \quad \text{at } z=0, H \text{ for any } x \text{ and } y \quad (4.55)$$

These two boundary conditions for the z direction are converted into collocation equations and then incorporated in the diffusion equation, as it will be seen later in this chapter. If for a particular case the gradient in equation (4.55) is not equal to zero, e.g.

$$-K_z \frac{\partial C}{\partial z} = Q_s(x, y, t) \quad \text{at } z=0 \text{ for any } x \text{ and } y \quad (4.56)$$

where $Q_s(x, y, t)$ is the surface flux of the pollutant studied, the collocation equations resulted from conditions (4.55) have to be changed.

The bulk transport of the pollutant is due primarily to the effect of the x -component of the wind velocity. Therefore, it can be assumed that at certain distance in the y -direction, the mean concentration is negligible, i.e.

$$C \rightarrow 0 \quad \text{at } y = -y_{\max}, y_{\max} \text{ for any } x \text{ and } z \quad (4.57)$$

where $2 \cdot y_{\max}$ is the entire region of interest. In general,

$$C = f(x, z, t) \quad \text{at } y = -y_{\max}, y_{\max} \\ \text{for any } x \text{ and } z \quad (4.58)$$

This can also be included in the model by changing the resulting collocation equations from conditions (4.57).

For the purposes of solving equation (4.53), it is necessary to define the location of the sources. These sources can be defined with the aid of a boundary condition in the x-direction.

Let us consider a general case, i.e., a multiple source problem, where there is more than one source involved. If the position of the i th source is defined by the coordinate point $(JS(i), KS(i), LS(i))$, the boundary condition related to the i th source is given by

$$C = \begin{cases} C_o(i, t) & \text{at } x=JS(i), y=KS(i), z=LS(i) \\ 0 & \text{at } x=JS(i) \text{ and any other } y \text{ and } z \end{cases} \quad (4.59)$$

where $C_o(i, t)$ is the i th source concentration, and in general a function of time. For the purpose of studying different situations, each C_o , assumed constant in the present model, and its position is supplied as input information. The way of handling multiple source will be discussed in detail in Chapter V.

As a convention, and knowing that for any case there will be at least one source, the first source will always be at $x=0$, that is $JS(1)=0$. Therefore, if the problem involves only one source, the boundary condition in the x -direction is given by

$$C = \begin{cases} C_o(1) & \text{at } x=0, y=KS(1), z=LS(1) \\ 0 & \text{at } x=0 \text{ and any other } y \text{ and } z \end{cases} \quad (4.60)$$

Sometimes the emission rate (mass/time) and not the source concentration is given as information. This problem can be overcome by the use of quadrature weights in orthogonal collocation and will be discussed later in Chapter V.

There is no need for a second boundary condition in the x -direction, due to the assumption of negligible turbulent diffusivity in this direction. This will be discussed in the next section.

Turbulent Diffusivities, K_z

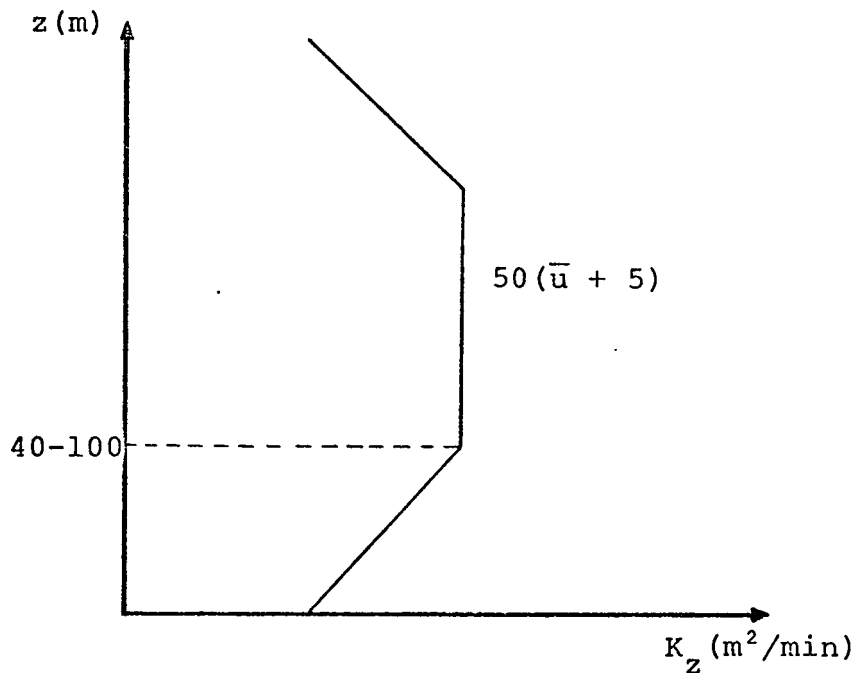
Eschenroeder and Martinez [7] assumed a trapezoidal shaped vertical profile from the ground up to the inversion base for K_z , the turbulent diffusion coefficient in the vertical direction. At low levels, K_z increases linearly with z to some constant value. At intermediate levels, K_z then is constant. As the mixing depth top is

approached, K_z decreases linearly with increasing z . The ground level and inversion layer values are assumed to be equal. The maximum constant value is expected to vary with wind speed approximately like

$$K_z = 50(\bar{u}+5) \quad \text{m}^2/\text{min} \quad (4.61)$$

where $\bar{u}$ is in m/s. This equation starts applying from an elevation of 40 to 100 meters, depending upon meteorological conditions:

Figure 4.1: Variations of Diffusivity with Height



Eschenroeder et al. [8] reviewed their previous work based on more experimental data and concluded that equation (4.61) gives an estimate of vertical diffusivity only in the neutral stability range, and that temperature gradients are apparently far more influential than wind speed in determining vertical diffusivity values.

As an improvement on their previous approach, the dependence on wind speed was dropped, and the diffusivity profiles were reconstructed to represent the broad stability categories (defined by Pasquill and Gifford [30]), as shown in Figure 4.2.

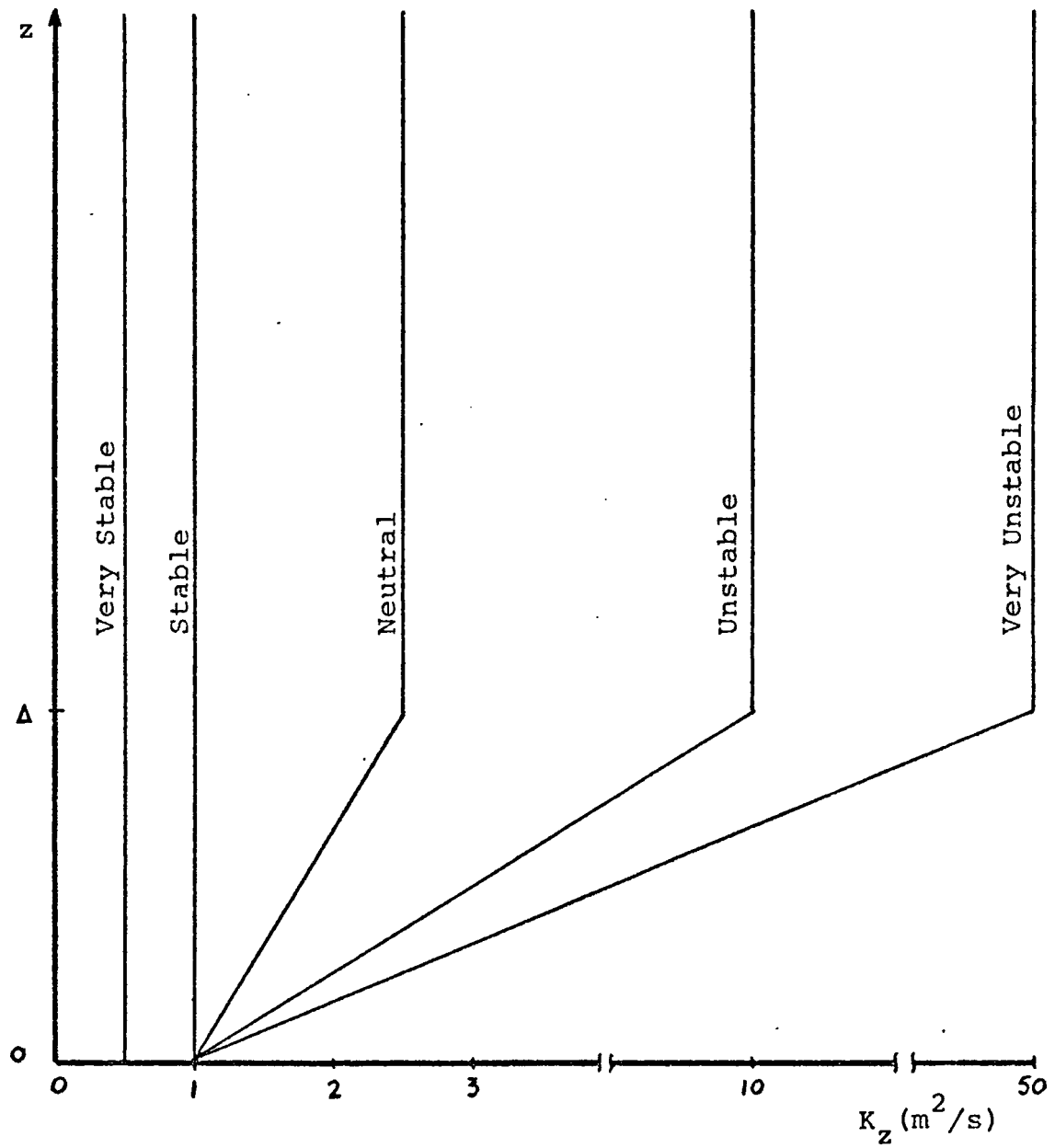
The knee height Δ , where the constant values for K_z apply, varies between 25m to 75m above the ground, depending on the height range of the model and the mesh interval size.

Eschenroeder et al. assumed constant diffusivity profiles all the way to the top because of their little influence for the space and time scales in their calculations at the top of the mesh.

In the present model, the calculation procedure for the turbulent diffusivities is based upon the latter approach used by Eschenroeder et al. [8]. Using their approach, K_z will depend only on the stability class and the vertical direction. Some slight changes were made in that approach and are now discussed.

Figure 4.2: Vertical Diffusivity Profiles.

$$(1 \leq \bar{u} \leq 7 \text{ m/s})$$



An additional stability class, between the neutral and unstable, was incorporated in the model so that the six classes presented by Turner [13] could be taken into account.

The knee height Δ , was made dependent on the stability class, as suggested by Pasquill [18], so that the more unstable the conditions, the higher the knee.

The last change made to Eschenroeder's approach was to remove their assumption of constant diffusivity profiles from intermediate levels all the way to the top. As the mixing depth top is approached then, the turbulent diffusivities decrease linearly with increasing z , and the ground level and inversion layer values are assumed to be equal. This is done for the last 100 meters of the z -dimension, with $H \geq 300\text{m}$.

Taking all these changes into account, Figure 4.2 remains as shown in Figure 4.3.

This model was implemented in the computer program by using the following equations⁽¹⁾:

For $\text{ISTB} \leq 4$:

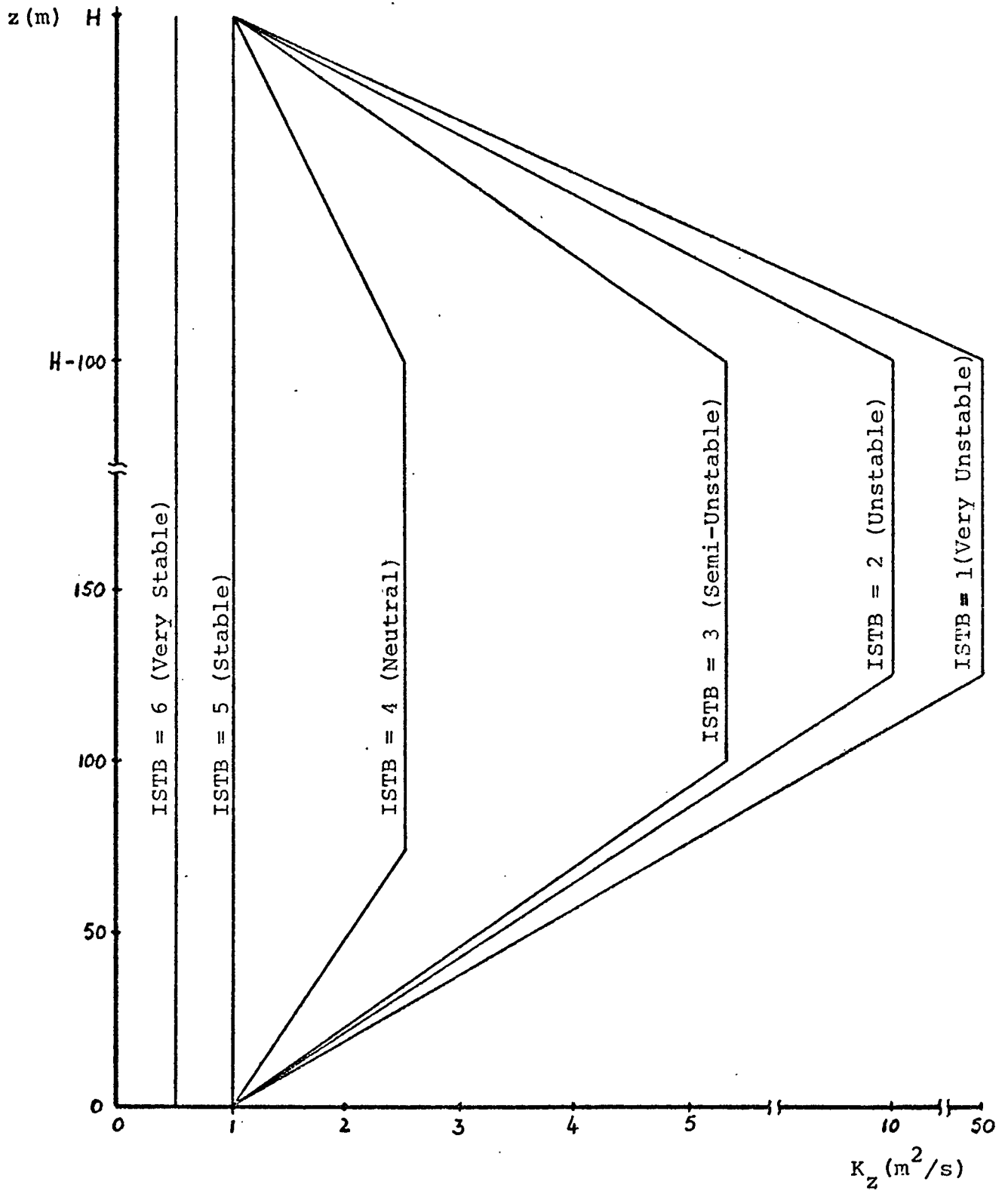
$$K_z = \text{COEFK}(\text{ISTB}) \cdot z/\Delta(\text{ISTB}) + 60., \text{ for } z < \Delta(\text{ISTB})$$

$$K_z = \text{COEFK}(\text{ISTB}) + 60., \quad \text{for } \Delta(\text{ISTB}) \leq z \leq (H-100)$$

$$K_z = \text{COEFK}(\text{ISTB}) \cdot (H-z)/100 + 60., \text{ for } z > (H-100)$$

(1) In the computer program the units for K_z are m^2/min .

Figure 4.3: Vertical Diffusivity Profiles
in the Present Model.



$$\begin{aligned}
\text{where, } \text{COEFK}(1) &= 2940 & \Delta(1) &= 125 \\
\text{COEFK}(2) &= 540 & \Delta(2) &= 125 \\
\text{COEFK}(3) &= 258 & \Delta(3) &= 100 \\
\text{COEFK}(4) &= 90 & \Delta(4) &= 75
\end{aligned} \tag{4.62}$$

For ISTB = 5: $K_z = 60 \text{ m}^2/\text{min}$, for any z
for ISTB = 6: $K_z = 30 \text{ m}^2/\text{min}$, for any z

In order to have a flexible model, the stability class, ISTB, is supplied as input information by the user. Because of the fact that once it is defined it remains the same during the simulation, the algorithm that calculates the turbulent diffusivities at each orthogonal point was incorporated in the MAIN of the computer program.

In the region of interest, the turbulence is almost perfectly isotropic, and even below 100 meters, the degree of isotropy seems to be sufficiently high in order to consider, as Sutton [28] has suggested, that K_y varies in an identical way as K_z . In addition, most of the previous models, discussed in Chapter III, considered a constant turbulent diffusivity in the y direction. This suggested then to relate, in the present model, K_y to K_z in the following manner:

$$K_y = \alpha K_z'(\text{ISTB}) \tag{4.63}$$

where α is a positive constant which has to be supplied as input information by the user, and K'_z is the maximum constant value for K_z and thus dependent only on the stability class.

In the present model, the turbulent diffusivity in the x-direction will be neglected as compared to the mean wind velocity. The reason being that its behavior is not well understood and in most of the cases it has no significant effect on the results [24].

Velocity Profiles

Davies [5], Pasquill [17], Smith [26], Tennekes and Lumley [29], and others have developed expressions for the velocity profiles especially in the mean flow direction. Two equation forms have been used often in previous studies. A semi-logarithmic form for rough flows, of the type

$$\bar{u}(z) = \frac{u_*}{k_0} \ln\left(\frac{z}{z_0}\right) \quad (4.64)$$

where u_* is the friction velocity, k_0 the von Karman's constant, and z_0 a length characterizing the effect of the surface roughness.

The second is a power law equation which has the following form:

$$\bar{u}(z) = \bar{u}_1 \left(\frac{z}{z_1} \right)^m \quad (4.65)$$

where $\bar{u}_1$ is the mean velocity at a reference height z_1 , and m is a constant.

For this problem, the latter form describes in a better way the mean velocity in the x-direction. Therefore, equation (4.65) will be used in the diffusion equation.

This form of the velocity profile is used for the lower part of the z dimension, that is from the ground level to the knee height Δ , previously defined, and from this elevation up to the mixing depth top a constant value for the velocity is used, UST. This means then that u will depend on the stability class, z , and the parameters u_1 , z_1 , m , and UST.

Usually UST, the geostrophic wind speed, is the easiest value to obtain whether by experimental data or previous records of the zone in question. This is the reason why UST is required as input information in the model.

Having in mind further adjustments for u , the constant m has also to be provided as input information by the user. This exponent m is a number which varies from

0.1 to 0.4, depending on the roughness of the ground surface as well as on atmospheric stratification. The rougher the terrain, i.e., the larger the surface obstructions, the thicker will be the affected layer of air, and the more gradual will be the increase of velocity with height. Thus, as the roughness increases, the exponent m increases, as it is shown in Table 4.1 which was presented by Seinfeld [22]:

TABLE 4.1 : ESTIMATES FOR m in eq.(4.65)

	<u>Type of terrain</u>		
	<u>open country</u>	<u>suburbs</u>	<u>urban</u>
m	.16	.28	.40

The stability limits of m , also presented by Seinfeld [22], are:

$$m = \begin{cases} .83 & \text{very stable} \\ 1/7 & \text{neutral} \\ .02 & \text{very unstable} \end{cases}$$

For purposes of continuity calculations (see Chapter V) the ground level value for the mean wind velocity in the x-direction, UGR, is also taken into consideration in the model and is supplied as input information. If its value is not known at the moment of simulating a case,

as it happened in this work, it can be assumed to be equal to the friction velocity, u_* .

The algorithm for obtaining u then, as used in the MAIN program, is described by the following equations:

For $ISTB \leq 4$:

$$\begin{aligned} u &= UGR & \text{for } z = 0 \\ u &= UST \left(\frac{z}{\Delta(ISTB)} \right)^{AM} & \text{for } 0 < z < \Delta(ISTB) \\ u &= UST & \text{for } z \geq \Delta(ISTB) \end{aligned}$$

For $ISTB > 4$: (4.66)

$$\begin{aligned} u &= UGR & \text{for } z = 0 \\ u &= UST & \text{for } z > 0 \end{aligned}$$

In almost all the previous works in air pollution modeling, the y -component of the mean wind velocity as well as the z -component are assumed to be negligible.

As it was discussed before, the present model does not increase in difficulty by including more than one component for the mean wind velocity. In spite of this, it has been difficult to obtain equation forms for the other two components of the wind velocity. Therefore, it will be assumed that w , the vertical component is negligible, and that v , the y -component is some fraction of u .

To make a general case for this study, let us consider that v also varies with respect to time in a linear

dependence until it reaches its maximum value. Because of this dependency on time, the algorithm used to its calculation, as described by the following equations, was incorporated in a subroutine called FCT:

$$v = Pu \frac{t}{TCH} \quad \text{for} \quad 0 \leq t < TCH \quad (4.67)$$

$$v = Pu \quad \text{for} \quad t \geq TCH$$

where P is a constant that will determine the direction of the mean wind velocity, and TCH another parameter that will specify the time required for v to change from its value at $t=0$ to its maximum value, $P \cdot u$. Both, P and TCH have to be supplied as input information in the computer program by the user.

Chemical Reactions

In the development of equation (2.6), the general diffusion equation, an approximation concerning the chemical reaction term was made: the term $\langle R_i(\langle C_1 \rangle + C_1', \dots, \langle C_s \rangle + C_s') \rangle$ was replaced by $\langle R_i(\langle C_1 \rangle, \dots, \langle C_s \rangle) \rangle$, i.e., the effect of concentration fluctuations on the rate of reaction was neglected. This is true only for first-order reactions, however, conditions under which this assumption is valid can be obtained for higher order reactions.

Lamb [15] analyzed this problem for a two-dimensional turbulent fluid transporting a single chemical species

involving a nonlinear chemical reaction (second-order reaction). In this case, the chemical reaction term is expressed by

$$R = -k[\langle C \rangle^2 + \langle C'^2 \rangle] \quad (4.68)$$

He concluded that the replacement of equation (4.68) by $-k\langle C \rangle^2$ is valid when the reaction process is slow compared with turbulent transport and the characteristic length and time scales for changes in the mean concentration field are large compared with the corresponding scales for turbulent transport.

Although these conditions were derived for a relatively simple two-dimensional case, the essential aspects of those restrictions were found to apply to the general three-dimensional equation as well. In addition, they give a good indication of the conditions of validity for general R_i .

Let us turn our attention now to the mechanisms of removal of sulfur dioxide in the atmosphere, since this will be the chemical species used to validate the present model.

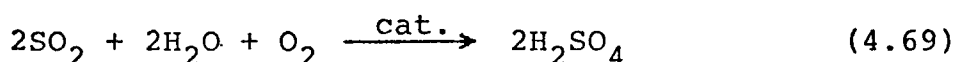
Although a great deal of importance has been given to sulfur oxides, in particular sulfur dioxide, the chemistry of sulfur dioxide in the atmosphere is still far from being fully understood.

The removal of SO_2 in the atmosphere is quite complex and can take place through several mechanisms. It has

been suggested that atmospheric SO_2 can undergo oxidation to sulfates by mainly two mechanisms: catalytic (heterogeneous) oxidation and photochemical (homogeneous) oxidation. However, sulfur dioxide is removed from the atmosphere not only by oxidation, but also by sedimentation, rainout and washout.

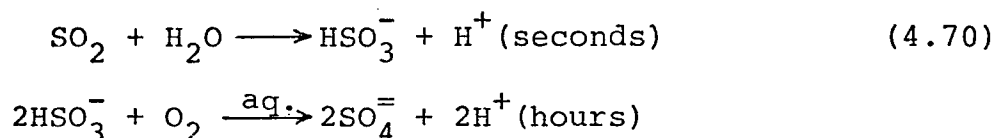
Photochemical oxidation of SO_2 is apparently a gas-phase process consisting of several chemical reactions. In the presence of air, SO_2 is oxidized to SO_3 when exposed to solar radiation, and if water is present, the SO_3 is rapidly converted to sulfuric acid. The conversion of SO_2 to SO_3 involves excited SO_2 molecules, oxygen, and oxides of sulfur other than SO_2 . Although photochemical oxidation of SO_2 can take place in clean air, the more important process of SO_2 photooxidation occurs in atmospheres containing hydrocarbons and oxides of nitrogen. In this case, the rate of conversion of SO_2 to SO_3 increases markedly over that observed in pure air.

Catalytic oxidation is the principal process for SO_2 conversion under conditions of high humidity and high particulate concentration. It occurs in aqueous solution, involves both water and dissolved O_2 , and requires the presence of a catalyst. The overall reaction can be expressed as



Catalysts for this reaction include several metal salts, such as sulfates and chlorides of manganese and iron. However, most of the recent work has been dedicated to manganous salts only.

The same reaction can also occur without the presence of a catalyst, as discussed by Worley [34], and shown in the following equations,



In the sedimentation or deposition process, SO_2 behaves as if it were a particle with a settling velocity. Rainout and washout also serve as additional removing mechanisms. Rainout is the incorporation of gaseous SO_2 in cloud droplets, while washout is the removal of SO_2 by rain falling through air masses below the cloud level. Once SO_2 is absorbed, it is converted via oxidation (4.70)-the heterogenous aspect causes apparent SO_2 level to fall.

As it can be observed, a model that would take into account all the possible mechanisms for SO_2 removal in the atmosphere and all the variables involved would be quite complex.

Because of the fact that the processes previously discussed are not very well understood yet, and the incorporation and thus the study of such a complex model is not the main objective in the present work, only photochemical oxidation will be considered here. Furthermore, the reactions taking place in a system of SO_2 , hydrocarbons, NO_x , and air are probably the least well understood of all those in atmospheric chemistry, and thus will not be considered either.

Since data for photochemical oxidation in clean air are extremely scattered, a simplified first order reaction model will be used to represent SO_2 removal from the atmosphere,

$$R = -kC \quad (4.71)$$

where k is the reaction rate constant. The value of 5.8×10^{-5} per minute or 0.35% loss of SO_2 per hour, used by Hallidy and Anderson [12] in their work will be the rate constant in the present model, and must be supplied as input information in the computer program.

Development of the Collocation Equations

The diffusion equation to be solved, and the corresponding initial and boundary conditions, under the assumptions previously discussed, are:

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = \frac{\partial}{\partial y} (K_y \frac{\partial C}{\partial y}) + \frac{\partial}{\partial z} (K_z \frac{\partial C}{\partial z}) + R \quad (4.72)$$

$$C = 0 \quad \text{at } t=0, \text{ and any } (x, y, z) \quad (4.73)$$

$$\frac{\partial C}{\partial z} = 0 \quad \text{at } z=0, H \text{ for any } x \text{ and } y \quad (4.74)$$

$$C^{(*)} = \begin{cases} C_o(1) & \text{at } x=0, y=KS(1), z=LS(1) \\ 0 & \text{at } x=0, \text{ and any other } y \\ & \text{and } z \end{cases} \quad (4.75)$$

$$C = 0 \quad \text{at } y = -y_{\max}, y_{\max} \quad (4.76)$$

for any x and z

In equation (4.72), the velocity profiles are assumed to be,

$$u = \psi(z, ISTB) \quad (4.77)$$

$$v = \eta(z, t, ISTB) \quad (4.78)$$

the turbulent diffusivities,

$$K_y = \xi(ISTB) \quad (4.79)$$

$$K_z = \zeta(z, ISTB) \quad (4.80)$$

and the rate of reaction,

$$R = -kC \quad (4.81)$$

For this problem, let us transform the spatial coordinates to yield limits of 0 to 1 by the following procedure:

(*) The multiple sources case will be discussed in Chapter V.

$$x^* = \frac{x}{x_{\max}} \quad (4.82)$$

$$y^* = \frac{\frac{y}{y_{\max}} + 1}{2} \quad (4.83)$$

$$z^* = \frac{z}{H} \quad (4.84)$$

For simplicity, from now on the asterisk will be dropped out from the independent variables, x^* , y^* , and z^* .

Substituting equations (4.77) through (4.84) into equation (4.72) one obtains

$$\begin{aligned} \frac{\partial C}{\partial t} + R_1 \frac{\partial C}{\partial x} + R_2 \frac{\partial C}{\partial y} - R_3 \frac{\partial C}{\partial z} = R_5 \frac{\partial^2 C}{\partial y^2} + \\ + R_6 \frac{\partial^2 C}{\partial z^2} - kC \end{aligned} \quad (4.85)$$

where

$$R_1(z) = \psi(z, \text{ISTB}) \frac{1}{x_{\max}} \quad (4.86)$$

$$R_2(z, t) = \eta(z, t, \text{ISTB}) \frac{1}{2y_{\max}} \quad (4.87)$$

$$R_3(z) = \frac{d\{\zeta(z, \text{ISTB})\}}{dz} \frac{1}{H^2} \quad (4.88)$$

$$R_5 = \xi(\text{ISTB}) \cdot \frac{1}{4y_{\max}^2} \quad (4.89)$$

$$R_6(z) = \zeta(z, \text{ISTB}) \frac{1}{H^2} \quad (4.90)$$

There are many ways in which orthogonal collocation can be applied to equation (4.85), but it is chosen to collocate only in the three directions, x , y , and z , so that a system of ordinary differential equations with respect to time is left to be solved. The reason of doing this is because the solution of the diffusion equation is primarily wanted at any instant of time.

If the emission source is put in the middle of the interval in the y -direction, and only the x -component of the wind velocity is taken into account, then by examining the boundary conditions it can be concluded that this problem would be symmetric with respect to y . Since this is only a particular case, it is better to apply the equations for a non-symmetric case to every direction.

In doing this, let N_x , N_y , and N_z be the number of collocation points in the x , y , and z directions, respectively, and C_{jkl} the mean concentration at the point (x_j, y_k, z_l) .

Equation (4.85) remains then as,

$$\begin{aligned}
 \frac{dC_{jkl}}{dt} + R_1(l) \sum_{i=1}^{N_x+2} A_{ji}^{(1)} C_{ikl} + R_2(l,t) \sum_{i=1}^{N_y+2} A_{ki}^{(2)} C_{jil} - \\
 - R_3(l) \sum_{i=1}^{N_z+2} A_{li}^{(3)} C_{jki} = R_5 \sum_{i=1}^{N_y+2} B_{ki}^{(2)} C_{jil} + \\
 + R_6(l) \sum_{i=1}^{N_z+2} B_{li}^{(3)} C_{jki} - kC_{jkl}
 \end{aligned} \tag{4.91}$$

for $j=1, \dots, N_x+2$
 $k=1, \dots, N_y+2$
 $l=1, \dots, N_z+2$

As discussed before, matrices A and B depend on the number of collocation points. For a general case, that number of points can be different for each direction and therefore, A and B would be different. Furthermore, N_x , N_y , and N_z could be changed between runs. These reasons lead to the conclusion that it is better to include subroutines JCBI and DFOPR in the computer program rather than putting matrices A and B as input data each time the collocation points are changed.

In equation (4.91), the indices of matrices A and B represent the direction and thus the way they are computed, i.e., (1), (2), and (3) stand for the x, y, and z directions, respectively.

The application of orthogonal collocation to the boundary conditions, equations (4.74) through (4.76), gives the following expressions:

$$\sum_{i=1}^{N_z+2} A_{li}^{(3)} C_{jki} = 0 \quad \text{at } z=0 \quad (4.92)$$

$$\sum_{i=1}^{N_z+2} A_{N_z+2,i}^{(3)} C_{jki} = 0 \quad \text{at } z=1 \quad (4.93)$$

$$C_{1k\ell} = \begin{cases} C_o(1) & \text{at point source} \\ 0 & \text{elsewhere} \end{cases} \quad (4.94)$$

$$C_{j1\ell} = 0 \quad \text{at } y=0 \quad (4.95)$$

$$C_{jN_y+2\ell} = 0 \quad \text{at } y=1 \quad (4.96)$$

Equations (4.92) and (4.93) can also be written as

$$A_{11}^{(3)} C_{jkl} + \sum_{i=2}^{N_z+1} A_{1i}^{(3)} C_{jki} + A_{1N_z+2}^{(3)} C_{jKN_z+2} = 0 \quad (4.97)$$

$$\begin{aligned} A_{N_z+2,1}^{(3)} C_{jkl} + \sum_{i=2}^{N_z+1} A_{N_z+2,i}^{(3)} C_{jki} + \\ + A_{N_z+2N_z+2}^{(3)} C_{jKN_z+2} = 0 \end{aligned} \quad (4.98)$$

Solving for C_{jkl} and C_{jKN_z+2} one obtains:

$$C_{jKN_z+2} = \frac{\sum_{i=2}^{N_z+1} (A_{11}^{(3)} A_{N_z+2,i}^{(3)} - A_{N_z+2,1}^{(3)} A_{1i}^{(3)}) C_{jki}}{A_{N_z+2,1}^{(3)} A_{1N_z+2}^{(3)} - A_{11}^{(3)} A_{N_z+2N_z+2}^{(3)}} \quad (4.99)$$

$$C_{jkl} = - \frac{A_{1N_z+2}^{(3)} C_{jKN_z+2} + \sum_{i=2}^{N_z+1} A_{1i}^{(3)} C_{jki}}{A_{11}^{(3)}} \quad (4.100)$$

These expressions can be simplified by defining,

$$\text{DEN} = A_{N_z+2,1}^{(3)} A_{1N_z+2}^{(3)} - A_{11}^{(3)} A_{N_z+2N_z+2}^{(3)} \quad (4.101)$$

$$APAl(i) = \frac{A_{11}^{(3)} A_{N_z+2i}^{(3)} - A_{N_z+21}^{(3)} A_{1i}^{(3)}}{DEN} \quad (4.102)$$

so that equation (4.99) remains as

$$C_{jkN_z+2} = \sum_{i=2}^{N_z+1} APAl(i) C_{jki} \quad (4.103)$$

In cases where there is no inversion layer at the maximum elevation, H , as it has been assumed so far, a new boundary condition at this point can be assumed as

$$C = 0 \quad \text{at} \quad z=H \quad \text{for any } x \text{ and } y \quad (4.104)$$

This condition can be easily included in equation (4.103):

$$C_{jkN_z+2} = \sum_{i=2}^{N_z+1} APAl(i) C_{jki} \quad INVRS \quad (4.105)$$

where $INVRS=1$ means that there is inversion at $z=H$, and $INVRS=0$ means that there is no inversion and the concentration at $z=H$ is equal to zero.

By substituting equations (4.94) through (4.96), equation (4.91) remains as follows:

$$\begin{aligned}
\frac{dC_{jkl}}{dt} + S(j) + R_1(\ell) \sum_{i=2}^{N_x+2} A_{ji}^{(1)} C_{ikl} + R_2(\ell, t) \sum_{i=2}^{N_y+1} A_{ki}^{(2)} C_{jil} - \\
- R_3(\ell) A_{\ell 1}^{(3)} C_{jkl} - R_3(\ell) \sum_{i=2}^{N_z+1} A_{\ell i}^{(3)} C_{jki} - \\
- R_3(\ell) A_{\ell N_z+2}^{(3)} C_{jN_z+2} = R_5 \sum_{i=2}^{N_y+1} B_{ki}^{(2)} C_{jil} + \\
+ R_6(\ell) B_{\ell 1}^{(3)} C_{jkl} + R_6(\ell) \sum_{i=2}^{N_z+1} B_{\ell i}^{(3)} C_{jki} + \\
+ R_6(\ell) B_{\ell N_z+2}^{(3)} C_{jN_z+2} - kC_{jkl} \quad (4.106)
\end{aligned}$$

And rearranging,

$$\begin{aligned}
\frac{dC_{jkl}}{dt} = -S(j) - R_1(\ell) \sum_{i=2}^{N_x+2} A_{ji}^{(1)} C_{ikl} + \\
+ [R_3(\ell) A_{\ell 1}^{(3)} + R_6(\ell) B_{\ell 1}^{(3)}] C_{jkl} + \\
+ [R_3(\ell) A_{\ell N_z+2}^{(3)} + R_6(\ell) B_{\ell N_z+2}^{(3)}] C_{jN_z+2} + \\
+ \sum_{i=2}^{N_z+1} [R_3(\ell) A_{\ell i}^{(3)} + R_6(\ell) B_{\ell i}^{(3)}] C_{jki} + \\
+ \sum_{i=2}^{N_y+1} [R_5 B_{ki}^{(2)} - R_2(\ell, t) A_{ki}^{(2)}] C_{jil} - kC_{jkl} \quad (4.107)
\end{aligned}$$

or,

$$\begin{aligned}
 \frac{dC_{jkl}}{dt} = & -S(j) - R_1(\ell) \sum_{i=2}^{N_x+2} A_{ji}^{(1)} C_{ikl} + R361(\ell) C_{jkl} + \\
 & + R362(\ell) C_{jkN_z+2} + \sum_{i=2}^{N_z+1} R36I(\ell, i) C_{jki} + \\
 & + \sum_{i=2}^{N_y+1} R52I(\ell, k, i, t) C_{jil} - k C_{jkl}
 \end{aligned} \tag{4.108}$$

$$\text{for } j=2, \dots, N_x+2$$

$$k=2, \dots, N_y+1$$

$$\ell=2, \dots, N_z+1$$

where

$$S(j) = \begin{cases} R_1(LS(1)) A_{j1}^{(1)} C_o(1) & \text{at } k=KS(1) \\ & \ell=LS(1) \\ 0 & \text{elsewhere} \end{cases} \tag{4.109}$$

and C_{jkl} and C_{jkN_z+2} are given by equations (4.100) and (4.105), respectively.

Equation (4.108) gives then a set of $(N_x+1)(N_y)(N_z)$ first-order ordinary differential equations to solve for the concentration as a function of time at the orthogonal collocation points in the three directions, x , y , and z .

Chapter V

FORMULATION OF CALCULATIONAL SCHEME

Calculation Procedure

It has previously been shown that the solution to the turbulent diffusion process in the atmosphere can be obtained by the use of the K-theory, which can be accomplished by solving a partial differential equation. Orthogonal collocation simplifies this, reducing that equation to a system of first-order ordinary differential equations with respect to time.

The basic calculational procedure then is to solve that system of equations (4.108) on a digital computer. There are several methods that can be used for this purpose, but in this work it was decided to use RKGS, a subroutine furnished by IBM [14] which in essence is a fourth-order Runge-Kutta method.

In addition to RKGS, two other subroutines must be supplied: A function subroutine, called FCT in the computer program (see Appendix A), where the system of first-order ordinary differential equations to be solved are provided; and an output subroutine, called OUTP in the computer program, which will print the results computed by RKGS.

In RKGS, the integration is performed with respect to time, and therefore the solution of the problem can be obtained at any moment. However, it is usually desired to print it only at every defined interval of time. Having this in mind, an algorithm that uses a variable called PRDEL was incorporated in OUTP so that it will allow the computer to print the results only every PRDEL units of time.

Due to the nature of orthogonal collocation, small oscillations can be introduced in the solution of the problem. Although these are part of the true solution of the collocation equations, there might be small negative concentrations as output for points that follow zero levels of concentration. Because of this, and by suggestions of Stewart [27] and Villadsen [33], a subroutine called ZERO is always called before printing the results. This subroutine will convert all the concentration values that follow the zero level to zero. This testing is done in all three directions.

Because of the fact that actual data are available as average concentrations, the computer program contains a subroutine called AVG, which will convert the solution to a time average solution, so that a comparison to experimental data can be performed. To do this, AVG subroutine computes the time average concentrations at

every collocation point for three consecutive points in time; i.e., θ , t , and Ω , where t is any point in time, $\theta (=t-PRDEL)$ is the time between the pollutant release ($t=0$) and the initiation of the averaging time, and $\Omega (=t+PRDEL)$ is the end of the averaging time. In order to reduce the program storage requirement, AVG subroutine is performed by direct-access input/output statements.

Multiple sources

In Chapter IV, orthogonal collocation was applied to problems involving only one point source. The same resulting collocation equations can be used to multiple source cases, but the calculational procedure is different.

As it was previously discussed, the concentration at the source is considered here as the boundary condition in the x-direction. If the problem involves only one source, the input information required to solve it consists of $C_0(1)$, the concentration at the source, $KS(1)$ and $LS(1)$, the location of the point source in the y and z directions, respectively ($JS(1)$ in this case is equal to zero, i.e., $x=0$), and $XMAX$, $YMAX$, and H , the dimensions in the three directions. The calculation of the solution starts at $TINIT$, the initial time and ends at $ENDS$, the end of the simulation time. Intermediate results are computed at every interval of integration time, $PRMT(3)$,

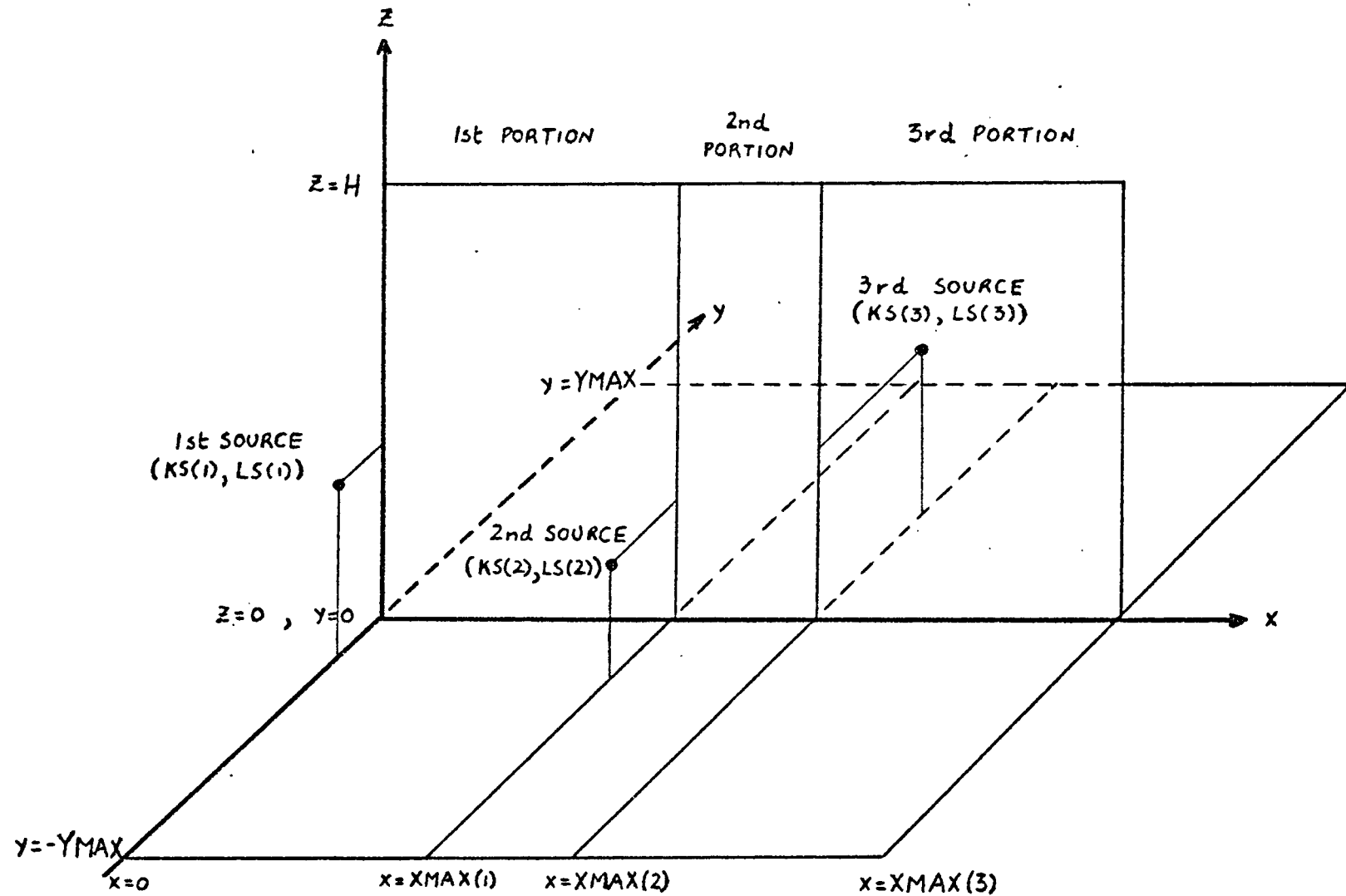
but are printed only every PRDEL units of time. TINIT, ENDS, PRMT(3), and PRDEL are also required as input information.

The calculation procedure for cases involving more than one source is different than the one previously presented. The reason being the interaction that occurs on the concentration distribution due to the multiple sources.

In order to describe the calculation procedure for multiple sources, let us analyze a situation that involves three point sources. In this case, the source concentrations, $C_0(i)$ are still considered as boundary conditions in the x-direction, but while the first source is located at $x=0$, the following ones can be located in general at $x>0$. The entire domain in the x-direction is divided into three portions, so that the first source is located at $x=0$, the second at $XMAX(1)$, and the third at $XMAX(2)$. In order to define completely each source, its position in the y and z directions must be supplied by the values of $KS(i)$ and $LS(i)$, respectively, where i indicates the number of the source. This case then can be represented as it is shown in Figure 5.1.

The input information given by TINIT, ENDS, PRMT(3), PRDEL, NX, NY, NZ, YMAX, and H is the same for each source. The number of sources, NSRCS, must also be supplied as input information, and in the present model

Figure 5.1: Multiple Sources Representation



NSRCS ≤ 3 . If more than three sources are to be considered, changes should be made in the dimension and common statements, initial conditions, and RKGS call statements.

The results for the first portion of Figure 5.1 are the same as if they were computed for a single source problem, but for the next portions this is different. The concentrations in the second portion not only depend on $C_0(2)$, but also on the mass flux that comes from the first portion. The same reasoning applies for subsequent portions.

The calculation procedure then is as follows: at every interval of integration time, the concentration values at any orthogonal point in the y-z plane at $x=XMAX(1)$ are recorded and used, with $C_0(2)$, as boundary conditions for the second portion. The same procedure is also utilized for the following portions. This method can be implemented in the computer program by two ways:

- (1) Integrating the three portions at the same time for every interval of time, printing every PRDEL units of time, and continuing to do this until ENDS is reached. This can be done by integrating first the last portion for one interval of time. The values recorded for the preceding portion at the previous interval of time are used as boundary conditions for the interval of time and the portion in question. After this calculation is over,

the same procedure can be applied for the next portion going backwards, and continuing to do this until the first portion is reached. In this way, the same storage can be used to record the values at $x=XMAX(1)$ and $XMAX(2)$ for every interval of time. Furthermore, once the values are printed, the concentration distribution at $time=0$ are not used any more and that storage can be utilized for the next PRDEL units of time.

(2) Integrating the first portion between TINIT and ENDS and recording all the values, then integrating the next portion i all the way, using the values at $x=XMAX(i-1)$ for every interval of integration time recorded previously, and continuing to do this until the last portion is reached. Then, at every PRDEL units of time the solution for that portion and the ones in the disk can be printed. The simulation stops when ENDS is reached for that last portion. It is evident that this method will require more storage capacity than the previous one.

An analysis made on both methods indicated less computational time for the latter way. Therefore, the second method was put in the system.

It should be pointed out that the position of any source can be located only at orthogonal collocation points. That position, given by KS and LS, must be supplied with point numbers. For example, if $N_z=7$ and

the location of a source is at one half of the z-dimension, LS should be 5 (the total number of collocation points is 9, including $z=0$ and $z=1$).

Continuity

In the present model, the concentration at the source, $C_0(i)$, is used to represent the source, and therefore is a required input information. Unfortunately, the emission rate is, in many cases, the only information that is available. One of the objectives of the present study is to obtain a general model that would also compute the concentration distribution when only the emission rate of the source is given.

There is a need then to develop a calculational procedure which would compute a concentration equivalent to the emission rate. The concept of continuity can be used for this purpose. Moreover, the flux at any x is a valuable piece of information that can be obtained from the results of an air pollution model. Therefore, a general continuity calculation will be obtained and then used for the particular problem of computing $C_0(i)$ from the emission rate $Q(i)$.

The flux across any plane normal to the x axis can be expressed by the following equation:

$$\int_0^H \int_{-Y_{MAX}}^{Y_{MAX}} C \cdot u \, dydz = Q_{x_j} \quad (5.1)$$

where C is the mean concentration at any point in the y - z plane, u its corresponding x -component of the mean wind velocity, and Q_{x_j} the mass rate at $x=x_j$.

If there was no mechanism of removal in a model involving one source, the pollutant would be not created or lost within the region of interest, and at steady state Q_{x_j} would be the same for any value of x , and equal to $Q(1)$. For a multiple source case, Q_{x_j} would be equal to the sum of the constant emission rates for a particular source and its precedings. In such a case, the continuity condition should be included in the model, but since removal is taken into account in the present study, the values of Q_{x_j} will vary along the x direction.

Transforming the spatial coordinates into an interval between 0 and 1, equation (5.1) remains as follows:

$$\int_0^1 \int_0^1 C \cdot u \, (2 \cdot Y_{MAX} \cdot H) \, dydz = Q_{x_j} \quad (5.2)$$

Using the quadrature weights, the double integral can be transformed into a double summation leading to the following collocation equation

$$\sum_{k=1}^{N_y+2} \sum_{\ell=1}^{N_z+2} W^{(2)}(k) W^{(3)}(\ell) C_{jkl} u(\ell) (2 \cdot Y_{MAX} \cdot H) = Q_{x_j} \quad (5.3)$$

$$\text{for } j=2, \dots, N_x+2$$

But from the boundary conditions in the y direction,

$$C_{j1\ell} = C_{jN_y+2\ell} = 0 \quad j=2, \dots, N_x+2 \quad (5.4)$$

$$\ell=1, \dots, N_z+2$$

Finally then, equation (5.3) remains as

$$Q_{x_j} = \sum_{k=2}^{N_y+1} \sum_{\ell=1}^{N_z+2} W^{(2)}(k) W^{(3)}(\ell) C_{jkl} u(\ell) (2 \cdot Y_{MAX} \cdot H) \quad (5.5)$$

$$\text{for } j=2, \dots, N_x+2$$

Equation (5.5) was included in the model (in subroutine OUTP) so that the mass flux can be known at any time and at any position in the x direction. In a case of no removal, these values, if they were equal as it will be shown in the next chapter, serve as a proof of the validity of the model and the numerical technique used.

In the case of using equation (5.5) to calculate the equivalent $C_o(i)$, Q_{x_j} is equated to the constant rate of emission, $Q(i)$, and all the concentrations but the one at the point source are made equal to zero. Equation (5.5) becomes then

$$Q(i) = W^{(2)}(KS(i)) W^{(3)}(LS(i)) C_o(i) u(LS(i)) (2 \cdot YMAX \cdot H) \quad (5.6)$$

for $i=1, \dots, NSRCS$

Therefore, whenever $Q(i)$ is the only information available, the equivalent concentration at the source can be calculated from the following equation:

$$C_o(i) = \frac{Q(i)}{W^{(2)}(KS(i)) W^{(3)}(LS(i)) u(LS(i)) 2 \cdot YMAX \cdot H} \quad (5.7)$$

Chapter VI

PRESENTATION AND ANALYSIS OF RESULTS

The objective of the current study was to demonstrate the suitability of the present method to simulate diffusion in the atmosphere. To do this, experimental cases are simulated with the present model, and the results compared to the corresponding experimental data. Unfortunately, at the present moment there are almost no experimental data available in the literature. This is the reason why only the Project Prairie Grass diffusion data at O'Neill, Nebraska, were considered. Four cases from this Project were simulated and the results compared to the experimental data.

In addition, a parametric study was performed, and the sensitivity of the present model to variations in the atmospheric conditions analyzed. This was done by simulating several hypothetical cases.

Comparison to Experimental Values

The atmospheric diffusion data from Runs #20, #24, #45, and #54 of the Project Prairie Grass data [2, 3, 13] were used as a test of the present method.

Project Prairie Grass was a field program designed to provide experimental data on the diffusion of a tracer gas in the atmosphere. The sulfur dioxide tracer gas was released for ten minutes over a flat prairie at O'Neill, Nebraska. The emission was done at about 50 centimeters above the ground and the gas was sampled along semicircular arcs from 50 meters to 800 meters from the source. Samplers were placed at 1.5m above the ground. In addition, concentration profiles along the vertical were measured from samplers located at nine levels on each of six towers positioned along the 100m arc.

In the experiments, the entire sampling network was put in operation just before the start of the gas release and the operation continued until the tracer was transported beyond the 800m arc. Although the actual measurements were of total exposure for each gas release, the investigators reported average concentrations for a ten minute sampling time. It was estimated that the concentration measurements were accurate to within about 10%.

Several meteorological measurements were taken during the tracer release. Among others, the mean wind velocity at two meters above ground. These values were used in the present model to simulate the mean wind velocity profile.

The source strengths Q , and the mean wind velocities at 2 meters u_1 , for the four cases simulated in the present study were as follows:

Table 6.1 : Source Strengths and Mean Velocities (at 2m)
for Experimental Cases Simulated

Run No.	Q (g/s)	u_1 (m/s)
20	101.2	9.38
24	41.2	5.86
45	100.8	6.02
54	43.4	3.94

In the present model, concentration profiles were simulated using the power law equation for the mean wind velocity as

$$\bar{u} = u_1 \left(\frac{z}{z_1} \right)^{.14} \quad (6.1)$$

where u_1 corresponds to the value given in Table 6.1 for an elevation of $z_1 = 2\text{m}$, and z = elevation in meters.

It can be observed that the source emission rate is the only available information related to the source. Therefore, the equivalent concentration at the source, $C_o(1)$, was calculated using equation (5.7) with the source strength $Q(1)$ given by Table 6.1.

Since no data for the turbulent diffusivities were available, the four cases were simulated assuming $\alpha=1$, i.e., the turbulent diffusivities in the y and z directions were the same; and a stability class 4, i.e., neutral stability. In addition, INVRS was made equal to zero, i.e., no inversion at the maximum elevation; and a first-order reaction with $k = 5.8 \times 10^{-5} \text{ min}^{-1}$ was assumed for all cases.

In addition to the experimental values, the concentration profiles calculated by the present method were also compared to the ones (#45 and #54) obtained by the statistical method developed by Bullin [4].

Simulated vertical profiles at the centerline for Runs #20, #24, and #45, and at 20m from the centerline for Run #54 (no experimental data for the centerline were available) are compared with the limited experimental data available in Figures 6.1 through 6.4. There is good agreement between experimental and simulated vertical profiles except for Run #45, where the concentration values near ground level were much lower than the experimental ones. The reason for this discrepancy is a higher simulated velocity profile, u_s , as compared to the actual one u_a . This difference, especially near ground level, can be observed in Table 6.2.

Table 6.2 : Comparison Between Actual and
Theoretical Values for the Mean
Velocity in Run #45

z (m)	u_a (m/s)	u_s (m/s)
0.25	3.78	4.50
0.5	4.60	4.96
1.0	5.31	5.46
2.0	6.02	6.02
4.0	6.65	6.63
8.0	7.35	7.31
16.0	7.88	8.05

Another reason for the discrepancy in Run #45 can be due to a possible smaller simulated turbulent diffusivity in the z direction. This was checked by simulating the same problem, but with stability class 3, i.e., semi-unstable. The results are also plotted in Figure 6.3, and it can be observed that the concentration values increased and thus the difference between the experimental and theoretical values decreased.

Horizontal concentration profiles for the four cases at 1.5m above ground and at downwind distances of 200m and 400m are shown in Figures 6.5 through 6.8. In general, the agreement between experimental and simulated values is good.

The mass flux (g/s) across y-z planes at any x were also calculated using the results obtained for the concentration. These values are given in Figures 6.1 through (6.8) for all the four cases analyzed. The comparison of these values with the experimental data shows good agreement with an average difference of about 1.39%, and a maximum of 2.67%.

Figure 6.1: Comparison of Vertical Concentration Profile.

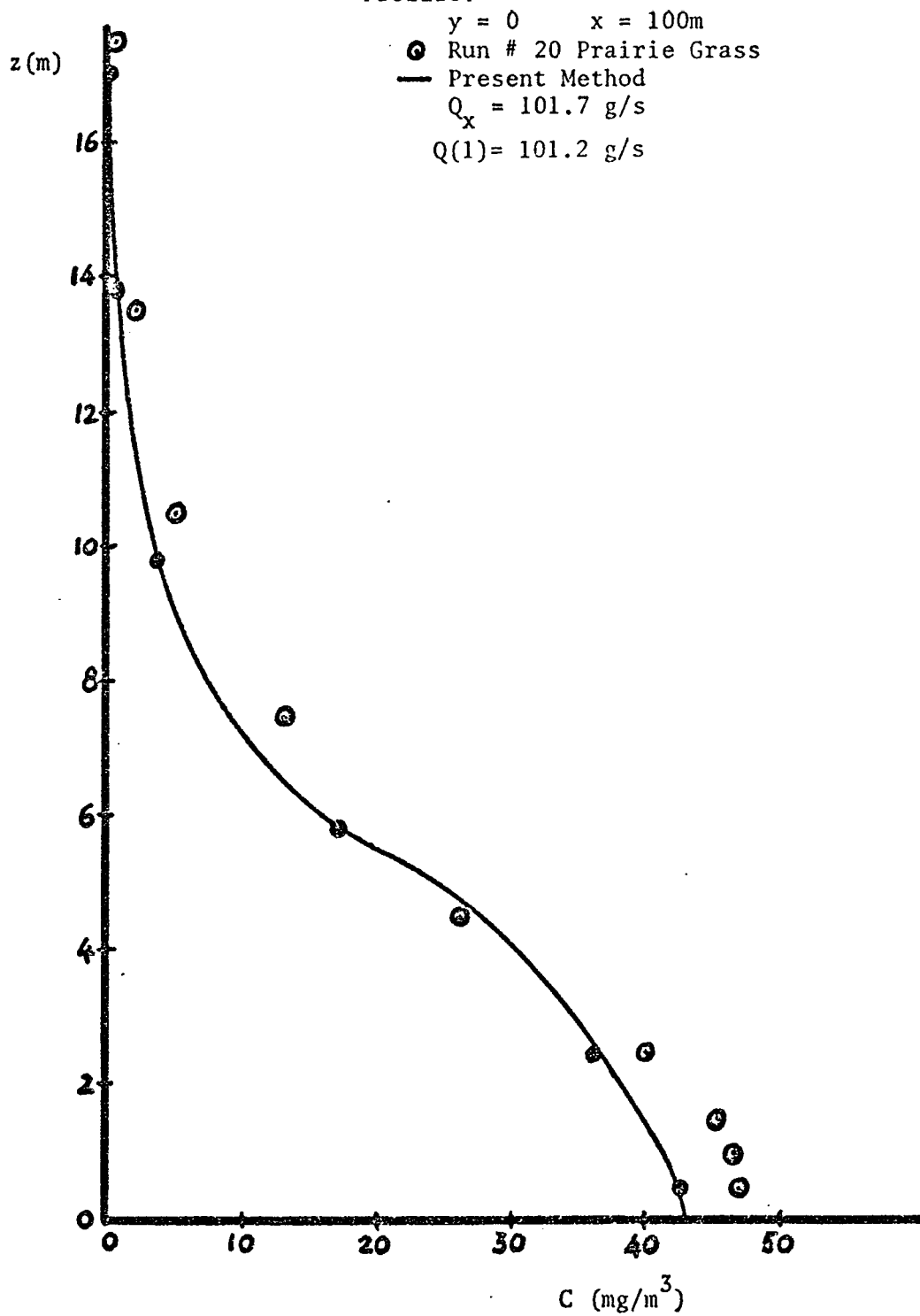


Figure 6.2: Comparison of Vertical
Concentration Profile.

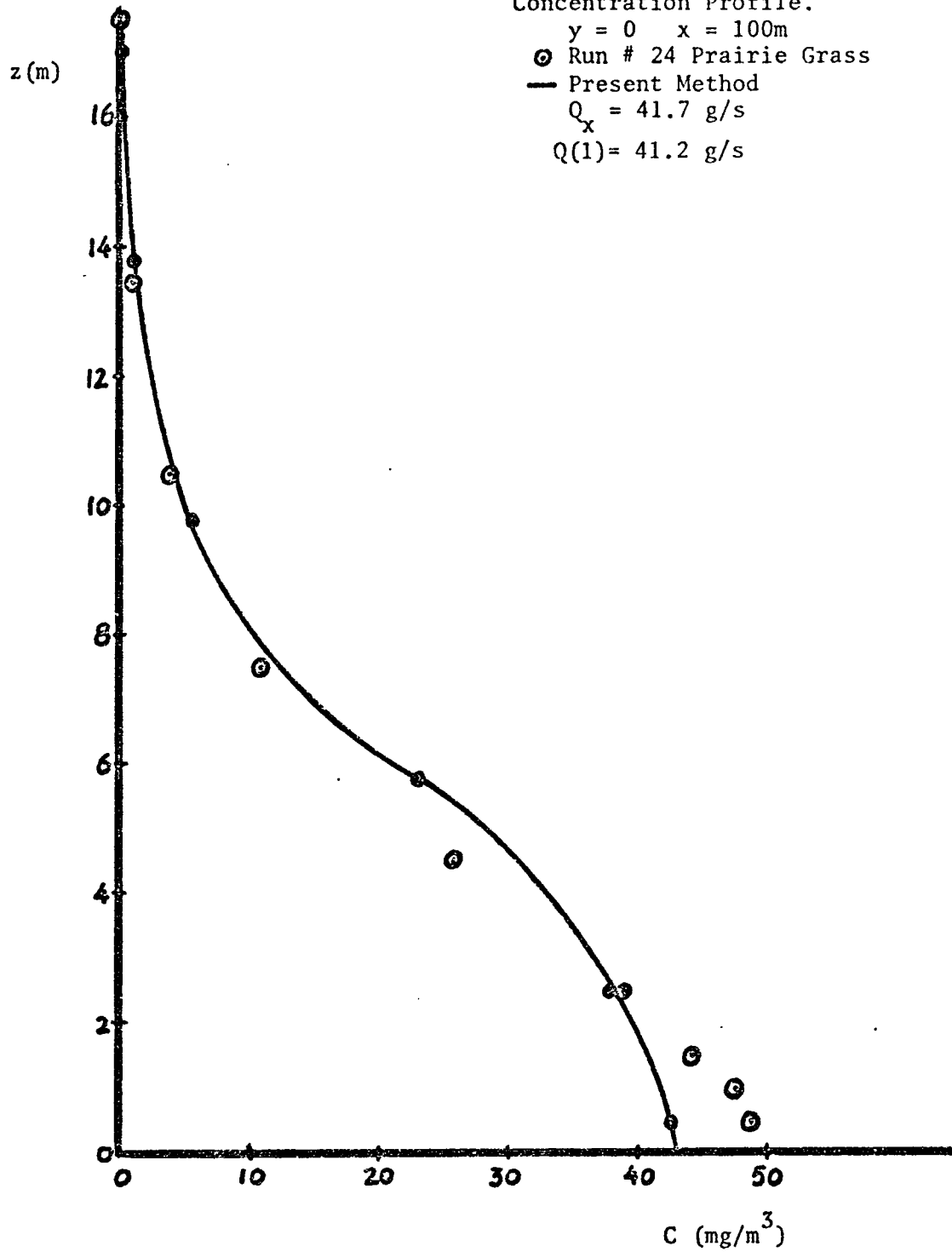


Figure 6.3: Comparison of Vertical
Concentration Profile.

$y = 0 \quad x = 100\text{m}$

● Run # 45 Prairie Grass

--- Bullin' Method

— Present Method

$Q_x = 101.3 \text{ g/s}$

$Q(1) = 100.8 \text{ g/s}$

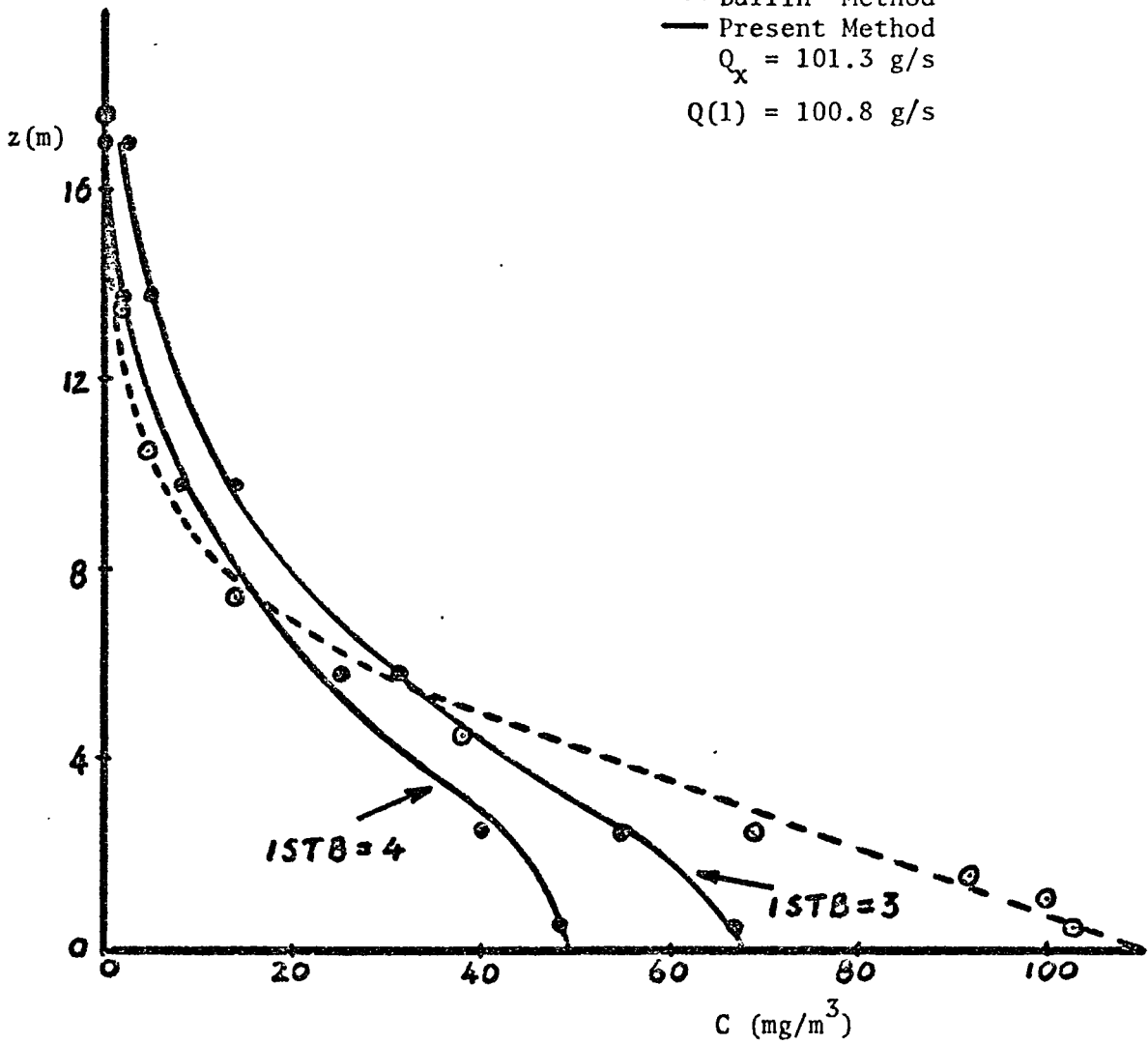


Figure 6.4: Comparison of Vertical
Concentration Profile.

$y = 0 \quad x = 100\text{m}$

● Run # 54 Prairie Grass

--- Bullin' Method

— Present Method

$Q_x = 44.4 \text{ g/s}$

$Q(1) = 43.4 \text{ g/s}$

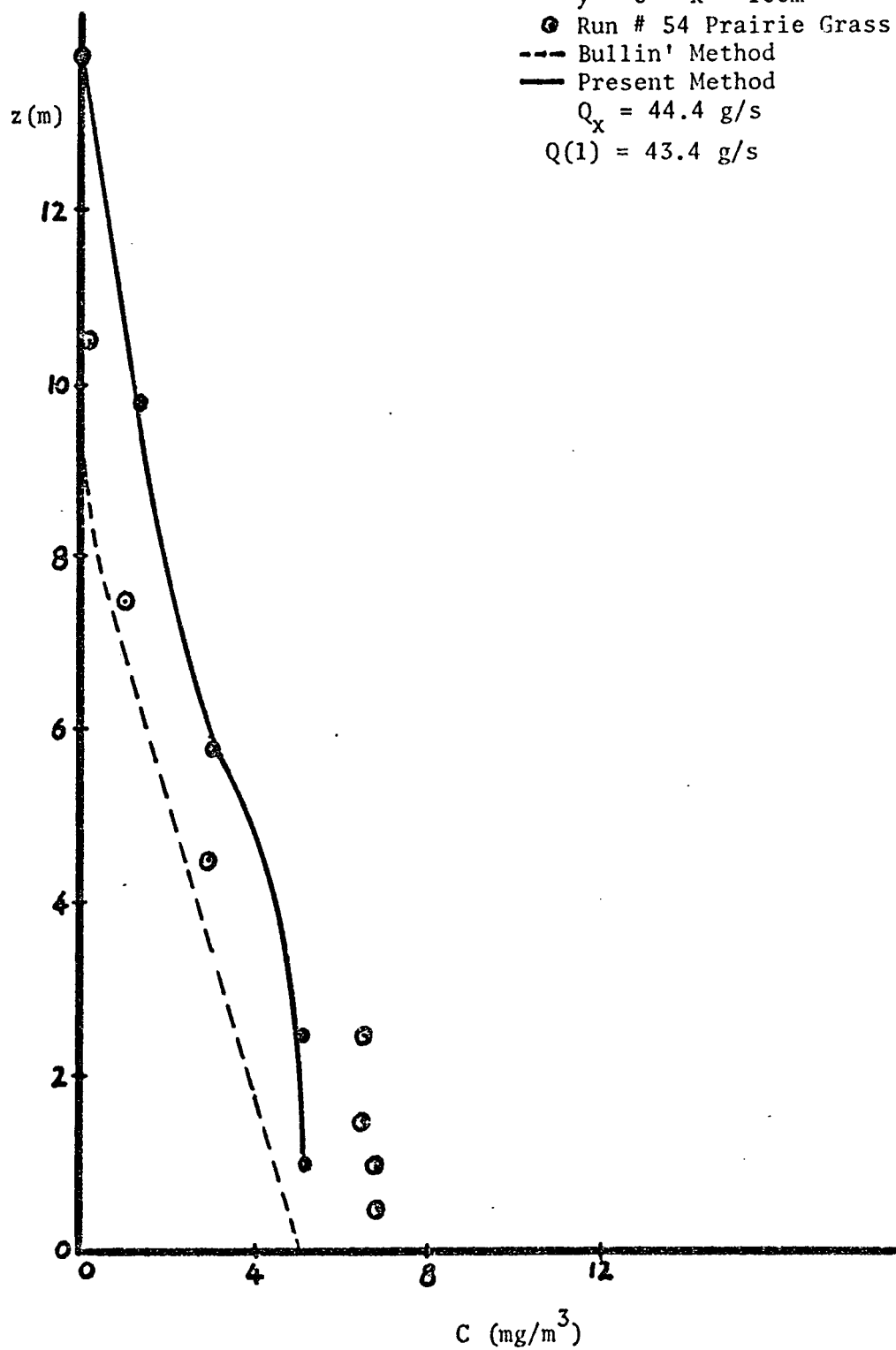


Figure 6.5: Comparison of Horizontal Concentration Profile.

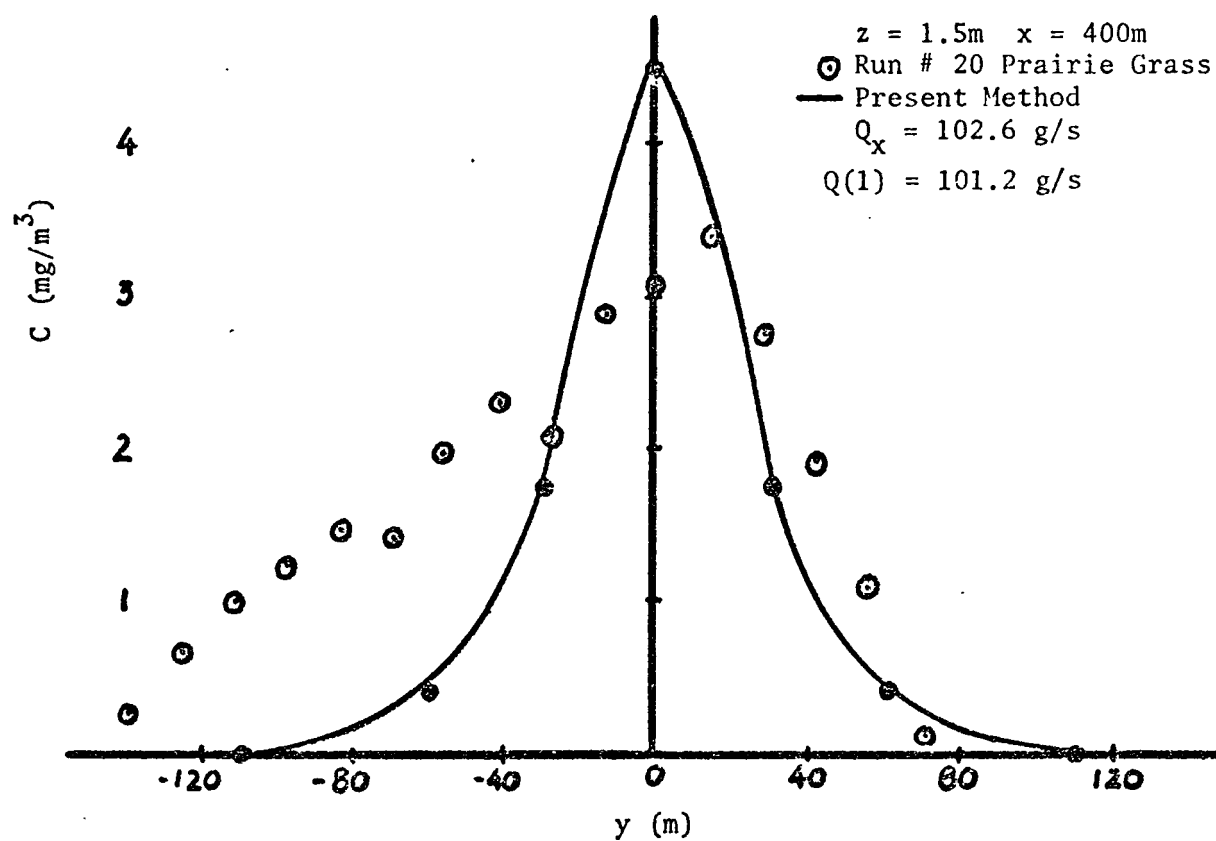
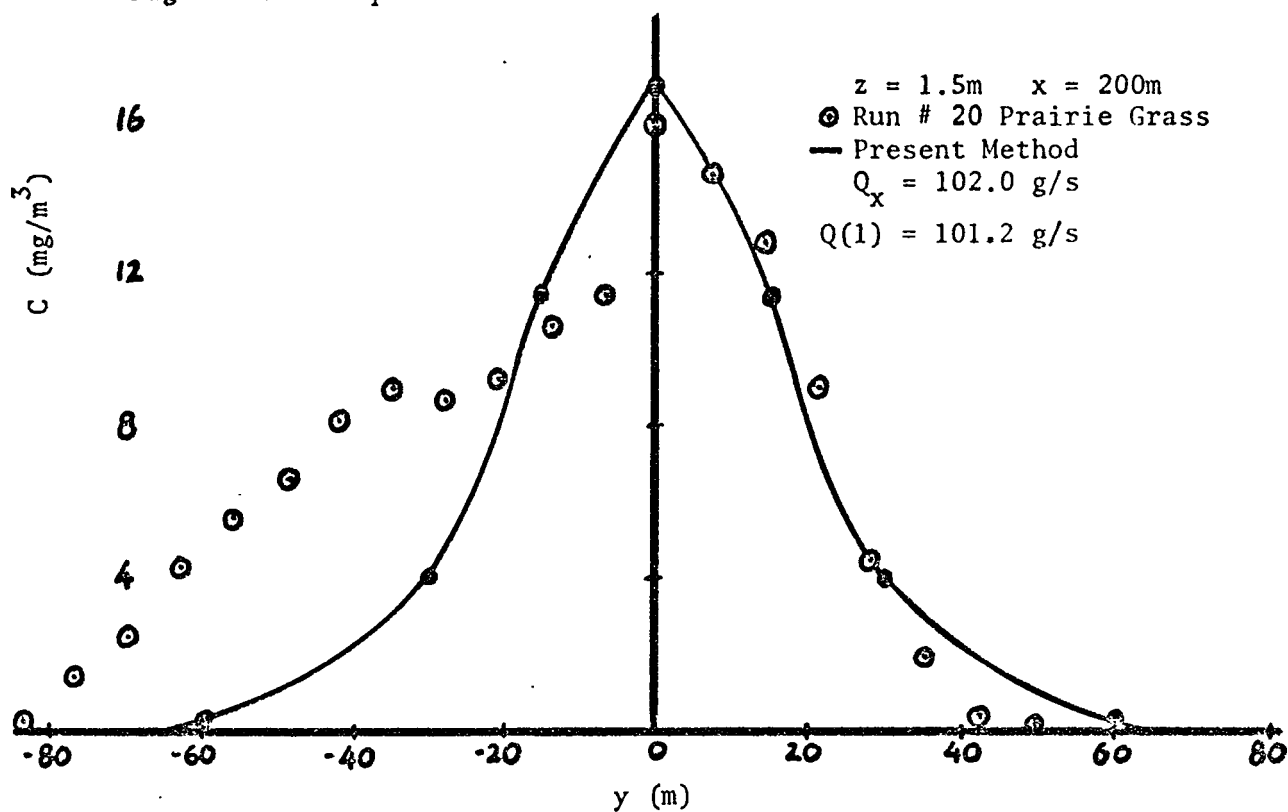


Figure 6.6: Comparison of Horizontal Concentration Profile.

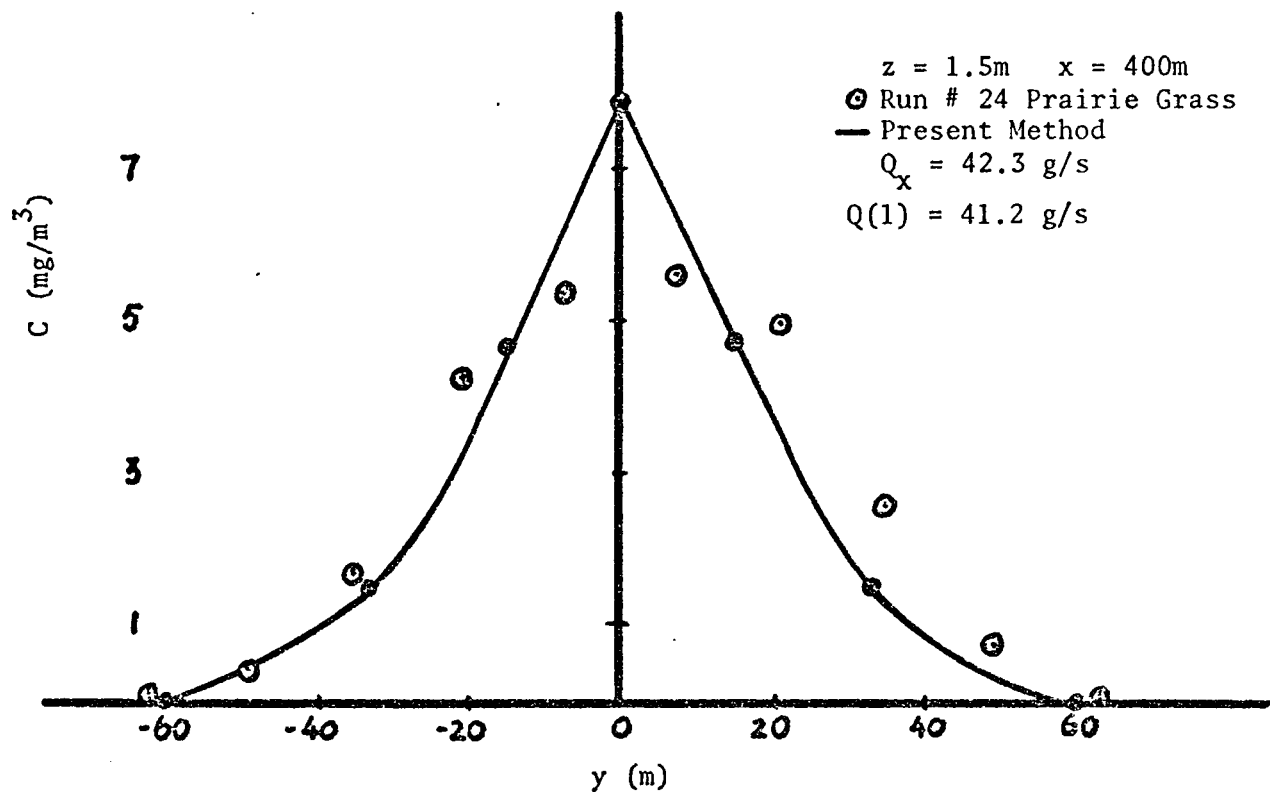
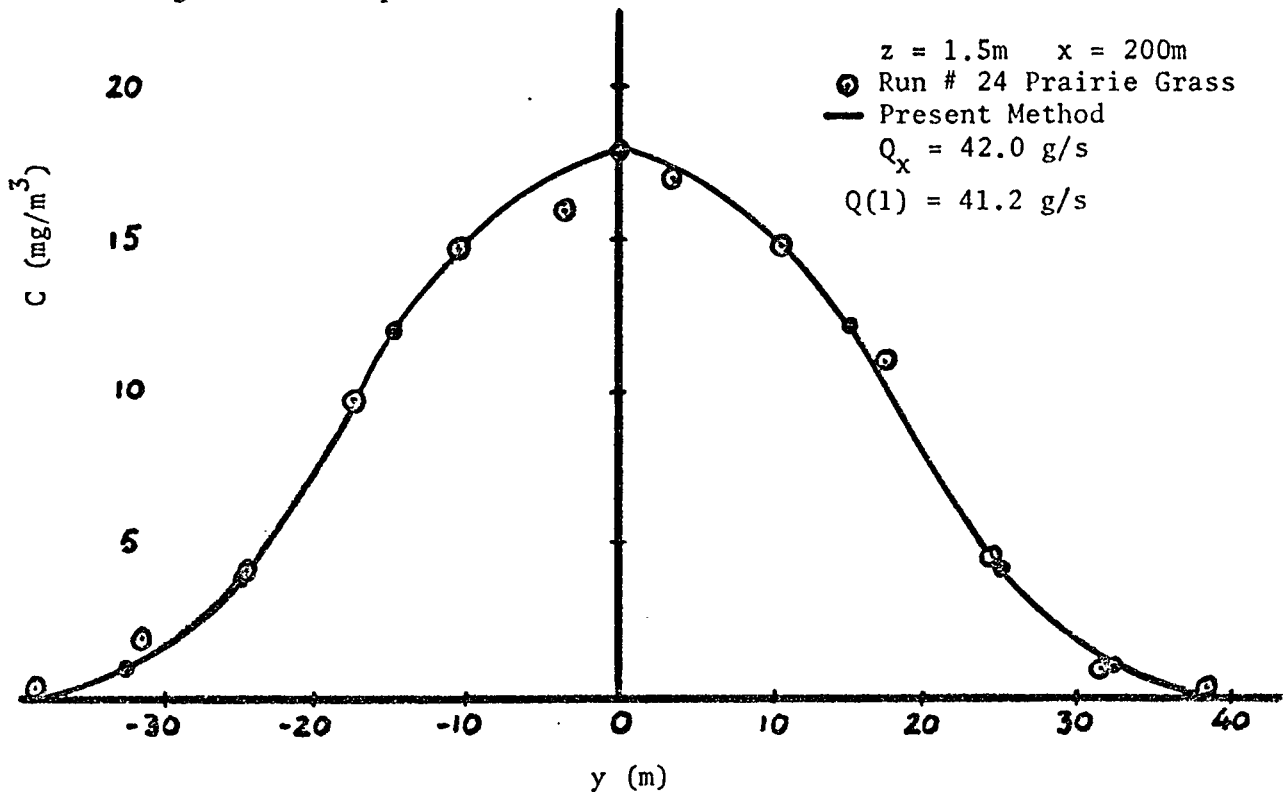


Figure 6.7: Comparison of Horizontal Concentration Profile.

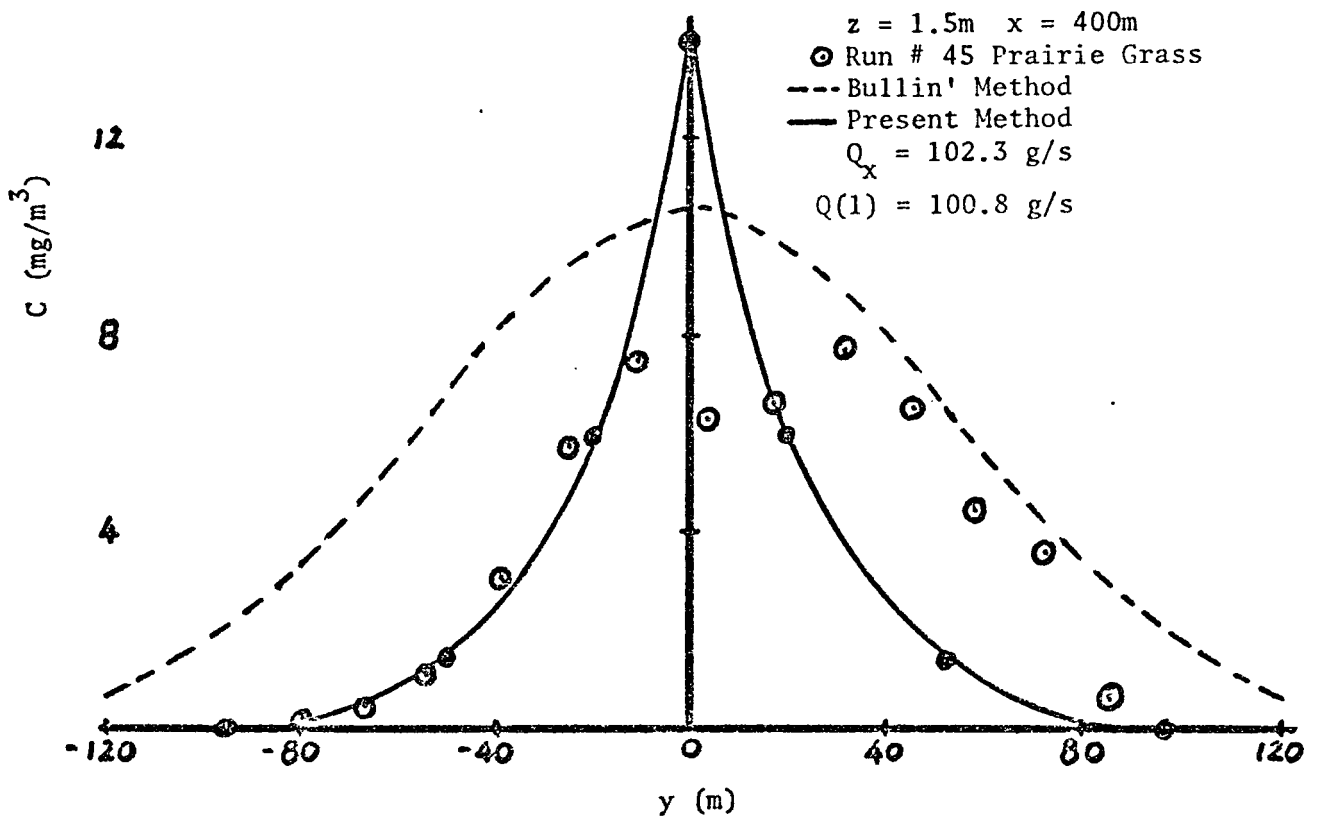
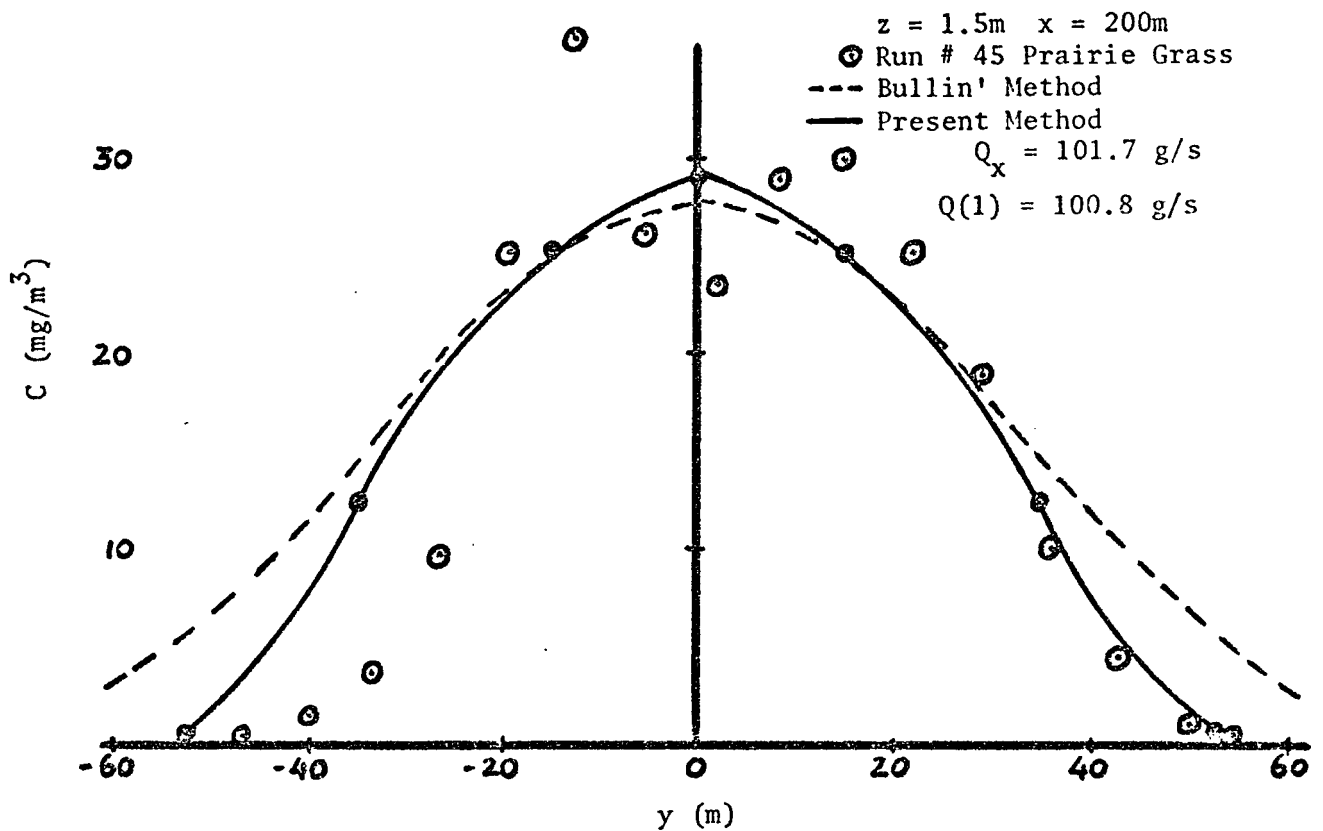
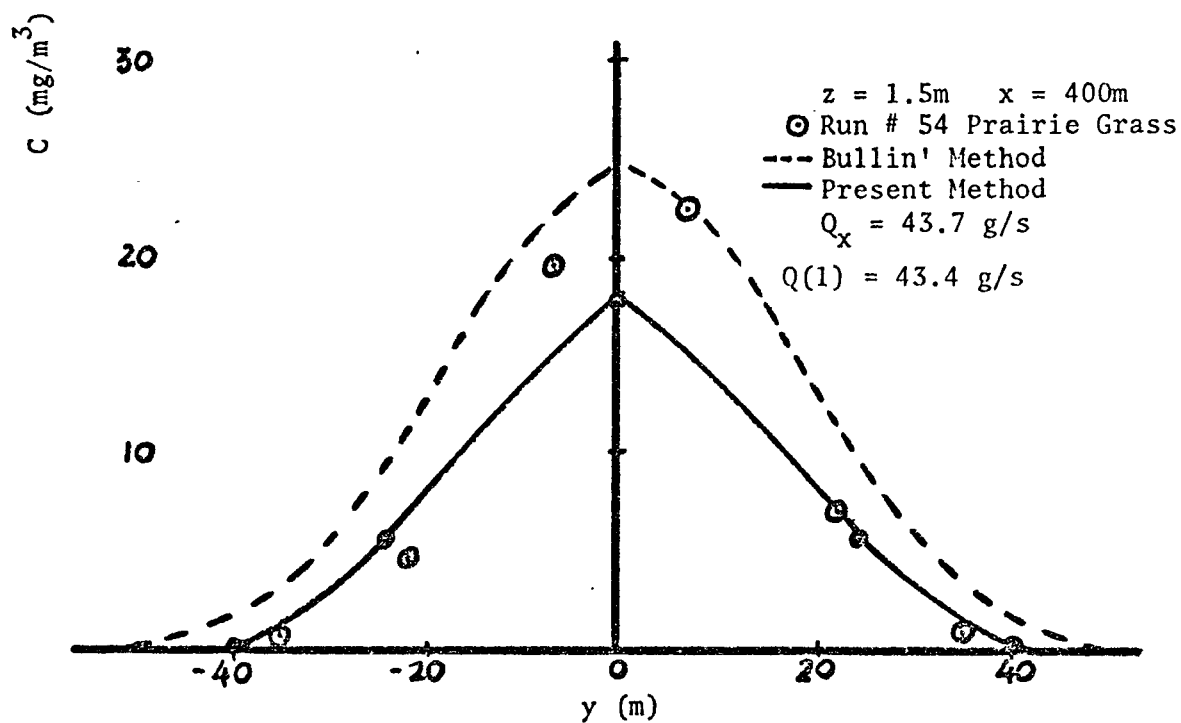
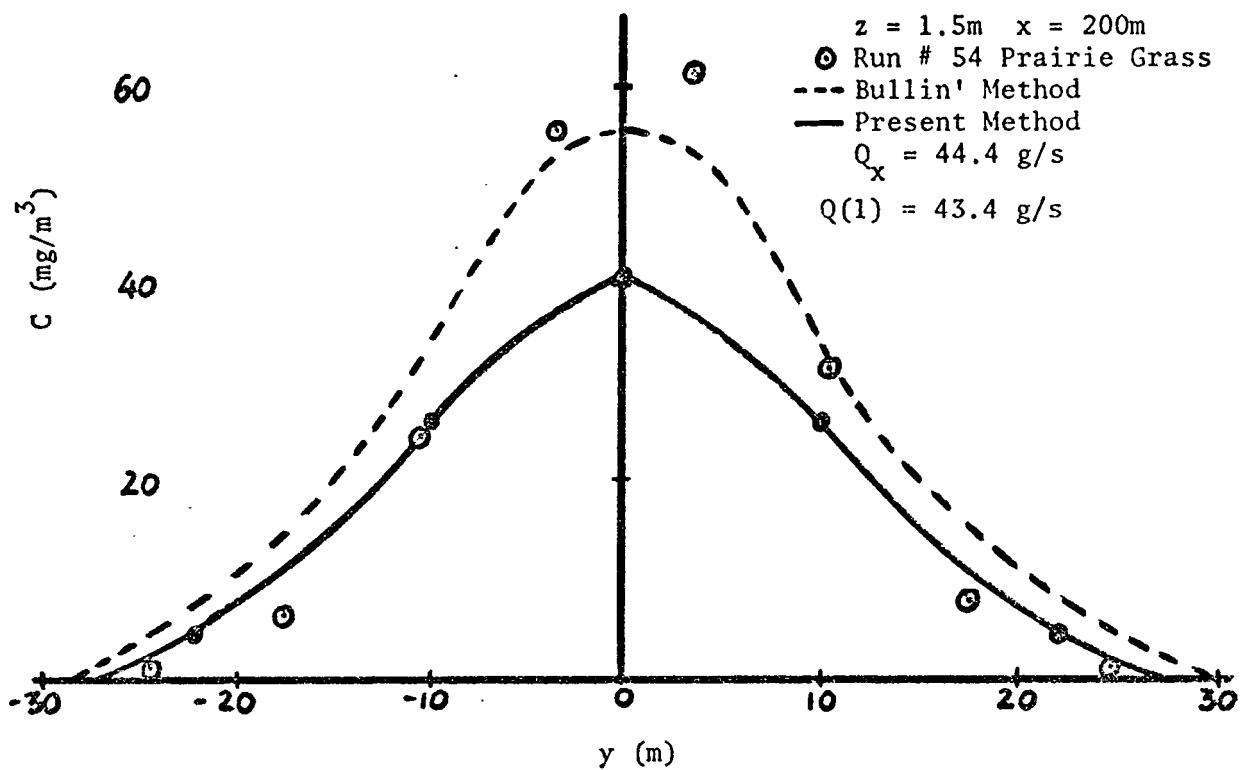


Figure 6.8: Comparison of Horizontal Concentration Profile.



Hypothetical Cases

Concentration profiles were simulated for all the hypothetical cases shown in Table 6.3. Vertical profiles at the centerline ($y=0$) and at several downwind locations for cases 4 through 6 are shown as a function of time in Figures 6.9 through 6.12. As it would be expected, there is a peak in the concentration at the elevation of the effective emission height. The value of this concentration peak increases as the atmospheric stability increases.

The concentration distribution for cases 1 through 7, at the steady state and for different x and y locations are shown in Tables 6.4 and 6.5. These correspond to an elevation of the effective emission height and the ground level, respectively.

Tables 6.6 and 6.7 show case 8, where a velocity in the y direction is included. This case is explained as a function of time so that the development of the plume can be clearly visualized.

This parametric study, i.e., cases 1 through 8, will be analyzed in more detail in the next section.

A multiple source case is shown in Table 6.9, and each source acting individually is shown in Table 6.8. The effect of their interaction can be obtained by comparing both Tables.

Table 6.3 : Hypothetical Cases Simulated

CASE	NO. OF SOURCES	SOURCE ⁽¹⁾ LOCATION (m)	SOURCE STRENGTH (kg/s)	STABILITY CLASS ⁽²⁾	ALPHA	UST (m/s)	RATE OF ⁽³⁾ REACTION (min ⁻¹)	AM	P (%)
1	1	(0,0,150)	5	D	1	5	0	.25	0
2	1	(0,0,150)	5	D	2	5	0	.15	0
3	1	(0,0,150)	5	D	2	5	0	.25	0
4	1	(0,0,150)	5	D	2	5	5.8×10^{-5}	.25	0
5	1	(0,0,150)	5	B	2	5	5.8×10^{-5}	.25	0
6	1	(0,0,150)	5	E	2	5	5.8×10^{-5}	.25	0
7	1	(0,0,252.5)	5	D	2	5	5.8×10^{-5}	.25	0
8	1	(0,0,150)	5	D	2	5	5.8×10^{-5}	.25	5
9	1	(0,-284.1, 252.5)	3	D	2	5	5.8×10^{-5}	.25	0
10	2	(0,0,150)	5	D	2	5	5.8×10^{-5}	.25	0
		(10000,-284.1, 252.5)	3	D	2	5	5.8×10^{-5}	.25	0

(1) The value in the z direction refers to the effective emission height.

(2) Using Pasquill-Gifford definition for stability categories.

(3) Rate of reaction for a first-order reaction.

It should be noted that the concentration distribution due to each source acting individually is at the steady state. This occurs when the time between the start of release and the initiation of the averaging time, θ , is equal to 80 minutes and the end of the averaging time, Ω , is equal to 90 minutes. However, when both sources are put together, the steady state is reached after a longer time.

For all of the cases simulated without reaction, the differences between the mass flux at any x location, at steady state, and the constant source emission rate were not more than 4% of the emission rate. These results show the validity of the model in computing the concentration distribution, and also that the present method can handle continuity calculations.

Figure 6.9: Vertical Concentration Profiles for
Hypothetical Cases 4, 5 and 6.

$\Theta = 0$ min

$\Omega = 10$ min

$y = 0$

..... Stability Class B

--- Stability Class D

— Stability Class E

$x = 1.7$ km

$x = 6.2$ km

$x = 10$ km

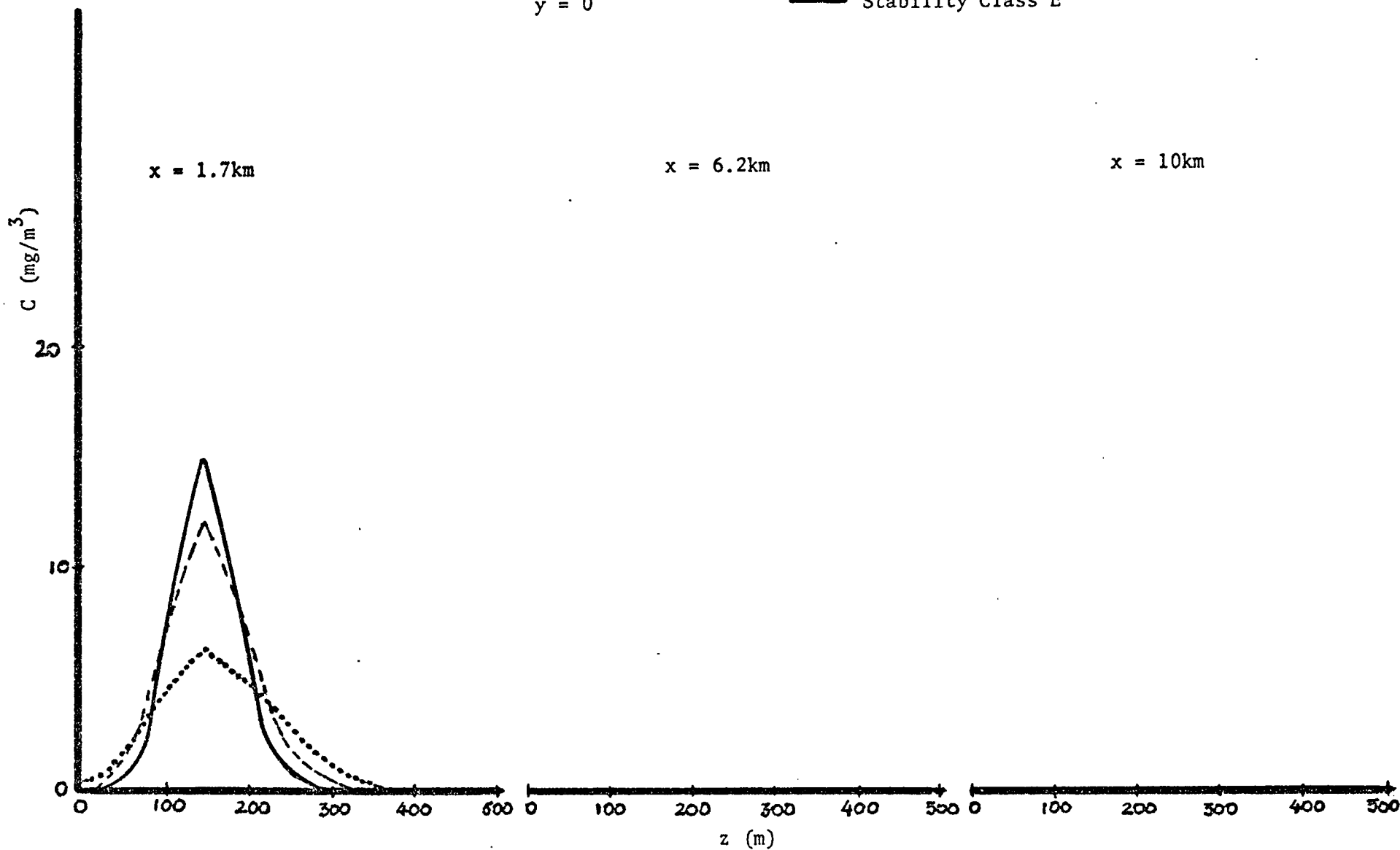


Figure 6.10: Vertical Concentration Profiles for
Hypothetical Cases 4, 5 and 6.

$\Theta = 20$ min

$\Omega = 30$ min

$y = 0$

..... Stability Class B

--- Stability Class D

— Stability Class E

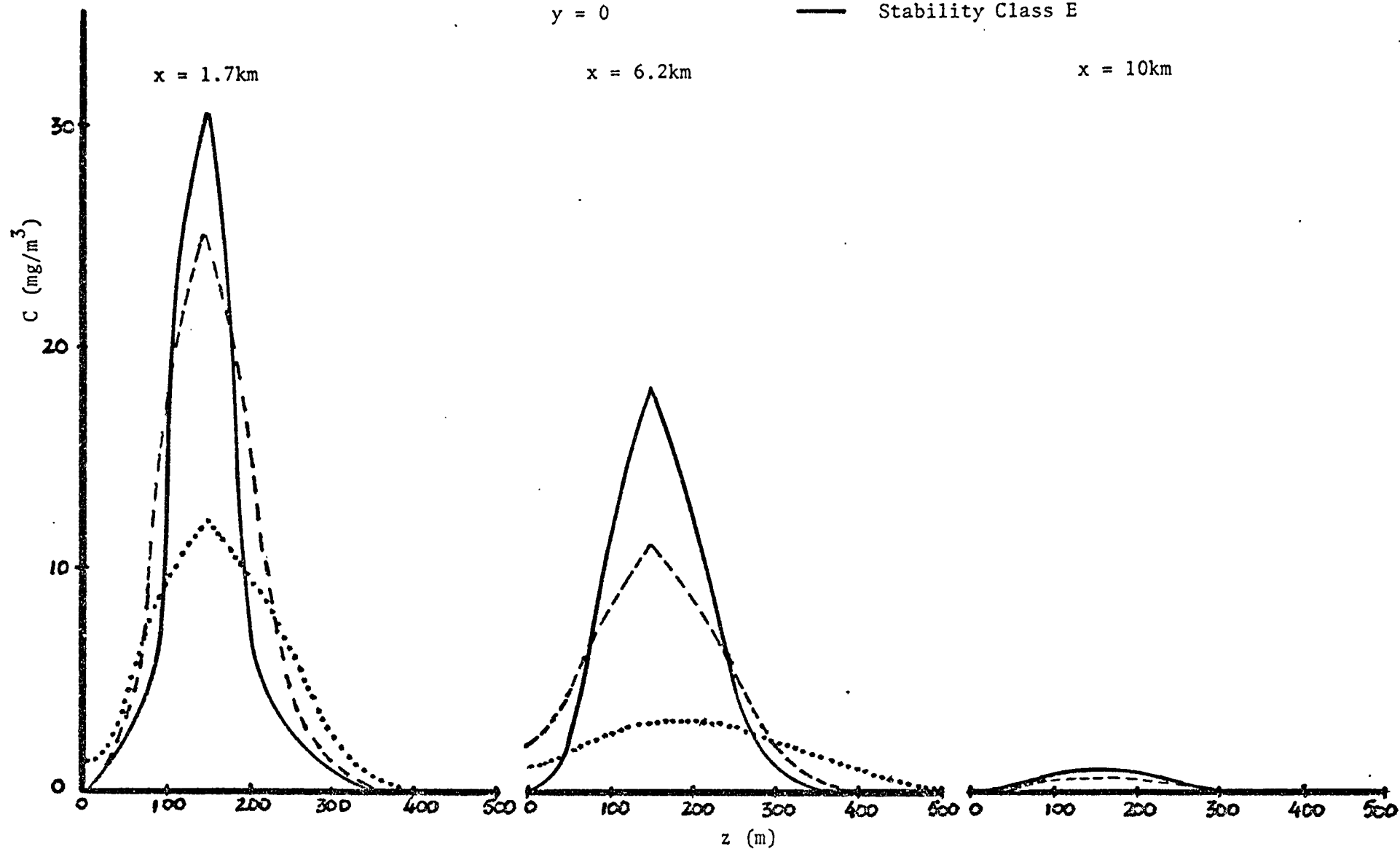


Figure 6.11: Vertical Concentration Profiles for
Hypothetical Cases 4, 5 and 6.

$\Theta = 35$ min

$\Omega = 45$ min

$y = 0$

..... Stability Class B

--- Stability Class D

— Stability Class E

$x = 1.7\text{km}$

$x = 6.2\text{km}$

$x = 10\text{km}$

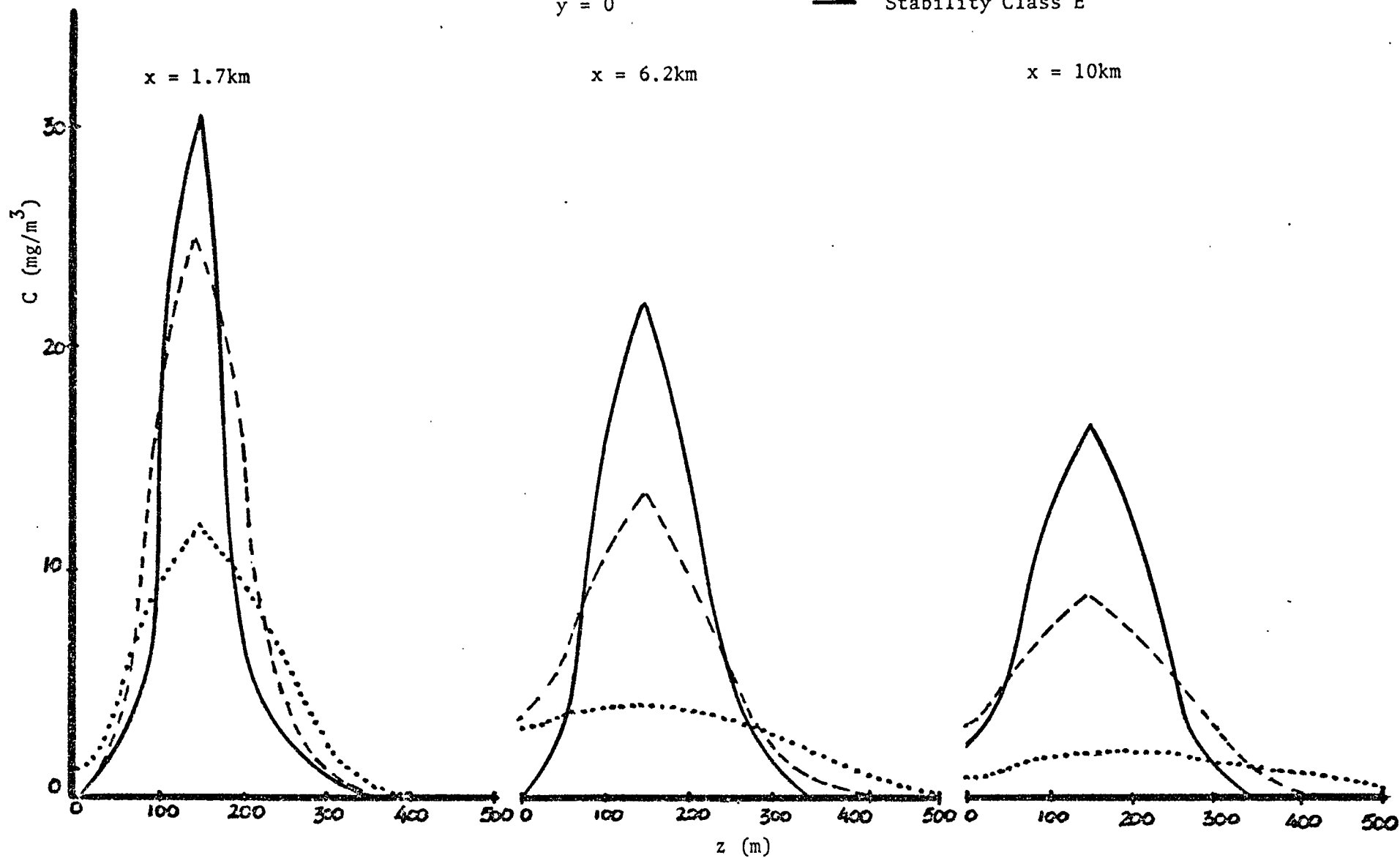


Figure 6.12: Vertical Concentration Profiles for
Hypothetical Cases 4, 5 and 6.

$\Theta = 80 \text{ min}$

$\Omega = 90 \text{ min}$

$y = 0$

..... Stability Class B

--- Stability Class D

— Stability Class E

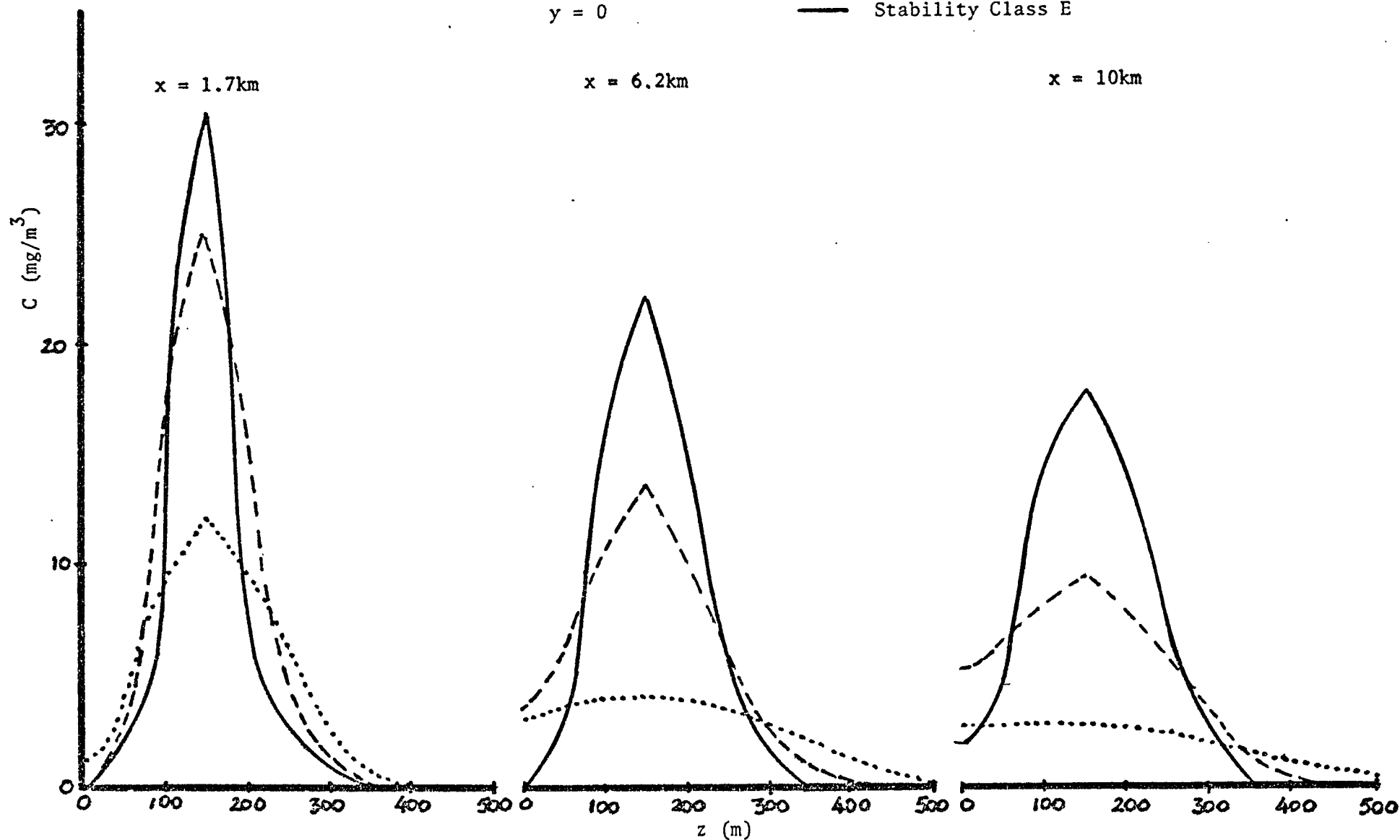


Table 6.4 Concentration Distribution for Hypothetical Cases
1 Through 7 ($\theta = 80$ min, $\Omega = 90$ min)

X DIRECTION (METERS)								
0.0	337.7	1694.0	3806.9	6193.1	8306.0	9662.3	10000.0	
CONCENTRATION (MG/CU.M)								

Z DIRECTION = 150.0 M								
Y=-664.4 M	C.0	0.0	0.0	0.0	0.0	6.0	C.C	C.C
Y=-519.1 M	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0
Y=-284.1 M	0.0	0.16	0.61	1.00	1.24	1.37	1.44	1.45
Y= 0.0 M	35.45	33.11	26.06	19.48	15.15	12.72	11.57	11.32
Y= 284.1 M	C.C	C.16	C.61	1.00	1.24	1.37	1.44	1.45
Y= 519.1 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Y= 664.4 M	C.0	C.0	0.0	0.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.C	C.C	C.C	C.0	0.0	0.0	0.0	0.0
Y=-519.1 M	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0
Y=-284.1 M	C.0	0.31	1.16	1.81	2.12	2.24	2.28	2.28
Y= 0.0 M	35.45	32.88	25.22	18.18	13.63	11.11	9.92	9.67
Y= 284.1 M	C.0	0.31	1.16	1.81	2.12	2.24	2.28	2.28
Y= 519.1 M	0.0	C.C	0.0	C.0	C.C	C.C	C.C	C.C
Y= 664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0
Y=-664.4 M	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0
Y=-519.1 M	0.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-284.1 M	C.C	C.31	1.16	1.81	2.12	2.25	2.29	2.30
Y= 0.0 M	35.45	32.88	25.22	18.19	13.65	11.14	9.96	9.71
Y= 284.1 M	0.0	0.31	1.16	1.81	2.12	2.25	2.29	2.30
Y= 519.1 M	C.0	C.0	C.0	C.0	0.0	0.0	C.C	C.C
Y= 664.4 M	C.0	C.C	C.C	C.0	0.0	0.0	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.0	C.31	1.16	1.81	2.12	2.24	2.29	2.29
Y= 0.0 M	35.45	32.88	25.22	18.18	13.63	11.12	9.94	9.66
Y= 284.1 M	0.0	C.31	1.16	1.81	2.12	2.24	2.29	2.29
Y= 519.1 M	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0
Y= 664.4 M	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.C
Y=-664.4 M	C.C	C.0	0.0	0.0	0.10	0.41	1.34	1.80
Y=-519.1 M	C.C	C.C	C.C	C.0	0.28	0.41	0.33	0.27
Y=-284.1 M	0.0	0.95	2.13	2.11	1.56	1.81	1.78	1.78
Y= 0.0 M	35.45	26.93	12.15	6.44	3.98	3.19	2.72	2.64
Y= 284.1 M	C.C	C.95	2.13	2.11	1.96	1.81	1.78	1.78
Y= 519.1 M	0.0	0.0	C.0	C.0	C.28	C.41	C.33	C.27
Y= 664.4 M	C.0	C.0	0.0	0.0	0.10	0.41	1.34	1.80
Y=-664.4 M	0.0	0.0	0.0	0.0	C.C	C.C	0.0	0.0
Y=-519.1 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-284.1 M	C.0	C.13	0.58	1.08	1.47	1.70	1.82	1.85
Y= 0.0 M	35.45	34.38	30.61	26.02	22.13	19.48	18.06	17.74
Y= 284.1 M	0.0	C.13	0.58	1.08	1.47	1.70	1.82	1.85
Y= 519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y= 664.4 M	C.C	C.C	C.C	C.0	0.0	0.0	0.0	0.0
Y=-664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-519.1 M	C.C	C.C	C.C	C.0	0.0	0.0	0.0	0.0
Y=-284.1 M	0.0	0.01	0.18	C.57	C.95	1.21	1.23	1.36
Y= 0.0 M	C.0	1.08	3.91	5.70	6.14	6.00	5.81	5.76
Y= 284.1 M	C.C	C.C1	C.18	C.57	C.95	1.21	1.23	1.36
Y= 519.1 M	0.0	0.0	C.0	C.0	C.C	0.0	0.0	0.0
Y= 664.4 M	0.0	C.C	C.0	C.0	C.C	C.C	C.C	C.C
Z DIRECTION = 252.5 M								
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=-284.1 M	C.C	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 0.0 M	32.39	30.35	24.00	17.79	13.56	11.13	9.56	9.70
Y= 284.1 M	0.0	C.29	1.11	1.77	2.11	2.24	2.28	2.29
Y= 519.1 M	C.C	C.C	C.C	C.0	C.0	0.0	0.0	C.C
Y= 664.4 M	0.0	0.0	C.0	C.0	C.C	C.C	0.0	C.C
Y=-664.4 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C
Y=-519.1 M	C.0	C.0	0.0	0.0				

Table 6.7 Concentration Distribution for Hypothetical Case #8

X DIRECTION (METERS)									
C.O	237.7	1694.C	3806.9	6193.1	8306.0	9662.3	10000.0		
CONCENTRATION (PG/CU.M)									

Z DIRECTION *	C.O M								
Y=-664.4 M	0.0	0.0	0.0	0.0	C.C	0.0	0.0	0.0	$\Theta = 0 \text{ min}$ $\Omega = 10 \text{ min}$
Y=-519.1 M	C.O	C.C	0.0	C.O	C.C	C.C	C.C	C.C	
Y=-284.1 M	C.C	C.C	0.0	0.0	0.0	0.0	0.0	0.0	
Y= 0.0 M	C.O	C.C	C.O	C.O6	C.O	0.0	0.0	0.0	
Y= 284.1 M	0.0	0.0	0.0	0.01	C.C	C.C	C.C	C.C	
Y= 519.1 M	C.O	0.0	0.0	0.0	0.0	0.0	0.0	C.C	
Y= 664.4 M	C.O	C.C	C.O	C.O	0.0	0.0	0.0	0.0	
Y=-664.4 M	0.0	0.0	0.0	0.0	C.O	0.0	0.0	0.0	$\Theta = 5 \text{ min}$ $\Omega = 15 \text{ min}$
Y=-519.1 M	C.O	C.C	0.0	C.O	C.C	C.C	0.0	C.C	
Y=-284.1 M	C.O	C.C	0.0	0.0	0.0	0.0	0.0	0.0	
Y= 0.0 M	C.O	0.0	0.0	0.27	0.0	0.0	0.0	0.0	
Y= 284.1 M	C.O	0.0	0.0	0.11	C.C	C.C	C.C	C.C	
Y= 519.1 M	C.O	C.O	0.0	0.0	0.0	0.0	0.0	0.0	
Y= 664.4 M	C.O	C.C	C.C	C.O	C.O	0.0	0.0	0.0	
Y=-664.4 M	C.O	0.0	0.0	C.O	C.C	C.C	C.C	C.C	$\Theta = 10 \text{ min}$ $\Omega = 20 \text{ min}$
Y=-519.1 M	C.C	C.C	0.0	0.0	0.0	0.0	0.0	C.C	
Y=-284.1 M	C.C	C.C	C.C	C.O	0.0	0.0	0.0	0.0	
Y= 0.0 M	0.0	0.0	C.O	0.63	C.13	C.C	C.C	C.C	
Y= 284.1 M	0.0	C.C	C.O	0.44	0.16	0.0	C.C	C.C	
Y= 519.1 M	C.C	C.C	C.O	C.O	0.0	0.0	0.0	0.0	
Y= 664.4 M	0.0	0.0	0.0	C.O	C.C	C.O	0.0	C.C	
Y=-664.4 M	C.O	C.O	0.0	0.0	0.0	0.0	C.C	C.C	$\Theta = 20 \text{ min}$ $\Omega = 30 \text{ min}$
Y=-519.1 M	C.O	C.C	C.O	C.O	0.0	0.0	0.0	C.C	
Y=-284.1 M	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C	
Y= 0.0 M	0.0	0.0	0.0	0.96	0.84	0.14	C.C	C.C	
Y= 284.1 M	C.C	C.C4	C.C	1.21	1.84	0.47	0.0	0.0	
Y= 519.1 M	0.0	0.0	0.0	0.06	C.49	0.26	0.01	0.0	
Y= 664.4 M	C.O	C.O	0.0	C.O	C.C	0.01	0.01	C.C1	
Y=-664.4 M	C.O	0.0	0.0	0.0	C.C	C.C	C.C	C.C	$\Theta = 40 \text{ min}$ $\Omega = 50 \text{ min}$
Y=-519.1 M	C.O	C.O	0.0	0.0	0.0	0.0	C.C	C.C	
Y=-284.1 M	C.C	C.C	C.O	C.O	0.0	0.0	0.0	0.0	
Y= 0.0 M	0.0	0.0	0.0	0.80	C.74	C.C	C.C	C.C	
Y= 284.1 M	C.C	C.C	0.0	1.17	3.26	0.0	C.C	C.C	
Y= 519.1 M	C.C	C.C	C.O	C.O2	1.77	0.0	0.0	0.0	
Y= 664.4 M	0.0	0.0	0.0	C.O	C.C	0.0	0.0	C.C	
Y=-664.4 M	0.0	0.0	C.O	C.O	C.C	C.C	C.C	C.C	$\Theta = 80 \text{ min}$ $\Omega = 90 \text{ min}$
Y=-519.1 M	0.0	C.C	C.O	0.0	0.0	0.0	C.C	C.C	
Y=-284.1 M	C.C	C.C	C.C	C.O	C.O	0.0	0.0	0.0	
Y= 0.0 M	0.0	0.0	0.0	0.80	C.73	0.0	0.0	C.C	
Y= 284.1 M	C.O	C.O	0.0	1.18	3.26	C.O	C.C	C.C	
Y= 519.1 M	C.C	C.C	C.C	C.O3	1.76	C.O	0.0	0.0	
Y= 664.4 M	0.0	0.0	0.0	0.0	C.O	0.0	0.0	0.0	

Table 6.8 Concentration Distribution

Case #4 ($\theta = 0$ min)

Case #9

($\Omega = 10$ min)

R DIRECTION (METERS)										R DIRECTION (METERS)									
0.0	337.7	1494.0	3806.9	6193.1	8304.0	9622.3	10000.0	0.0	270.8	1355.2	3045.5	4534.5	4644.8	7725.9	8000.0	0.0	0.0	0.0	0.0
CONCENTRATION (PG/CM ³)										CONCENTRATION (PG/CM ³)									
*****										*****									
Z DIRECTION = 305.0 P																			
Y=464.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=284.1 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 0.0 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 284.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 519.1 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 464.4 P	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 497.1 M																			
Y=464.4 M	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 M	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 0.0 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 284.1 P	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 464.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Z DIRECTION = 439.7 P																			
Y=464.4 P	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 0.0 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 284.1 P	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 464.4 M	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 355.0 P																			
Y=464.4 P	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	1.20	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 0.0 P	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	0.00	0.04	0.03	C.0	C.0	C.0	C.0	C.0
Y= 284.1 P	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	C.0
Y= 464.4 P	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Z DIRECTION = 252.5 P																			
Y=464.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.19	0.54	0.23	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	0.0	0.01	0.08	0.03	C.0	C.0	C.0	C.0	C.0	21.27	12.58	9.36	2.13	C.0	C.0	C.0	C.0	C.0	C.0
Y= 0.0 P	C.0	0.03	1.74	0.33	0.0	0.0	0.0	0.0	0.0	C.0	0.10	0.31	0.14	0.0	0.0	0.0	0.0	C.0	C.0
Y= 284.1 P	C.0	C.0	C.0	C.0	0.03	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 464.4 P	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 150.0 M																			
Y=464.4 P	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	C.0	C.0
Y=519.1 P	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.01	0.02	0.06	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	C.0	C.24	0.52	0.10	C.0	C.0	C.0	C.0	C.0	C.0	0.43	1.19	0.51	C.0	C.0	C.0	C.0	C.0	C.0
Y= 0.0 P	35.45	22.17	12.04	1.15	C.0	C.0	C.0	C.0	C.0	C.0	0.00	0.04	0.03	0.0	0.0	0.0	0.0	C.0	C.0
Y= 284.1 P	C.0	0.24	0.52	0.10	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 464.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Z DIRECTION = 65.3 P																			
Y=464.4 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	C.0	C.02	0.12	0.04	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 0.0 P	C.0	1.34	2.56	0.41	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 284.1 P	0.0	C.02	0.12	0.04	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 464.4 M	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 12.9 P																			
Y=464.4 P	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=284.1 P	C.0	C.0	C.0	C.00	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0
Y= 0.0 P	0.0	0.0	0.0	0.07	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 284.1 P	0.0	C.0	0.0	0.00	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 464.4 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 0.0 P																			
Y=464.4 P	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	0.0	0.0	0.0	C.00	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 0.0 P	C.0	C.0	0.0	0.08	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 284.1 P	C.0	C.0	C.0	C.00	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 464.4 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0

Table 6.8 Continuation

(θ = 10 min)

(Ω = 20 min)

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θ DIRECTICA (PETERS)										θ DIRECTICA (PETERS)									
0.0	337.7	1694.0	3806.9	6193.1	8304.0	9462.3	10000.0	0.0	270.1	1355.2	3045.3	4554.5	6444.8	7725.5	8000.0	0.0	0.0	0.0	0.0
CONCENTRATION (PG/CL.P)										CONCENTRATION (PG/CL.P)									
*****										*****									
Z DIRECTICA = 505.0 M																			
Y=664.4 M	C.0	C.C	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C
Y=519.1 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	0.00	0.00	0.0	0.0	0.0	0.0
Y=284.1 P	C.0	C.0	0.0	0.0	C.C	C.C	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 0.0 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.00	0.00	C.C	C.C	C.C	C.C
Y= 284.1 M	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0
Y= 519.1 P	C.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.0	C.C	0.0	0.0	C.C	C.C	C.C
Y= 664.4 M	C.0	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C
Z DIRECTICA = 492.1 P																			
Y=664.4 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0
Y=519.1 P	C.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	C.C	0.00	C.C	C.C	C.C	C.C
Y=284.1 P	C.0	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.03	0.00	C.C	C.C	C.C	C.C
Y= 0.0 P	C.C	C.C	C.C	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	C.C	0.00	C.C	C.C	C.C	C.C
Y= 284.1 P	0.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.0	C.C	0.0	0.0	0.0	0.0	0.0
Y= 519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.C	C.C	0.0	0.0	C.C	C.C
Z DIRECTICA = 439.7 P																			
Y=664.4 P	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.0	C.C	0.0	0.0	0.0	0.0	0.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=284.1 M	C.C	C.C	C.0	C.0	0.00	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.03	0.03	0.0	C.C	C.C	C.C
Y= 0.0 P	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.0	0.0	0.0	0.0	C.C	0.00	0.0	0.0	0.0	0.0
Y= 284.1 P	0.0	C.0	0.0	0.0	0.00	0.0	0.0	0.0	0.0	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 P	C.C	C.C	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.0	0.0	C.C	C.C	C.C	C.C
Y= 664.4 P	0.0	0.0	C.0	0.0	C.C	0.0	0.0	0.0	0.0	C.0	C.C	C.C	C.0	C.C	0.0	0.0	0.0	0.0	0.0
Z DIRECTICA = 325.0 P																			
Y=664.4 P	C.C	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	0.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 P	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	0.14	0.16	0.28	0.07	0.0	C.C	C.C	C.C
Y=284.1 M	0.0	0.0	0.0	0.0	0.00	0.0	C.C	C.C	C.C	C.0	C.C	2.26	2.87	1.55	0.30	0.0	0.0	0.0	0.0
Y= 0.0 P	C.0	C.C	C.0	0.0	0.02	0.0	0.0	C.C	C.C	0.0	C.C	0.01	0.08	0.22	0.12	C.C	C.C	C.C	C.C
Y= 284.1 P	C.C	C.C	C.0	C.0	0.00	0.0	0.0	0.0	0.0	C.0	C.C	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 519.1 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	C.C	0.0	0.0	0.0	0.0	0.0
Y= 664.4 P	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTICA = 252.5 M																			
Y=664.4 P	C.C	C.C	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C
Y=519.1 M	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	1.01	1.32	C.75	0.15	0.0	0.0	0.0	0.0
Y=284.1 P	C.0	C.C	0.19	0.37	C.13	C.C	C.C	C.C	C.C	21.27	20.01	16.73	10.75	4.08	C.65	C.C	C.C	C.C	C.C
Y= 0.0 P	C.0	1.03	4.00	3.80	C.91	0.0	0.0	0.0	0.0	C.0	C.13	0.56	0.80	0.47	C.10	C.C	C.C	C.C	C.C
Y= 284.1 P	C.0	0.01	0.19	0.37	0.13	0.0	0.0	0.0	0.0	C.C	C.C	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0
Y= 519.1 P	C.0	C.C	C.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	C.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 P	C.0	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	0.0	0.0	C.C	C.C	C.C	C.C
Z DIRECTICA = 150.0 P																			
Y=664.4 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0
Y=519.1 P	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.01	0.13	0.36	C.18	C.07	C.C	C.C	C.C	C.C
Y=284.1 P	C.C	C.10	1.19	1.20	0.31	0.0	0.0	0.0	0.0	C.0	C.55	2.25	2.87	1.55	0.30	C.C	C.C	C.C	C.C
Y= 0.0 P	35.45	32.72	25.44	12.77	2.14	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.18	0.04	C.C	C.C	C.C	C.C
Y= 284.1 P	0.0	0.10	1.19	1.20	C.31	C.C	C.C	C.C	C.C	0.0	0.0	C.0	C.0	C.C	C.0	C.C	C.C	C.C	0.0
Y= 519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	C.C	C.C	C.C	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	0.0	0.0	C.0	0.0	0.0	0.0	0.0	C.C
Z DIRECTICA = 65.3 P																			
Y=664.4 P	C.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	C.0	C.0	C.C	C.0	0.0	0.0	0.0	0.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=284.1 M	C.0	C.C	C.29	C.49	0.15	0.0	0.0	0.0	0.0	C.0	C.C	0.0	0.0	C.04	0.03	0.0	C.C	C.C	C.C
Y= 0.0 P	0.0	1.73	3.99	4.96	1.04	C.C	C.C	C.C	C.C	C.0	0.0	0.0	0.0	C.C	0.00	C.C	C.C	C.C	0.0
Y= 284.1 P	C.C	C.01	0.29	0.49	0.15	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 P	C.C	C.C	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 664.4 M	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	C.0	C.0	C.C	0.0	0.0	0.0	0.0	0.0
Z DIRECTICA = 12.9 P																			
Y=664.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 P	C.C	C.C	C.C	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Y=284.1 P	0.0	0.0	0.0	0.09	0.04	0.0	C.C	C.C	C.C	C.0	C.C	C.0	C.0	C.C	C.C	0.0	0.0	0.0	0.0
Y= 0.0 P	C.0	C.0	C.0	0.90	0.24	0.0	C.C	C.C	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 284.1 M	C.0	C.C	C.0	0.09	0.04	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 519.1 P	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.0	C.0	C.C	0.0	0.0	0.0	0.0	0.0
Y= 664.4 P	C.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTICA = 0.0 M																			
Y=664.4 M	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C
Y=519.1 M	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0
Y=284.1 P	C.0	0.0	0.0	0.06	C.03	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 0.0 P	C.C	C.0	0.0	C.01	0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Y= 284.1 M	C.0	0.0	0.0	0.08	C.03	0.0	0.0	0.0	0.0	C.0	C.C	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0
Y= 519.1 P	C.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.0	C.C	C.0	0.0	0.0	0.0	0.0
Y= 664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.C	C.0	0.0	0.0	0.0	0.0

Table 6.8 Continuation

($\theta = 20$ min)

($\Omega = 30$ min)

[illegible]

Table 6.8 Continuation

 $(\theta = 40 \text{ min})$ $(\Omega = 50 \text{ min})$

B DIRECTION (METERS)										B DIRECTION (METERS)									
C.O	337.7	1494.0	3806.9	4193.1	8306.0	9422.3	10000.C	C.O	270.1	1355.2	3045.5	4954.5	6644.8	7725.9	8000.C	C.O	C.O	C.O	C.O
CONCENTRATION(MG/CL.M)										CONCENTRATION(MG/CL.M)									
*****										*****									
Z DIRECTION = 305.0 P																			
Y=444.4 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Y=519.1 P	C.O	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.O	C.O	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=284.1 P	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	0.0	0.0	0.05	0.06	0.09	0.11	0.11	0.11
Y= 0.0 M	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.O	C.O	C.O	C.O	0.02	0.02	0.02	0.02
Y= 284.1 P	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.O	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 P	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0
Y= 444.4 M	C.O	C.C	C.O	C.O	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.O	C.O	C.O	0.0	0.0	0.0	0.0	0.0
Z DIRECTION = 492.1 P																			
Y=444.4 P	C.O	C.O	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	C.O	0.0	C.O	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 P	C.O	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	0.0	0.0	0.0	0.01	0.02	0.03	0.04	0.04
Y=284.1 P	C.C	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.O	C.O	C.O	C.O	0.02	0.12	0.13	0.13
Y= 0.0 P	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C
Y= 284.1 P	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 519.1 P	C.C	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0
Y= 444.4 P	0.0	0.0	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 435.7 P																			
Y=444.4 P	C.O	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.O	C.O	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y=519.1 P	C.C	C.C	C.O	C.O	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.O	C.O	C.O	C.O	0.11	0.17	0.18	0.18
Y=284.1 P	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.O	0.0	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.O
Y= 0.0 P	C.O	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.01	0.07	C.O	C.O	C.O
Y= 284.1 P	C.C	C.C	C.O	0.0	0.0	0.01	0.01	0.03	0.03	C.O	C.C	C.C	C.O	C.O	0.0	0.0	C.C	C.C	C.C
Y= 519.1 P	0.0	0.0	C.O	C.O	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	0.0	0.0	0.0	0.0
Y= 444.4 P	C.O	C.O	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.O	C.C	0.0	C.C	C.C	C.C	C.C
Z DIRECTION = 355.0 M																			
Y=444.4 M	C.C	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.O	C.O	0.0	0.0	C.C	C.C	C.C
Y=519.1 P	0.0	0.0	0.0	C.O	C.O	0.0	0.0	0.0	0.0	0.0	0.01	0.13	0.42	C.O	C.O	0.93	1.02	1.05	1.05
Y=284.1 P	C.O	C.O	0.0	C.O	C.O	C.O	0.17	0.27	0.25	C.O	C.O	2.20	3.40	3.84	3.85	3.17	3.15	3.15	3.15
Y= 0.0 M	C.C	C.C	0.0	0.0	0.31	0.85	1.16	1.21	1.21	C.C	C.C	C.O	C.O	C.O	0.61	0.68	0.70	0.70	0.70
Y= 284.1 P	C.O	0.0	0.0	C.O	C.O	0.17	0.27	0.29	0.29	0.0	0.0	C.O	C.O	C.C	C.C	0.0	0.0	0.0	0.0
Y= 519.1 P	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.O	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 444.4 M	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	0.0	C.C	C.C	C.C	0.0	0.0	0.0	0.0
Z DIRECTION = 252.5 P																			
Y=444.4 P	0.0	C.O	0.0	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	0.0	0.0	0.0	0.0
Y=519.1 P	C.O	C.O	0.0	C.O	C.C	C.C	C.C	C.C	C.C	0.0	0.26	0.99	1.57	1.87	1.57	1.59	1.55	1.55	1.55
Y=284.1 P	C.C	C.O	0.18	0.57	0.94	1.21	1.36	1.35	1.35	21.27	20.14	16.48	12.63	9.86	8.16	7.32	7.14	7.14	7.14
Y= 0.0 M	C.C	1.00	3.90	5.72	4.10	4.03	5.92	5.86	5.86	C.O	0.14	0.57	C.O	1.18	1.28	1.32	1.33	1.33	1.33
Y= 284.1 P	C.O	C.O	0.18	0.57	C.O	C.O	1.21	1.36	1.35	C.O	0.0	0.0	C.O	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 P	C.C	C.C	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.O	C.O	0.0	0.0	C.O	C.O	C.O	C.O	C.O	C.O
Y= 444.4 P	C.C	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.O	C.C	C.C	0.0	C.C	C.C	C.C
Z DIRECTION = 150.0 P																			
Y=444.4 P	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 P	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	0.13	0.42	0.73	0.31	1.03	1.05	1.05	1.05
Y=284.1 P	C.C	C.O	1.16	1.82	2.10	2.26	2.34	2.34	2.34	C.O	C.O	2.20	3.39	3.84	3.86	3.79	3.77	3.77	3.77
Y= 0.0 P	35.45	32.89	25.20	18.21	13.57	11.18	10.12	9.83	9.83	0.0	C.O	0.08	C.O	C.O	C.O	C.O	C.O	C.O	C.O
Y= 284.1 P	C.O	C.O	1.16	1.82	2.10	2.26	2.34	2.34	2.34	C.O	C.O	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C
Y= 519.1 P	C.C	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.O	C.O	0.0	0.0	0.0	0.0	0.0
Y= 444.4 M	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 45.3 P																			
Y=444.4 P	C.O	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y=519.1 P	C.C	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.O	C.O	0.13	0.20	0.22	0.22	0.22
Y=284.1 P	0.0	0.02	0.27	0.77	1.21	1.57	1.72	1.72	1.72	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.O	C.O	C.O
Y= 0.0 P	C.O	1.81	3.85	7.61	7.67	7.53	7.51	7.51	7.51	0.0	C.O	0.0	0.0	0.0	0.02	C.O	C.O	C.O	C.O
Y= 284.1 P	C.C	C.O	0.27	0.77	1.21	1.57	1.72	1.72	1.72	C.O	C.C	C.C	C.O	C.O	0.0	C.C	C.C	C.C	C.C
Y= 519.1 P	0.0	0.0	0.0	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C
Y= 444.4 P	C.O	0.0	0.0	C.O	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.C	C.C	C.C	C.C
Z DIRECTION = 12.9 M																			
Y=444.4 M	C.O	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.O	C.O	C.O	0.0	0.0	C.C	C.C
Y=519.1 P	0.0	0.0	0.0	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.O	C.O
Y=284.1 P	C.O	C.O	0.0	0.17	0.65	1.12	1.22	1.22	1.22	C.O	C.O	0.0	0.0	0.0	0.05	0.11	C.O	C.O	C.O
Y= 0.0 P	C.O	C.C	C.O	1.60	3.74	4.90	4.78	4.78	4.78	C.O	C.C	C.C	C.O	C.O	0.01	0.02	C.O	C.O	C.O
Y= 284.1 P	0.0	0.0	0.0	0.17	0.65	1.12	1.22	1.22	1.22	0.0	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.O	C.O
Y= 519.1 P	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.C	C.C	C.C
Y= 444.4 M	C.O	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	0.0	0.0	C.O	C.O	0.0	C.C	C.C	C.C
Z DIRECTION = 0.0 P																			
Y=444.4 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	0.0	0.0	0.0	0.0
Y=519.1 P	C.O	C.O	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.O	0.0	0.0	0.0	C.O	C.O	C.O	C.O	C.O	C.O
Y=284.1 P	C.O	C.O	0.0	0.15	0.63	1.10	1.20	1.17	1.17	C.O	C.O	0.0	0.0	C.O	C.O	0.08	0.16	C.O	C.O
Y= 0.0 M	C.O	0.0	0.0	1.46	3.59	4.78	4.84	4.84	4.84	C.O	0.0	0.0	0.0	C.O	C.O	0.02	0.03	0.04	0.04
Y= 284.1 P	C.O	0.0	0.0	0.15	0.63	1.10	1.20	1.17	1.17	0.0	C.O	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 P	C.O	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.O	0.0	0.0	C.O	C.O	C.O	C.O	C.O	C.O
Y= 444.4 M	C.C	C.C	C.O	0.0	0.0	0.0	0.0	0.0	0.0	C.O	C.C	C.C	C.O	C.C	C.C	0.0	C.C	C.C	C.C

Table 6.8 Continuation

(θ = 80 min)

(Ω = 90 min)

X DIRECTION (METERS)								Y DIRECTION (METERS)								
0.0	337.7	1694.0	3606.9	6193.1	8306.0	9662.3	10000.0	0.0	270.1	1255.2	3045.5	4954.5	6644.8	7726.9	8444.0	
GEOMETRICAL (PC/CL/P)								CONCENTRATION (MG/CL/M)								
*****								*****								
Z DIRECTION = 353.0 P																
Y=664.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0
Y=284.1 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.05	0.06	0.10	C.11
Y= 0.0 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	0.02	0.02
Y= 284.1 M	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0
Y= 519.1 M	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0
Y= 664.4 M	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0
Z DIRECTION = 492.1 M																
Y=664.4 P	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0
Y=519.1 P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.01	0.02	C.03	C.04
Y=284.1 P	C.0	C.0	0.0	C.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.07	C.08	0.12	0.13
Y= 0.0 P	C.0	C.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.01	C.01	C.02	C.03
Y= 284.1 M	C.0	0.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 519.1 M	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 439.7 P																
Y=664.4 P	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.02	0.11	0.17	0.18
Y=284.1 P	C.0	C.0	0.0	0.0	0.01	0.02	0.03	0.03	0.0	0.0	0.0	0.0	C.12	C.15	C.13	C.13
Y= 0.0 P	C.0	C.0	C.0	C.0	C.08	0.07	0.11	0.12	0.0	0.0	0.0	0.0	0.01	0.07	C.11	C.12
Y= 284.1 M	0.0	C.0	0.0	C.0	C.01	C.02	C.03	0.03	0.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0
Y= 519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0
Y= 664.4 M	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 355.0 P																
Y=664.4 P	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	0.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	0.01	0.12	C.42	C.73	C.93	C.13	C.15
Y=284.1 P	C.0	C.0	C.0	C.0	0.05	0.17	0.26	0.28	0.0	C.57	2.20	3.41	3.84	3.86	3.79	3.77
Y= 0.0 P	0.0	0.0	0.0	0.0	C.32	C.86	1.12	1.18	C.0	C.0	C.08	C.26	C.46	0.61	0.68	C.70
Y= 284.1 M	C.0	C.0	0.0	0.0	0.05	0.17	0.26	0.28	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0
Y= 664.4 M	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 252.5 P																
Y=664.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.0	C.0	C.0	0.0	0.0	C.0
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	0.0	0.0	C.0	0.0	0.26	C.99	C.0	1.57	1.86	1.97	2.00
Y=284.1 P	0.0	0.01	0.12	0.57	C.95	1.21	1.33	1.36	21.27	20.14	16.48	12.63	9.85	7.75	7.17	7.17
Y= 0.0 P	C.0	1.08	3.71	5.70	6.14	6.00	5.81	5.76	0.0	0.14	0.57	C.95	1.18	1.29	1.33	1.34
Y= 284.1 M	C.0	C.0	C.0	C.0	C.95	1.21	1.33	1.36	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	0.0	0.0	C.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0
Y= 664.4 M	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 150.0 M																
Y=664.4 P	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0
Y=519.1 P	0.0	0.0	C.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	0.11	0.42	0.72	0.93	1.04	1.06
Y=284.1 P	C.0	C.0	1.16	1.81	2.12	2.24	2.29	2.25	C.0	C.0	2.19	3.39	3.84	3.87	3.81	3.79
Y= 0.0 P	35.45	32.68	25.22	18.18	13.63	11.12	9.94	9.69	0.0	C.0	0.08	C.26	C.46	C.61	C.69	C.71
Y= 284.1 M	C.0	C.0	1.16	1.81	2.12	2.24	2.29	2.25	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	C.0
Y= 664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 65.3 P																
Y=664.4 P	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.03	0.13	C.20	C.22
Y=284.1 P	C.0	C.0	0.27	0.76	1.22	1.55	1.72	1.76	0.0	0.0	C.0	C.0	C.0	C.17	C.54	C.73
Y= 0.0 P	C.0	1.08	5.76	7.59	7.72	7.44	7.23	7.17	0.0	C.0	C.0	0.0	0.02	0.09	C.19	C.15
Y= 284.1 M	0.0	0.02	C.27	C.76	1.22	1.55	1.72	1.76	C.0	C.0	C.0	C.0	C.0	0.0	C.0	C.0
Y= 519.1 P	C.0	C.0	0.0	0.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 664.4 M	C.0	C.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0
Z DIRECTION = 12.9 P																
Y=664.4 P	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	C.0	C.0	C.0	C.0	C.17	0.65	1.10	1.35	0.0	C.0	C.0	C.0	C.0	0.05	C.11	C.19
Y= 0.0 P	0.0	0.0	0.0	1.62	3.74	4.84	5.24	5.31	C.0	C.0	C.0	C.0	C.0	C.01	0.02	C.04
Y= 284.1 M	C.0	C.0	0.0	0.17	0.45	1.10	1.73	1.71	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0
Y= 519.1 P	C.0	C.0	C.0	C.0	0.0	0.0	0.0	C.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0
Y= 664.4 M	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0
Z DIRECTION = 0.0 P																
Y=664.4 P	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	0.0	C.0	C.0
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	0.0	0.0	0.0	C.0	C.15	0.63	1.08	1.34	C.0	C.0	C.0	C.0	C.0	C.02	0.08	C.15
Y= 0.0 P	C.0	C.0	0.0	1.48	3.58	4.72	5.14	5.22	C.0	C.0	0.0	C.0	C.0	C.0	C.0	C.0
Y= 284.1 M	C.0	C.0	C.0	C.0	C.15	0.63	1.08	1.34	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 519.1 P	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0	0.0	0.0	0.0	0.0	C.0	C.0
Y= 664.4 M	C.0	C.0	0.0	0.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0

($\Theta = 10 \text{ min}$)

 $(\Omega = 20 \text{ min})$

• DIRECTION (PETERS)

0.0 337.7 1694.0 3806.9 6193.1 8306.0 9662.3 10000.0 10270.1 11355.2 13045.5 14954.5 16644.8 17725.9 18000.0

CONCENTRATION (PG/CU.M)

2 DIRECTION = 5CS.0 P

Y=644.4	P	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Y=-519.1	H	C.C	C.C	C.O	C.O	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C
Y=-284.1	K	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.02	C.C.C	C.C
Y=C.O	F	C.O	C.O	0.0	C.O	C.C	C.O	0.0	0.0	C.C	C.C	C.O	0.0
Y=284.1	M	C.O	C.O	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.0
Y=519.1	H	C.O	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y=644.4	F	0.0	0.0	0.0	0.0	C.C	C.C	C.O	0.0	C.C	0.0	0.0	0.0

Z DIRECTION = 492.1 M

Y=244.4 F	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.0	0.0
Y=517.1 F	C.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C0	C.C0	C.C	C.C
Y=284.1 F	C.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.03	0.C0	0.0	0.0	0.0
Y= 0.0 F	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C0	C.CC	0.C	C.C	C.C
Y= 284.1 F	C.0	C.C	C.0	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C
Y= 519.1 F	0.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	0.0	0.0
Y= 844.4 F	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0

2 DIRECTICK - 439.7 M

Y=-264.4 F	C.0	C.C	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	0.C
Y=-519.1 F	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.C1	0.C1	0.0	0.C
Y=-264.1 F	C.0	C.0	0.0	0.0	0.00	0.0	C.C	C.C	C.C	C.C	C.C3	C.C3	C.0	C.C
Y= 0.0 H	C.0	C.C	C.0	C.0	C.02	0.0	0.0	0.0	0.0	0.0	C.C0	C.CC	C.C	C.C
Y= 284.1 F	0.0	0.0	0.0	0.0	C.CC	C.C	C.C	C.0	0.C	0.C	0.0	C.C	C.C	C.C
Y= 519.1 F	0.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.0	C.C	0.C	0.C
Y= 664.4 F	C.C	C.C	C.0	0.0	0.0	0.0	0.0	0.0	C.0	0.0	C.C	C.C	0.C	0.C

Z DIRECTION = 355.0 °

Y=-664.4 F	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	C.C	
Y=-519.1 F	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C1	C.14	0.36	0.28	C.C7	C.C	C.C
Y=-284.1 F	C.0	C.C	C.0	C.0	0.00	0.0	0.0	0.0	0.35	2.76	2.87	1.55	C.2C	C.C	C.C
Y= 0.0 F	0.0	0.0	0.0	0.0	C.C2	0.0	0.0	C.C	C.C1	G.C8	0.22	0.18	C.C4	C.C	C.C
Y= 284.1 F	0.0	C.0	0.0	0.0	0.00	0.0	0.0	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C
Y= 519.1 F	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 F	0.0	0.0	0.0	0.0	C.C	0.0	0.0	0.0	0.0	0.C	0.C	0.0	C.C	C.C	C.C

4 DIRECTION = 252.5 P

[illegible]

Z DIRECTION = 150.0 N

V=684.4	C.O	C.C	O.O	O.O	O.O	O.O	O.C	O.O	G.G	C.C	C.C	C.C	C.C	O.O
V=519.1	O.O	O.O	O.O	O.O	C.O	O.O	O.O	O.O	O.OI	O.13	O.36	O.28	C.C7	C.C
V=284.1	O.O	CJO	1.19	1.20	C.31	C.C	C.C	C.C	C.55	2.25	2.67	1.55	O.OO	O.O
V=C.C	35.45	32.72	25.44	12.27	2.14	O.O	O.O	O.O	O.C1	C.CC	C.22	C.18	C.C4	C.C
V=284.1	C.O	CJC	1.19	1.20	C.31	O.O	O.O	O.O	O.O	O.O	O.C	C.C	C.C	C.C
V=519.1	C.O	C.O	O.O	C.O	C.C	C.C	C.C	C.C	O.O	O.O	O.O	O.O	O.O	O.O
V=684.4	C.O	C.O	O.O	O.O	O.O	O.O	C.C	O.O	C.C	C.C	C.C	C.C	C.C	C.C

Z CIRCUTIGA 4 65.3 M

Y--664.4 N	C.0	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	0.0
Y--519.1 F	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	0.0
Y--724.1 F	C.0	C.01	0.24	0.49	0.15	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	0.0
Y= 0.0 F	C.0	1.73	5.94	4.96	1.04	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 284.1 F	0.0	0.01	0.24	0.49	0.15	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	C.C
Y= 519.1 F	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	C.C	C.C
Y= 664.4 F	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.0	C.C	C.C	C.0

2 DIRECTIVA • 12.9 F

Y=664.4 F	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	C.C
Y=519.1 F	C.C	C.C	0.0	0.0	0.0	0.0	0.C	C.C	C.C	C.C	0.0	C.C	0.0	0.0
Y=204.1 F	C.C	C.C	C.C	C.C	0.04	0.0	0.0	0.0	0.0	C.C	0.0	C.C	C.C	C.C
Y= 0.0 F	0.0	0.0	0.0	0.0	0.24	0.0	0.0	C.C	0.0	C.C	0.0	C.C	C.C	C.C
Y= 204.1 F	0.0	0.0	0.0	0.04	0.04	0.0	0.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0
Y= 517.1 F	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 F	0.0	0.0	0.0	0.0	C.C	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C

2 DIRECTOR • C.O.P.

[illegible]

$(\theta = 20 \text{ min})$
 $(\Omega = 30 \text{ min})$

X DIRECTION (METERS)

6.0 237.7 1694.6 3806.9 6193.1 8306.0 9662.3 10000.0 10270.1 11355.2 13045.9 14954.5 16644.8 17725.9 18688.0

CONCENTRATION (MG/CM³)

Z DIRECTION = 565.0 M

Y=664.4 M	C.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0
Y=519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C1	C.C1	C.C1
Y=284.1 M	C.0	C.C	C.0	C.0	0.0	0.0	0.00	0.00	0.0	0.0	0.0	C.C5	C.C4	C.C4	C.C4
Y= 0.0 M	0.0	0.0	0.0	0.0	C.C	C.C	C.C0	C.CC	C.C	0.0	0.0	0.0	C.C1	C.C1	C.C1
Y= 284.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.00	0.00	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 M	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C
Y= 664.4 M	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	C.C

Z DIRECTION = 492.1 M

Y=664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	0.0
Y=519.1 M	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C1	C.C1	C.C1	C.C1
Y=284.1 M	0.0	0.0	0.0	0.0	C.C	C.C	C.C0	C.CC	C.C	0.0	0.0	0.07	C.C6	C.C5	C.C5
Y= 0.0 M	C.0	C.0	0.0	0.0	0.0	0.0	0.00	C.CC	C.CC	C.C	C.C	C.C1	C.C1	C.C1	C.C1
Y= 284.1 M	C.0	C.C	C.0	C.0	0.0	0.0	0.00	0.00	0.0	0.0	0.0	C.C	C.C	C.C	C.C
Y= 519.1 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 664.4 M	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	0.0	0.0	0.0	0.0

Z DIRECTION = 439.7 M

Y=664.4 M	C.C	C.C	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y=519.1 M	0.0	0.0	0.0	0.0	C.0	C.C	C.C	C.C	C.C	0.0	0.0	0.02	C.C2	C.C2	C.C7
Y=284.1 M	C.0	C.0	0.0	0.0	0.01	0.00	0.00	0.00	C.C	C.C	C.C	0.12	0.32	0.28	0.26
Y= 0.0 M	C.0	C.C	C.0	C.0	0.07	0.02	0.01	0.01	C.CC	C.C	C.C	C.C1	C.C5	C.C5	C.C5
Y= 284.1 M	0.0	0.0	0.0	C.0	0.01	0.00	0.00	0.00	0.00	0.0	0.0	C.C	C.C	C.C	C.C
Y= 519.1 M	0.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C

Z DIRECTION = 355.0 M

Y=664.4 M	0.0	0.0	0.0	0.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	C.C	C.C
Y=519.1 M	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C1	C.13	C.42	C.72	C.66	0.47
Y=284.1 M	C.0	C.C	C.0	C.0	0.04	0.05	0.02	0.01	0.58	2.15	3.42	3.79	2.17	1.75	1.50
Y= 0.0 M	0.0	0.0	0.0	0.0	0.23	0.26	0.10	0.06	0.02	C.C7	0.26	C.45	C.43	C.31	C.28
Y= 284.1 M	C.0	0.0	0.0	C.0	C.C4	C.C5	C.C2	C.C1	C.CC	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.CC	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	C.C	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C

Z DIRECTION = 252.5 M

Y=664.4 M	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	0.0	0.0	0.0
Y=519.1 M	C.0	C.C	C.0	C.0	0.0	0.0	0.0	0.0	0.0	C.C26	C.58	1.57	1.84	1.41	0.92
Y=284.1 M	0.0	0.02	0.17	0.59	0.76	0.39	0.12	21.34	20.18	16.45	12.68	9.73	5.89	3.43	2.90
Y= 0.0 M	0.0	1.11	3.84	5.85	4.96	2.00	C.55	C.32	C.23	C.54	C.97	1.16	C.93	0.61	0.53
Y= 284.1 M	C.0	C.02	0.17	0.59	0.76	0.39	0.12	0.07	C.C1	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.01	0.0	0.0	0.0	C.C	C.C	C.C
Y= 664.4 M	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0	0.0	0.0

Z DIRECTION = 150.0 M

Y=664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.01	0.13	0.42	0.72	C.67	C.41
Y=284.1 M	C.0	0.32	1.14	1.86	1.71	C.73	C.21	C.12	C.61	2.18	3.41	3.79	2.77	1.76	1.51
Y= 0.0 M	35.45	32.97	25.06	18.50	11.09	3.74	0.94	0.52	C.15	C.C5	C.28	C.44	C.44	C.31	0.28
Y= 284.1 M	C.0	C.32	1.14	1.86	1.71	0.73	0.21	0.12	0.03	0.0	0.0	C.C	C.C	C.C	C.C
Y= 519.1 M	C.0	C.0	0.0	C.0	C.C	C.C	C.C	C.C	C.CC	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	C.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C

Z DIRECTION = 65.3 M

Y=664.4 M	C.0	C.C	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C
Y=519.1 M	0.0	C.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.03	C.C9	C.C8
Y=284.1 M	C.0	C.03	0.25	0.80	0.93	0.41	0.10	0.20	C.C	C.C	C.C	C.C	C.16	C.36	0.30
Y= 0.0 M	C.0	1.14	5.75	7.81	5.96	2.06	0.45	0.20	0.06	0.0	0.00	C.C2	C.C6	C.C5	C.C5
Y= 284.1 M	0.0	0.03	0.25	0.80	0.93	C.41	C.10	C.C5	C.C1	0.0	0.0	0.0	C.C	C.C	C.C
Y= 519.1 M	C.0	C.C	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	C.0	C.C	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C

Z DIRECTION = 12.9 M

Y=664.4 M	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	0.0	0.0	C.C	C.C	C.C
Y=519.1 M	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	0.0	C.C1	C.C1	C.C1
Y=284.1 M	C.C	C.C0	C.0	0.20	0.37	0.13	0.01	0.0	0.0	C.C	C.C	0.0	C.C2	C.C3	C.C4
Y= 0.0 M	0.0	0.0	0.0	1.75	2.23	0.61	0.01	C.C	C.CC	0.0	0.01	C.C0	C.C1	C.C1	C.C1
Y= 284.1 M	C.0	C.C0	0.0	C.20	0.37	0.13	0.01	0.0	C.C	C.C	C.C	0.0	C.C	C.C	0.0
Y= 519.1 M	C.0	C.C	C.0	C.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 M	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C

Z DIRECTION = C.C M

Y=664.4 M	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	0.0	0.0	0.0	0.0
Y=519.1 M	C.C	C.C	C.0	C.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.CC	C.C1	C.C1
Y=284.1 M	0.0	0.01	0.0	0.10	0.35	0.11	0.0	0.0	0.0	0.0	0.0	0.00	C.C1	C.C3	C.C3
Y= 0.0 M	C.0	0.0	0.0	1.41	2.05	C.52	C.C	0.0	C.C	C.C	C.C0	C.C0	C.C0	0.01	0.00
Y= 284.1 M	C.C	C.C1	0.0	0.10	0.35	0.11	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	0.0
Y= 519.1 M	0.0	0.0	0.0	0.0	C.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	C.C	C.C	C.C
Y= 664.4 M	0.0	0.0	0.0	0.0	C.C	C.C	C.C	C.C	C.C	C.C	0.0	0.0	C.C	C.C	0.0

(Θ = 40 min)

(Ω = 50 min)

X DIRECTION (METERS)

C.0 337.7 1694.C 3806.9 6193.1 8306.0 9662.3 100C0.0 10270.1 11355.2 13045.5 14554.5 16444.8 17725.9 18CCC.C

CCENTRATICA (PC/CO.M)

Z DIRECTION = 305.0 P															
Y=664.4 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C1	C.C1	C.C1	C.C3
Y=284.1 P	C.C	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C5	C.C5	C.C5	C.11
Y= 0.0 M	C.0	C.0	C.0	C.0	C.C	C.C	C.C1	C.C1	C.C1	C.C2	C.C2	C.C2	C.C1	C.C2	C.C2
Y= 284.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.CC	C.CC	C.C1	C.C1	C.CC	C.C	C.C	C.C
Y= 519.1 P	C.C	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C0	C.C	C.C	C.C
Y= 664.4 M	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.0	C.C	C.C	C.C	C.C
Z DIRECTION = 452.1 M															
Y=664.4 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 P	C.C	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C1	C.C2	C.C3	C.C4
Y=284.1 P	C.0	C.0	C.0	C.0	C.C	C.C	C.CC	C.CC	C.C	C.0	C.0	C.C7	C.C8	C.12	C.13
Y= 0.0 M	C.0	C.0	C.0	C.0	C.0	C.0	C.C1	C.C2	C.C2	C.C4	C.C4	C.C2	C.C1	C.C2	C.C2
Y= 284.1 M	C.0	C.C	C.0	C.0	C.0	C.0	C.C0	C.CC	C.CC	C.C1	C.01	C.C0	C.C	C.C	C.C
Y= 519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.0	C.0	C.C0	C.C	C.C	C.C
Y= 664.4 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.0	C.C	C.0	C.C
Z DIRECTION = 439.7 M															
Y=664.4 P	C.0	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C
Y=519.1 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.0	C.0	C.11	C.17	C.18
Y=284.1 P	C.0	C.0	C.0	C.0	C.01	C.01	C.C3	C.C3	C.C	C.C	C.C	C.13	C.45	C.62	C.66
Y= 0.0 M	C.0	C.C	C.0	C.0	C.08	C.07	C.11	C.13	C.13	C.14	C.12	C.C7	C.C7	C.11	C.12
Y= 284.1 M	C.0	C.0	C.0	C.0	C.01	C.03	C.03	C.03	C.03	C.C5	C.C4	C.01	C.C	C.C	C.C
Y= 519.1 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C0	C.C	C.C	C.C
Y= 664.4 M	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 355.0 M															
Y=664.4 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.0	C.0	C.C	C.C	C.C
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C1	C.13	C.43	C.73	C.93	C.102	C.105
Y=284.1 P	C.0	C.C	C.0	C.0	C.05	C.17	C.27	C.25	C.C7	C.54	C.66	C.53	C.65	C.76	C.74
Y= 0.0 M	C.0	C.0	C.0	C.0	C.31	C.86	C.16	C.21	C.24	C.33	C.12	C.72	C.61	C.64	C.68
Y= 284.1 P	C.0	C.0	C.0	C.0	C.C5	C.17	C.17	C.25	C.10	C.31	C.19	C.C4	C.C	C.C	C.C
Y= 519.1 M	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.CC	C.C2	C.C3	C.C2	C.C	C.C	C.C
Y= 664.4 M	C.C	C.0	C.0	C.0	C.0	C.0	C.C	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C
Z DIRECTION = 252.5 P															
Y=664.4 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.0	C.0	C.C	C.CC
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.55	C.58	C.58	C.57	C.59
Y=284.1 P	C.0	C.01	C.18	C.57	C.94	C.21	C.36	C.22	C.26	C.26	C.26	C.26	C.26	C.26	C.26
Y= 0.0 M	C.0	C.08	C.39	C.72	C.10	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12
Y= 284.1 P	C.0	C.01	C.18	C.57	C.94	C.21	C.36	C.22	C.26	C.26	C.26	C.26	C.26	C.26	C.26
Y= 519.1 M	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 150.0 P															
Y=664.4 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=519.1 P	C.C	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y=284.1 P	C.0	C.31	C.16	C.82	C.10	C.26	C.34	C.34	C.27	C.27	C.27	C.27	C.27	C.27	C.27
Y= 0.0 M	35.45	32.69	25.20	18.21	11.57	11.18	10.12	9.82	9.44	7.58	4.45	1.47	C.61	C.59	C.54
Y= 284.1 P	C.0	C.31	C.16	C.82	C.10	C.26	C.34	C.34	C.27	C.27	C.27	C.27	C.27	C.27	C.27
Y= 519.1 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.CC	C.C3	C.C5	C.C3	C.C	C.C	C.C
Y= 664.4 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 65.3 M															
Y=664.4 P	C.0	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.CC
Y=519.1 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.20	C.22
Y=284.1 P	C.0	C.C2	C.27	C.77	C.121	C.157	C.172	C.172	C.145	C.91	C.54	C.34	C.33	C.71	C.73
Y= 0.0 M	C.0	C.1	C.85	C.61	C.67	C.53	C.21	C.21	C.68	C.39	C.25	C.24	C.CC	C.C7	C.C5
Y= 284.1 P	C.0	C.02	C.27	C.77	C.121	C.157	C.172	C.172	C.147	C.76	C.16	C.C	C.C	C.C	C.C
Y= 519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.CC	C.C1	C.C1	C.C1	C.0	C.C	C.C
Y= 664.4 M	C.0	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 12.9 P															
Y=664.4 P	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.CC
Y=519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C7
Y=284.1 P	C.0	C.C	C.0	C.17	C.65	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12
Y= 0.0 M	C.0	C.0	C.0	C.10	C.74	C.90	C.78	C.55	C.18	C.18	C.18	C.18	C.18	C.18	C.18
Y= 284.1 P	C.0	C.0	C.0	C.17	C.65	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12	C.12
Y= 519.1 P	C.C	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.CC	C.C1	C.C1	C.C0	C.C	C.C	C.C
Y= 664.4 M	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Z DIRECTION = 0.0 P															
Y=664.4 P	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.CC
Y=519.1 P	C.0	C.C	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C
Y=284.1 P	C.0	C.0	C.0	C.15	C.63	C.10	C.10	C.10	C.10	C.10	C.10	C.10	C.10	C.10	C.10
Y= 0.0 M	C.0	C.0	C.0	C.14	C.74	C.90	C.78	C.55	C.18	C.18	C.18	C.18	C.18	C.18	C.18
Y= 284.1 P	C.0	C.0	C.0	C.15	C.63	C.10	C.10	C.10	C.10	C.10	C.10	C.10	C.10	C.10	C.10
Y= 519.1 P	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0	C.0
Y= 664.4 M	C.0	C.0	C.0	C.0	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C

(θ = 80 min)

(Ω = 90 min)

N DIRECTION (METERS)

E.O. 337.7 1694.C 3006.9 6193.1 8306.0 9662.3 10000.0 10270.1 11355.2 13045.5 14554.5 16444.2 17725.9 18000.C

CONCENTRATION (MG/CU.F)

Z DIRECTION = 365.0 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.O	C.CC	C.O
Y=519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.O	C.C	C.C	C.C	C.C	C.C	C.O
Y=264.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.O
Y= 0.0 F	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.O
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.O
Y= 519.1 F	C.C	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 664.4 F	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C

Z DIRECTION = 452.1 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.CC	C.O
Y=519.1 F	C.C	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.O
Y=264.1 F	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.O	C.C	C.C	C.O
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.O
Y= 264.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.O	C.C	C.C	C.O
Y= 519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.O	C.C	C.C	C.C
Y= 664.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C

Z DIRECTION = 439.7 M

Y=264.4 M	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.CC	C.O
Y=519.1 M	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.O	C.C	C.C	C.O
Y=264.1 M	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.O	C.C	C.C	C.O
Y= 0.0 M	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.O	C.C	C.C	C.O
Y= 264.1 M	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.O	C.C	C.C	C.O
Y= 519.1 M	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.O	C.C	C.C	C.C
Y= 664.4 M	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Z DIRECTION = 355.0 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=264.1 F	C.C	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 F	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Z DIRECTION = 252.5 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 F	C.C	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Z DIRECTION = 150.0 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y=264.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y= 664.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Z DIRECTION = 65.3 F

Y=264.4 F	C.C	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y=519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y=264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 664.4 F	C.C	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Z DIRECTION = 12.9 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C	C.C
Y=519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y=264.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 664.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Z DIRECTION = 0.0 F

Y=264.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O
Y=519.1 F	C.O	C.C	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y=264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 0.0 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 264.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 519.1 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C
Y= 664.4 F	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.O	C.C	C.C	C.C

Sensitivity Analysis

The merit of any model depends on its ability to represent the actual physics and chemistry.

It is evident from the diffusion equation that both the turbulent diffusivities and the velocity profiles have a direct influence on the values calculated by the present model. This is the reason why, as was previously discussed, general expressions are provided for the turbulent diffusivities and the velocity profiles by means of several parameters. In this way, different functional relationships can be easily tested with the present model.

All the parameters given in Table 6.10 must be supplied as input information by the user. Therefore, these parameters can be selected to obtain the best set which will represent the actual conditions of the problem to solve.

The influence of these parameters on the concentration distribution is discussed next. The basis of this analysis is the parametric study on hypothetical cases previously presented.

The influence of AM can be observed from a comparison between cases 2 and 3. As the wind velocity increases, i.e., AM decreases, the values for the mean concentration at a same position decrease. This effect is more evident for the concentration distribution at the ground level.

Table 6.10 : Parameters in Turbulent
Diffusivity and Velocity
Profiles

ISTB	the stability class
ALPHA	the coefficient in the equation for the y-component of the turbulent diffusivity vector
UST	the geostrophic wind speed
AM	the exponent in the power law equation for the velocity profiles
P	the constant that determines the direction of the mean wind velocity
TCH	the parameter that specifies the time required for the y-component of the wind velocity to change from its value at $t=0$ to its maximum value, $P \cdot u$

A comparison between cases 1 and 3 shows the effect of alpha on the concentration distribution. An increase in alpha (Case 3) means an increase in the y-component of the turbulent diffusivity vector, and thus more dispersion occurs in the y-direction. The net effect, as can be observed in Tables 6.4 and 6.5, is that the

concentration at the centerline decreases, and at any y different than zero increases, when compared to the values at same x and z for case 1.

The effect of the chemical reaction on the concentration distribution can be observed from a comparison between cases 3 and 4. The concentration values at any location, x , y , z , in case 4, where a chemical reaction occurs, are smaller than the values in case 3, where the rate of reaction is zero.

A comparison between cases 4, 5, and 6 shows the effect of the atmospheric stability on the concentration distribution. As the atmospheric stability increases, the concentration values at the centerline increase, and the concentration distribution at ground level decreases. It can also be observed that as the instability increases, the pollutant dispersion increases, and the x -position of the maximum ground level concentration moves closer to the source.

Case 7 shows the effect of the stack height on the concentration distribution. It is evident that as the stack height increases, the concentration values at ground level decrease (compare with case 4).

Finally, the effect of the y -component of the wind velocity (case 8) is shown in Tables 6.6 and 6.7. In this case, V was directed in the positive y -direction (from

-YMAX to YMAX), and the net effect is to move the plume more towards that direction.

From this analysis it can be concluded that the present model responds to variations in atmospheric conditions. Furthermore, the results indicate good agreement when compared to an actual response one would expect.

There are two additional parameters that will also influence the results of the present work. Although they do not affect the solution as much as the previous ones, some attention should be devoted to them.

One arises because of the use of RKGS subroutine for solving the system of first-order ordinary differential equations. This parameter is the upper error bound, which must be supplied as input information by the user, and is called PRMT(4) in the computer program.

Neither the truncation errors nor estimates of them are obtained in the calculational procedure performed by "RKGS". Therefore, control of accuracy and adjustment of the step size is done by comparison of the results due to double and single step size calculations.

The procedure is the following: a test value δ (see RKGS [14]), which is an approximate measure for the local truncation error, is compared to the given tolerance PRMT(4). If δ is greater the PRMT(4), the step size or increment of integration of the independent variable is

halved, and the procedure starts again. However, if δ is less than PRMT(4), the results are assumed to be correct.

It can be observed that the larger the value of PRMT(4), the faster the integration is performed. This indicates a decrease in the computing time required, but there is a possibility of obtaining less accurate results.

In order to avoid this inaccuracy on the results, the value of PRMT(4) is usually given small, i.e., in the range of 10^{-3} to 10^{-5} . However, its value and the value for PRMT(3), the initial step size, are actually dependent on the problem to be solved. Unfortunately, there is no general formula to evaluate these parameters. Therefore, for each particular problem, their values have to be studied in order to obtain a fast and accurate solution.

In the present work, this study was performed in the following way: initially, a small value for PRMT(4) was given, i.e., 10^{-5} . Then, this upper error bound was increased and the results for the concentration distribution compared to the previous ones. This procedure was stopped when a change in the second decimal on the concentration values was observed. The corresponding PRMT(4) was then used thereafter, for all the other cases solved.

A similar procedure was performed to obtain the best value for PRMT(3). In this case, several values were

tested and the corresponding computing times compared. It should be pointed out that this parameter affects only the number of bisections done on it, which is also related to the given tolerance PRMT(4).

For the present study, the best values obtained for these two parameters are given in Table 6.11.

Table 6.11 : PRMT(3) and PRMT(4) Values
Used in the Simulations

	Prairie Grass Runs	Hypothetical Cases
PRMT(3)	.05 min	2.5 min
PRMT(4)	.01 min	1.0 min

It can be observed that the values of PRMT(3) and PRMT(4) for the Prairie Grass runs are much smaller than those for the hypothetical cases. The reason being the much smaller dimensions in the three coordinate directions, and thus a smaller step size of integration and smaller upper error bound were needed.

Orthogonal collocation introduces a second parameter that can affect the solution of the model. It is evident that the number of equations increases as the number of

orthogonal points used to obtain the solution is increased. This situation will therefore increase the computer time requirements.

Having this in mind, the present method was developed for a variable number of orthogonal points in the x, y, and z directions. They must be supplied as input information by the user, and can be changed from one simulation to another. However, in the present program there is a restriction to use not more than 15 points in each direction and the product $(N_x+1)*N_y*N_z$ be less than 700. The reason being dimension and common statements presently used in the computer program. Actually, no limit exists except for computer capacities and time requirements to solve the problem.

A similar analysis to the one performed for PRMT(4) was done for the number of orthogonal points needed to obtain accurate results. It was concluded that 5 to 10 points in each direction were enough.

Facilities at U. of H. and Time Requirements

The computer facilities at the University of Houston consist of a UNIVAC 1108 digital computer at the University Computing Center and of an IBM 360 Model 44 digital computer in the Engineering Systems Simulation Laboratory of the Cullen College of Engineering.

The computer time required to simulate atmospheric diffusion by the present method depends on the type of problem to be solved. For all the hypothetical cases simulated, with the exception of cases 5 and 10, the ratio of CPU time to real time was about $1/93$ on the UNIVAC and $1/16$ on the IBM. Case 5 was solved with a ratio of $1/53$ on the UNIVAC and $1/10$ on the IBM, and the two sources case had a ratio of $1/46$ and $1/7$, respectively.

The computer time required to solve each of the Prairie Grass runs was higher than the hypothetical cases. The reason being the small dimensions in the x , y , z directions, and thus a very small diffusion time. This required, as it was previously discussed, a very small step size in the integration of the differential equations and a very small upper error bound. In these cases, the ratio of CPU time to real time was about $1/2$ on the UNIVAC and $3/1$ on the IBM..

Chapter VII

SUMMARY OF RESULTS AND RECOMMENDATIONS

Turbulent diffusion from single or multiple point sources in the atmosphere was successfully simulated using the K-theory and a new numerical technique, orthogonal collocation.

Excellent agreement was observed between simulated and experimental concentration profiles for ground level emission sources. The present model had also an excellent response to variations in atmospheric conditions. This was obtained by simulating hypothetical elevated source cases.

Empirical equations were used to describe the mean wind velocities and the turbulent diffusivities. Several parameters were included in these equations so that many atmospheric conditions can be simulated by the present technique.

The present method has several very significant advantages over other available methods, i.e.,

- 1.) A general 3-dimensional, unsteady state problem can be solved using a simpler numerical technique.

Accurate results can be obtained in very reasonable amount of computer time.

- 2.) The method can handle multiple sources put at any position, depending only on the orthogonal points considered.
- 3.) Several meteorological effects are taken into consideration.
- 4.) Mean velocities and turbulent diffusivities can be functions of all three position coordinates, time, and meteorological conditions.
- 5.) Cases with or without an inversion layer, and with or without generation or deposition at the ground level can be solved.
- 6.) The concentration at the source or the emission rate can be given as input information. The method will also calculate the flux across y-z planes at $x=\text{constant}$.
- 7.) Chemical reactions in the atmosphere can be incorporated.
- 8.) Most of the assumptions involved in the present method are in the input information.

Although the present model gives an improved method for solving atmospheric diffusion problems, it should be extended such that any general case could be solved.

These extensions should include:

- 1.) A better representation of true dispersion processes by means of improving the expressions for turbulent diffusivity and mean wind velocity profiles;
- 2.) The incorporation of more realistic chemical reactions and in general any type of removal processes;
- 3.) The incorporation of other atmospheric effects such as the Coriolis effect;
- 4.) Improvements in orthogonal collocation such as removing the restriction on the position of each point source; and
- 5.) Extension to area and line sources.

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APPENDIX

APPENDIX A
COMPUTER PROGRAM LISTING

The computer program used in the present work is shown next. All statements are written in Fortran IV. This program can be executed in IBM 360 or UNIVAC 1108 digital computers.

```

1: C *****MAIN 10
2: C *****MAIN 20
3: C MODEL FOR ATMOSPHERIC DIFFUSION BY ORTHOGONAL COLLOCATION MAIN 30
4: C *****MAIN 40
5: C MIGUEL T. FLEISCHER MAIN 50
6: C *****MAIN 60
7: C *****MAIN 70
8: C *****MAIN 80
9: C *****MAIN 90
10: C NOMENCLATURE MAIN 100
11: C *****MAIN 110
12: C *****MAIN 120
13: C IINIT,ENDS - INITIAL AND FINAL SIMULATION TIMES MAIN 130
14: C Y - CONCENTRATION (USED FOR PKCS) MAIN 140
15: C CC(I,J,K,L)- CONCENTRATION AT POINT (J,K,L) DUE PRIMARILY TO MAIN 150
16: C ITH. SOURCE (USED FOR OUTPUT) MAIN 160
17: C C(J,K,L) - CONCENTRATION AT POINT (J,K,L) (USED FOR ZERO AND AVG) MAIN 170
18: C NX - NUMBER OF POINTS IN X DIRECTION MAIN 180
19: C NY - NUMBER OF POINTS IN Y DIRECTION MAIN 190
20: C NZ - NUMBER OF POINTS IN Z DIRECTION MAIN 200
21: C XMAX(I) - MAXIMUM DISTANCE FROM THE ITH. SOURCE IN THE X MAIN 210
22: C DIRECTION MAIN 220
23: C YMAX - MAXIMUM DISTANCE IN Y DIRECTION MAIN 230
24: C H - MAXIMUM HEIGHT ABOVE TERRAIN MAIN 240
25: C AKY,AKZ - TURBULENT EDDY DIFFUSIVITIES IN Y AND Z DIRECTIONS MAIN 250
26: C ALPHA - CONSTANT USED TO CALCULATE AKY MAIN 260
27: C U,V,W - COMPONENTS OF MEAN WIND VELOCITY VECTOR MAIN 270
28: C UST,UM - PARAMETERS IN U EXPRESSION MAIN 280
29: C TCH - TIME WHEN V BECOMES 100 % MAIN 290
30: C P - CONSTANT USED TO SPECIFY THE VALUE OF V MAIN 300
31: C UGR - VELOCITY AT GROUND LEVEL MAIN 310
32: C AK - RATE OF REACTION MAIN 320
33: C ISTB - STABILITY CLASS (1 VERY UNSTABLE, 6 VERY STABLE) MAIN 330
34: C INVR - 1 OR 0, IF 1 THERE IS INVERSION AT Z=H; IF 0 THERE IS MAIN 340
35: C NO INVERSION MAIN 350

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36: C      NSRCS      - NUMBER OF SOURCES                      MAIN 350
37: C      KS(I),LS(I)- POSITION OF ITH. SOURCE IN THE Y AND Z DIRECTIONS MAIN 370
38: C      CO(I)      - CONCENTRATION AT ITH. SOURCE          MAIN 380
39: C                                                     MAIN 390
40: C                                                     MAIN 400
41:      EXTERNAL FCT,OUTP                                     MAIN 410
42:      DIMENSION PRMT(5),Y1(700),Y2(700),Y3(700),DERY1(700),DERY2(700), MAIN 420
43:      1DERY3(700),AUX(8,700),FA(15),FB(15),FC(15),ROOT(15),VEC(15), MAIN 430
44:      2X7(15),AKY(15),AKZ(15),DAK7(15),COEFF(4),DKN(4),TDFKN(4) MAIN 440
45:      DEFINE FILE 2(2000,225,U,IIPNT)                      MAIN 450
46:      DEFINE FILE 3(200,225,U,IPOINT)                      MAIN 460
47:      DEFINE FILE 4(200,225,U,IPOINT)                      MAIN 470
48:      COMMON /BLK1/ A1(15,15),A2(15,15),A3(15,15),B1(15,15),B2(15,15), MAIN 480
49:      1B3(15,15),R1(15),R3(15),R5(15),R6(15),R361(15),R362(15),APA1(15), MAIN 490
50:      2R36I(15,15),O(700),U(15),V(15),XXX(3,15),XYY(15),XZ7(15),XMAX(3), MAIN 500
51:      3YMAX,H,AK,TCH,P,KS(3),LS(3),CO(3),NX,NY,NZ,N1,N2,N3,KX,KY,KZ, MAIN 510
52:      4V1(15),W2(15),W3(15),NSRCS,IFLG,MFLG,CC(3,15,15,15),PRDEL,PRMT3, MAIN 520
53:      5INVR5                                               MAIN 530
54: C                                                     MAIN 540
55: C                                                     MAIN 550
56: C READ AND WRITE INPUT DATA                            MAIN 560
57: C                                                     MAIN 570
58: C                                                     MAIN 580
59:      DATA COEFFK/2940.,540.,258.,70./                   MAIN 590
60:      DATA DKN/125.,125.,100.,75./                      MAIN 600
61:      WRITE(6,205)                                          MAIN 610
62:      WRITE(6,206)                                          MAIN 620
63:      READ(5,100) TINIT,ENDS,PRMT(2),PRMT(4)              MAIN 630
64:      WRITE(6,200) TINIT,ENDS,PRMT(3),PRMT(4)             MAIN 640
65:      READ(5,109) NSRCS                                     MAIN 650
66:      WRITE(6,209) NSRCS                                    MAIN 660
67:      READ(5,106) PRDEL                                     MAIN 670
68:      WRITE(6,208) PRDEL                                    MAIN 680
69:      READ(5,101) NX,NY,NZ                                  MAIN 690
70:      WRITE(6,201) NX,NY,NZ                                 MAIN 700
71:      READ(5,102) YMAX,H                                    MAIN 710

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72:	WRITE(6,202) YMAX,H	MAIN 720
73:	DO 85 I=1,NSRCS	MAIN 730
74:	READ(5,104) KS(I),LS(I),CO(I),XMAX(I)	MAIN 740
75:	85 WRITE(6,204) KS(I),LS(I),CO(I),XMAX(I)	MAIN 750
76:	READ(5,105) ISTR,INVRS,ALPHA,AK	MAIN 760
77:	WRITE(6,207) ISTR,INVRS,ALPHA,AK	MAIN 770
78:	READ(5,103) UST,UGR,AM,TCH,P	MAIN 780
79:	WRITE(6,203) UST,UGR,AM,TCH,P	MAIN 790
80:	C	MAIN 800
81:	C	MAIN 810
82:	C INITIAL CONDITIONS	MAIN 820
83:	C	MAIN 830
84:	C	MAIN 840
85:	NDIM=(NX+1)*NY*NZ	MAIN 850
86:	PRMT3=PRINT(3)	MAIN 860
87:	DO 51 I=1,NDIM	MAIN 870
88:	Q(I)=0.	MAIN 880
89:	Y1(I)=0.	MAIN 890
90:	Y2(I)=0.	MAIN 900
91:	51 Y3(I)=0.	MAIN 910
92:	SUM=0.	MAIN 920
93:	KK=NDIM-1	MAIN 930
94:	DO 52 I=1,KK	MAIN 940
95:	DERY1(I)=1./FLOAT(NDIM)	MAIN 950
96:	52 SUM=SUM+DERY1(I)	MAIN 960
97:	DERY1(NDIM)=1.-SUM	MAIN 970
98:	DO 86 I=1,NDIM	MAIN 980
99:	DERY2(I)=DERY1(I)	MAIN 990
100:	86 DERY3(I)=DERY1(I)	MAIN1000
101:	N1=NX+2	MAIN1010
102:	N2=NY+2	MAIN1020
103:	N3=NZ+2	MAIN1030
104:	KX=NX+1	MAIN1040
105:	KY=NY+1	MAIN1050
106:	KZ=NZ+1	MAIN1060
107:	DO 53 I=1,NSPCS	MAIN1070

108:	DO 53 J=1,N1	MAIN1080
109:	DO 53 K=2,KY	MAIN1090
110:	DO 53 L=1,N3	MAIN1100
111:	53 CC(I,J,K,L)=0.	MAIN1110
112:	C	MAIN1120
113:	C	MAIN1130
114:	C CALCULATION OF ORTHOGONAL POINTS, QUADRATURE WEIGHTS, AND	MAIN1140
115:	C MATRICES A AND B	MAIN1150
116:	C	MAIN1160
117:	C	MAIN1170
118:	C X DIRECTION	MAIN1180
119:	C	MAIN1190
120:	C	MAIN1200
121:	CALL JCPI(NX,1,1,0.,0.,FA,FB,FC,ROOT)	MAIN1210
122:	DO 20 I=1,N1	MAIN1220
123:	XXX(1,I)=ROOT(I)*XMAX(1)	MAIN1230
124:	IF(NSRCS.EQ.1) GO TO 20	MAIN1240
125:	XXX(2,I)=ROOT(I)*XMAX(2)+XMAX(1)	MAIN1250
126:	IF(NSRCS.EQ.2) GO TO 20	MAIN1260
127:	XXX(3,I)=ROOT(I)*XMAX(3)+XMAX(2)	MAIN1270
128:	20 CONTINUE	MAIN1280
129:	DO 60 I=1,N1	MAIN1290
130:	CALL DFOPR(NX,1,1,I,1,FA,FB,FC,ROOT,VEC)	MAIN1300
131:	DO 70 K=1,N1	MAIN1310
132:	70 A1(I,K)=VEC(K)	MAIN1320
133:	CALL DFOPR(NX,1,1,I,2,FA,FB,FC,ROOT,VEC)	MAIN1330
134:	DO 80 K=1,N1	MAIN1340
135:	80 B1(I,K)=VEC(K)	MAIN1350
136:	60 CONTINUE	MAIN1360
137:	CALL DFOPR(NX,1,1,I,3,FA,FB,FC,ROOT,W1)	MAIN1370
138:	C	MAIN1380
139:	C	MAIN1390
140:	C Y DIRECTION	MAIN1400
141:	C	MAIN1410
142:	C	MAIN1420
143:	CALL JCPI(NY,1,1,0.,0.,FA,FB,FC,ROOT)	MAIN1430

144:	DO 21 I=1,N2	MAIN1440
145:	21 XYY(I)=ROOT(I)*2.*YMAX-YMAX	MAIN1450
146:	DO 61 I=1,N2	MAIN1460
147:	CALL DFOPR(NY,1,1,I,1,FA,FB,FC,ROOT,VFC)	MAIN1470
148:	DO 71 K=1,N2	MAIN1480
149:	71 A2(I,K)=VEC(K)	MAIN1490
150:	CALL DFOPR(NY,1,1,I,2,FA,FB,FC,ROOT,VFC)	MAIN1500
151:	DO 81 K=1,N2	MAIN1510
152:	81 U2(I,K)=VEC(K)	MAIN1520
153:	61 CONTINUE	MAIN1530
154:	CALL DFOPR(NY,1,1,I,3,FA,FB,FC,ROOT,W2)	MAIN1540
155:	C	MAIN1550
156:	C	MAIN1560
157:	C 7 DIRECTION	MAIN1570
158:	C	MAIN1580
159:	C	MAIN1590
160:	CALL JCPI(NZ,1,1,0.,0.,FA,FB,FC,ROOT)	MAIN1600
161:	DO 92 I=1,N3	MAIN1610
162:	92 XZ(I)=ROOT(I)	MAIN1620
163:	DO 22 I=1,N3	MAIN1630
164:	22 XZZ(I)=ROOT(I)*H	MAIN1640
165:	DO 62 I=1,N3	MAIN1650
166:	CALL DFOPR(NZ,1,1,I,1,FA,FB,FC,ROOT,VEC)	MAIN1660
167:	DO 72 K=1,N3	MAIN1670
168:	72 A3(I,K)=VEC(K)	MAIN1680
169:	CALL DFOPR(NZ,1,1,I,2,FA,FB,FC,ROOT,VFC)	MAIN1690
170:	DO 82 K=1,N3	MAIN1700
171:	82 U3(I,K)=VEC(K)	MAIN1710
172:	62 CONTINUE	MAIN1720
173:	CALL DFOPR(NZ,1,1,I,3,FA,FB,FC,ROOT,V3)	MAIN1730
174:	C	MAIN1740
175:	C	MAIN1750
176:	C CALCULATION OF EXPRESSIONS USED IN MODEL	MAIN1760
177:	C	MAIN1770
178:	C	MAIN1780
179:	IF(ISTD.GE.5) GO TO 10	MAIN1790

180:	U(1)=UGP	MAIN1800
181:	TDFKN(ISTR)=DKN(ISTR)/H	MAIN1810
182:	TDSKN=1.-100./H	MAIN1820
183:	GO 2 L=2,N3	MAIN1830
184:	IF(XZ(L)-TDFKN(ISTR)) 11,12,12	MAIN1840
185:	11 AKZ(L)=COEFK(ISTR)*XZ(L)/TDFKN(ISTR)+60.	MAIN1850
186:	DAKZ(L)=COEFK(ISTR)/DKN(ISTR)	MAIN1860
187:	U(L)=UST*(XZ(L)*H/DKN(ISTR))*AM	MAIN1870
188:	GO TO 16	MAIN1880
189:	12 IF(XZ(L)-TDSKN) 13,13,14	MAIN1890
190:	13 AKZ(L)=COEFK(ISTR)+60.	MAIN1900
191:	DAKZ(L)=0.	MAIN1910
192:	GO TO 15	MAIN1920
193:	14 AKZ(L)=COEFK(ISTR)*H*(1.-XZ(L))/100.+60.	MAIN1930
194:	DAKZ(L)=-COEFK(ISTR)/100.	MAIN1940
195:	15 U(L)=UST	MAIN1950
196:	16 AKY(L)=ALPHA*(COEFK(ISTR)+60.)	MAIN1960
197:	2 CONTINUE	MAIN1970
198:	GO TO 50	MAIN1980
199:	10 IF(ISTR.EQ.6) GO TO 40	MAIN1990
200:	GO 3 L=2,N3	MAIN2000
201:	AKZ(L)=60.	MAIN2010
202:	U(L)=UST	MAIN2020
203:	DAKZ(L)=0.	MAIN2030
204:	3 AKY(L)=ALPHA*AKZ(L)	MAIN2040
205:	GO TO 50	MAIN2050
206:	40 GO 4 L=2,N3	MAIN2060
207:	AKZ(L)=30.	MAIN2070
208:	U(L)=UST	MAIN2080
209:	DAKZ(L)=0.	MAIN2090
210:	4 AKY(L)=ALPHA*AKZ(L)	MAIN2100
211:	50 CONTINUE	MAIN2110
212:	GO 41 L=2,KZ	MAIN2120
213:	R3(L)=DAKZ(L)/H**2	MAIN2130
214:	R5(L)=AKY(L)/(4.*YMAX**2)	MAIN2140
215:	41 R6(L)=AKZ(L)/H**2	MAIN2150

216:	DO 30 L=2,KZ	MAIN2160
217:	R361(L)=R3(L)*A3(L,1)+R6(L)*P3(L,1)	MAIN2170
218:	30 R362(L)=P3(L)*A3(L,N3)+R6(L)*R3(L,N3)	MAIN2180
219:	DEN=A3(N3,1)*A3(1,N3)-A3(1,1)*A3(N3,N3)	MAIN2190
220:	DO 31 I=2,KZ	MAIN2200
221:	31 APA1(I)=(A3(1,1)*A3(N3,I)-A3(N3,1)*A3(1,I))/DEN	MAIN2210
222:	DO 32 L=2,KZ	MAIN2220
223:	DO 32 I=2,KZ	MAIN2230
224:	32 R36I(L,I)=R3(L)*A3(L,I)+R6(L)*P3(L,I)	MAIN2240
225:	C	MAIN2250
226:	C	MAIN2260
227:	C WRITE INITIAL CONDITIONS	MAIN2270
228:	C	MAIN2280
229:	C	MAIN2290
230:	MFLG=1	MAIN2300
231:	IFLG=0	MAIN2310
232:	PRMT(1)=0.	MAIN2320
233:	PRMT(2)=0.	MAIN2330
234:	CALL OUTP(C.,Y1,DERY1,0,NDIM,PRMT)	MAIN2340
235:	C	MAIN2350
236:	C	MAIN2360
237:	C INTEGRATION USING RKCS	MAIN2370
238:	C	MAIN2380
239:	C	MAIN2390
240:	MFLG=2	MAIN2400
241:	PRMT(1)=TINIT	MAIN2410
242:	PRMT(2)=CHDS	MAIN2420
243:	IFLG=1	MAIN2430
244:	CALL RKCS(PRMT,Y1,DERY1,NDIM,IHLF,FCT,OUTP,AUX)	MAIN2440
245:	IF(NSRCS.EQ.1) GO TO 59	MAIN2450
246:	IFLG=2	MAIN2460
247:	CALL RKCS(PRMT,Y2,DERY2,NDIM,IHLF,FCT,OUTP,AUX)	MAIN2470
248:	IF(NSRCS.EQ.2) GO TO 59	MAIN2480
249:	IFLG=3	MAIN2490
250:	CALL RKCS(PRMT,Y3,DERY3,NDIM,IHLF,FCT,OUTP,AUX)	MAIN2500
251:	59 CONTINUE	MAIN2510

```

252: C
253: 100 FORMAT(4F10.5)
254: 101 FORMAT(3I5)
255: 102 FORMAT(2F15.7)
256: 103 FORMAT(5F10.3)
257: 104 FORMAT(2I5,2F15.4)
258: 105 FORMAT(2I2,F10.2,L12.3)
259: 106 FORMAT(F10.4)
260: 109 FORMAT(I3)
261: 200 FORMAT(5X,'TINIT =',F5.1,5X,'ENDS =',F6.1,' MIN',5X,'PRMT(3) =',
262: 1F6.2,' MIN',5X,'PRMT(4) =',F8.5,/)
263: 201 FORMAT(5X,'IX =',I3,5X,'IY =',I3,5X,'IZ =',I3,/)
264: 202 FORMAT(5X,'YMAX =',F9.1,' M',5X,'H =',F8.2,' M',/)
265: 203 FORMAT(5X,'UST =',F8.2,' M/MIN',5X,'UGX =',F8.2,' M/MIN',5X,'A' =',
266: 1,F7.3,5X,'TCH =',F5.1,' MIN',5X,'P =',F6.2)
267: 204 FORMAT(5X,'KS =',I3,3X,'LS =',I4,2X,' CO =',F9.2,' MS/CM',3X,
268: 1'XMAX =',F9.1,' M',/)
269: 205 FORMAT(10(/),5X,'INPUT DATA')
270: 206 FORMAT(35X,'***** ***/)
271: 207 FORMAT(5X,'STABILITY CLASS =',I4,5X,' I IVPS =',I3,5X,' ALPHA =',F7
272: 1.2,5X,' AK =',E10.2,' 1/MIN',/)
273: 208 FORMAT(5X,'PROFL =',F6.2,' MIN',/)
274: 209 FORMAT(5X,'NUMBER OF SOURCES =',I4,/)
275: STOP
276: END

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1:      SUBROUTINE FCT(X,Y,DERY)                                FCT  10
2:      C                                                        FCT  20
3:      C                                                        FCT  30
4:      C THIS SUBROUTINE COMPUTES THE DERIVATIVES(RIGHT HAND SIDES) OF THE FCT  40
5:      C SYSTEM TO GIVEN VALUES OF X(TIME) AND Y(CONCENTRATION) FCT  50
6:      C                                                        FCT  60
7:      C                                                        FCT  70
8:      C      DIMENSION Y(700),DERY(700),PAC(700),C70(700),CZ1(700),CZ2(700), FCT  80
9:      C      1CZ1(700),CYK(700),R2(15),R52I(15,15,15),CCC(15,15) FCT  90
10:     C      COMMON /BLK1/ A1(15,15),A2(15,15),A3(15,15),B1(15,15),B2(15,15), FCT 100
11:     C      113(15,15),R1(15),R3(15),R5(15),R6(15),R361(15),R362(15),APA1(15), FCT 110
12:     C      2R36I(15,15),J(700),U(15),V(15),XXX(3,15),XYY(15),XZ7(15),XMAX(3), FCT 120
13:     C      3YMAX,H,AK,TCH,P,KS(3),LS(3),CO(3),NX,JY,NZ,N1,N2,N3,KX,KY,KZ, FCT 130
14:     C      4v1(15),W2(15),W3(15),NSRCS,IFLG,'FLG',CC(3,15,15,15),PRDEL,PRMT3, FCT 140
15:     C      5INVR5 FCT 150
16:     C      INTEGER VAR1,VAR2,VAR3,VAR4,VAR5,VAR6,VAR7 FCT 160
17:     C      DIM=(NX+1)*NY*N7 FCT 170
18:     C      DO 4 L=2,K7 FCT 180
19:     C      4 R1(L)=U(L)/XMAX(IFLG) FCT 190
20:     C                                                        FCT 200
21:     C VARIATION IN THE V VELOCITY FCT 210
22:     C                                                        FCT 220
23:     C      IF(X-TCH) 1,2,2 FCT 230
24:     C      1 CONTINUE FCT 240
25:     C      DO 5 L=2,KZ FCT 250
26:     C      V(L)=P*U(L)*(X/TCH) FCT 260
27:     C      5 R2(L)=V(L)/(2.*YMAX) FCT 270
28:     C      GO TO 3 FCT 280
29:     C      2 CONTINUE FCT 290
30:     C      DO 6 L=2,KZ FCT 300
31:     C      V(L)=P*U(L) FCT 310
32:     C      6 R2(L)=V(L)/(2.*YMAX) FCT 320
33:     C      3 CONTINUE FCT 330
34:     C                                                        FCT 340
35:     C COMPUTATION OF THE DERIVATIVES FCT 350

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36:	C		FCT	360
37:		DD 33 L=2,KZ	FCT	370
38:		DD 33 K=2,KY	FCT	380
39:		DD 33 I=2,KY	FCT	390
40:	33	R52I(L,K,I)=R5(L)*P2(K,I)-R2(L)*A2(K,I)	FCT	400
41:		DD 39 LL=1,NDIM	FCT	410
42:		C70(LL)=0.	FCT	420
43:		CZI(LL)=0.	FCT	430
44:		CZ2(LL)=0.	FCT	440
45:	39	CYK(LL)=0.	FCT	450
46:		J=1	FCT	460
47:		JJ=KX	FCT	470
48:		IF(IFLG.EQ.1) GO TO 35	FCT	480
49:		IX=IFIX(X/(PRMT3-.01))	FCT	490
50:		IIFK=(IFLG-2)*97+(IX+1)	FCT	500
51:		HEAD(4'IIBK) ((CCC(K,L),K=2,KY),L=1,N3)	FCT	510
52:	35	CONTINUE	FCT	520
53:		DD 51 LK=2,KY	FCT	530
54:		DD 51 LZ=2,KZ	FCT	540
55:		DD 50 LJ=J,JJ	FCT	550
56:		VAR1=KS(IFLG-1)	FCT	560
57:		VAR2=LS(IFLG-1)	FCT	570
58:		VAR3=LJ-(J-1)+1	FCT	580
59:		IF(IFLG.EQ.1) GO TO 40	FCT	590
60:		IF(LK.EQ.KS(IFLG).AND.LZ.EQ.LS(IFLG)) GO TO 10	FCT	600
61:		PAC(LJ)=0.	FCT	610
62:		IF(CCC(VAR1,VAR2).GT.0.) PAC(LJ)=CCC(LK,LZ)*A1(VAR3,1)	FCT	620
63:		GO TO 20	FCT	630
64:	10	PAC(LJ)=C0(IFLG)*A1(VAR3,1)	FCT	640
65:		IF(CCC(VAR1,VAR2).GT.0.) PAC(LJ)=PAC(LJ)+CCC(LK,LZ)*A1(VAR3,1)	FCT	650
66:		GO TO 20	FCT	660
67:	40	IF(LK.EQ.KS(1).AND.LZ.EQ.LS(1)) GO TO 11	FCT	670
68:		PAC(LJ)=0.	FCT	680
69:		GO TO 20	FCT	690
70:	11	PAC(LJ)=C0(1)*A1(VAR3,1)	FCT	700
71:	20	CONTINUE	FCT	710

72:	DO 60 I=1,KX	FCT	720
73:	VAR4=I+1	FCT	730
74:	VAR5=I+J-1	FCT	740
75:	60 PAC(LJ)=PAC(LJ)+A1(VAR3,VAR4)*Y(VAR5)	FCT	750
76:	DO 70 I=2,KZ	FCT	760
77:	VAR6=LJ+KX*(I-LZ)	FCT	770
78:	CZ2(LJ)=CZ2(LJ)+APA1(I)*Y(VAR6)*FLOAT(INVPS)	FCT	780
79:	C70(LJ)=CZ0(LJ)+A3(1,I)*Y(VAR6)	FCT	790
80:	70 CZI(LJ)=CZI(LJ)+R36I(LZ,I)*Y(VAR6)	FCT	800
81:	CZ1(LJ)=(-A3(1,N3)*C72(LJ)-C70(LJ))/A3(1,1)	FCT	810
82:	DO 80 I=2,KY	FCT	820
83:	VAR7=LJ+(I-LK)*(KZ-1)*KX	FCT	830
84:	80 CYK(LJ)=CYK(LJ)+R52I(LZ,LK,I)*Y(VAR7)	FCT	840
85:	50 DERY(LJ)=-R1(L7)*PAC(LJ)+R361(L7)*CZ1(IJ)+R362(LZ)*CZ2(LJ)+CZI(LJ)	FCT	850
86:	1+CYK(LJ)+C(LJ)-AK*Y(IJ)	FCT	860
87:	J=JJ+1	FCT	870
88:	JJ=J+KX-1	FCT	880
89:	51 CONTINUE	FCT	890
90:	RETURN	FCT	900
91:	END	FCT	910

1:	SUBROUTINE JCBI(N,NO,N1,AL,PE,FA,FP,FC,ROOT)	JCBI 10
2:	C	JCBI 20
3:	C	JCBI 30
4:	C THIS SUBROUTINE COMPUTES THE ROOTS OF AN NTH-DEGREE JACOBI POLYNOMIAL	JCBI 40
5:	C AND THE DERIVATIVES OF THE POLYNOMIAL AT THESE POINTS	JCBI 50
6:	C	JCBI 60
7:	C	JCBI 70
8:	C N - THE NUMBER OF INTERIOR POINTS	JCBI 80
9:	C NO - 1 OR 0 IF X=0 IS INCLUDED OR NOT	JCBI 90
10:	C N1 - SAME AS NO, FOR THE POINT X=1	JCBI 100
11:	C AL,BF - THE QUANTITIES ALFA AND BETA FOR THE WEIGHTING	JCBI 110
12:	C FUNCTION	JCBI 120
13:	C FA,FC,FC - THE FIRST,SECOND AND THIRD DERIVATIVES OF THE	JCBI 130
14:	C POLYNOMIAL AT THE ROOTS	JCBI 140
15:	C ROOT - OUTPUT ARRAY CONTAINING THE N+NO+N1 ROOTS OF THE	JCBI 150
16:	C POLYNOMIAL	JCBI 160
17:	C	JCBI 170
18:	C	JCBI 180
19:	DIMENSION FA(1),FC(1),FC(1),ROOT(1)	JCBI 190
20:	AP=AL+PE	JCBI 200
21:	AD=BF-AL	JCBI 210
22:	AP=BF*AL	JCBI 220
23:	FA(1)=(AD/(AB+2.))+1.)/2.	JCBI 230
24:	FP(1)=0.	JCBI 240
25:	DO 10 I=2,N	JCBI 250
26:	Z1=FLOAT(I)-1.	JCBI 260
27:	Z=AB+2.*Z1	JCBI 270
28:	FA(I)=(AB/Z*AD/(Z+2.))+1.)/2.	JCBI 280
29:	IF(I-2) 11,12,11	JCBI 290
30:	12 FP(I)=(AP+AP+Z1)/Z/Z/(Z+1.)	JCBI 300
31:	CONTINUE	JCBI 310
32:	11 Z=Z*Z	JCBI 320
33:	Y=Z1*(AP+Z1)	JCBI 330
34:	Y=Y*(AP+Y)	JCBI 340
35:	FP(I)=Y/7/(Z-1.)	JCBI 350

```

36: 10    CONTINUE
37:      X=0.
38:      DO 20 I=1,N
39:        I1=I-1
40: 25      XD=0.
41:        XN=1.
42:        XD1=0.
43:        XN1=0.
44:        DO 30 J=1,N
45:          XP=(FA(J)-X)*XN-FB(J)*XD
46:          XP1=(FA(J)-X)*XN1-FB(J)*XD1-XN
47:          XD=XP
48:          XD1=XN1
49:          XN=XP
50: 30      XN1=XP1
51:        ZC=1.
52:        Z=XN/XN1
53:        IF(I1) 21,21,22
54: 22      DO 23 J=1,I1
55: 23      ZC=ZC-Z/(X-ROOT(J))
56: 21      Z=Z/ZC
57:        X=X-Z
58:        IF(ABS(Z)-1.E-7) 26,26,25
59: 26      ROOT(I)=X
60:        X=X+0.0005
61: 20      CONTINUE
62:        NT=N+NO+N1
63:        IF(NO-1) 35,36,35
64: 36      DO 42 I=1,N
65:        J=N+1-I
66: 42      ROOT(J+1)=ROOT(J)
67:        ROOT(1)=0.
68: 35      IF(N1-1) 38,37,38
69: 37      ROOT(NT)=1.
70: 38      DO 40 I=1,NT
71:        X=ROOT(I)

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```

JCBI 360
JCBI 370
JCBI 380
JCBI 390
JCBI 400
JCBI 410
JCBI 420
JCBI 430
JCBI 440
JCBI 450
JCBI 460
JCBI 470
JCBI 480
JCBI 490
JCBI 500
JCBI 510
JCBI 520
JCBI 530
JCBI 540
JCBI 550
JCBI 560
JCBI 570
JCBI 580
JCBI 590
JCBI 600
JCBI 610
JCBI 620
JCBI 630
JCBI 640
JCBI 650
JCBI 660
JCBI 670
JCBI 680
JCBI 690
JCBI 700
JCBI 710

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72:      FA(I)=1.
73:      FB(I)=0.
74:      FC(I)=0.
75:      IF(40-J=1,NT)
76:      IF(J-I) 41,40,41
77:  41    Y=X-ROOT(J)
78:      FC(I)=Y*FC(I)+3.*FB(I)
79:      FB(I)=Y*FB(I)+2.*FA(I)
80:      FA(I)=Y*FA(I)
81:  40    CONTINUE
82:      RETURN
83:      END

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```

JCBI 720
JCPI 730
JCPI 740
JCBI 750
JCBI 760
JCPI 770
JCPI 780
JCPI 790
JCPI 800
JCPI 810
JCPI 820
JCPI 830

```

1:	SUBROUTINE DEOPR(J,NO,N1,I,ID,FA,FB,FC,ROOT,VECT)	DEOP	10
2:	C	DEOP	20
3:	C	DEOP	30
4:	C THIS SUBROUTINE CALCULATES THE A AND B MATRICES AND THE QUADRATURE	DEOP	40
5:	C WEIGHTS FROM THE QUANTITIES DERIVED IN SUBROUTINE JCBI	DEOP	50
6:	C	DEOP	60
7:	C	DEOP	70
8:	C N,NO,N1 - SAME AS JCBI	DEOP	80
9:	C I - DIFFERENTIAL OPERATOR AT X=ROOT(I)	DEOP	90
10:	C ID - INDICATOR, I.E. 1 FOR MATRIX A, 2 FOR MATRIX B,	DEOP	100
11:	C 3 FOR QUADRATURE WEIGHTS W	DEOP	110
12:	C FA,FB,FC - COMPUTED IN JCBI	DEOP	120
13:	C ROOT - COMPUTED IN JCBI	DEOP	130
14:	C VECT - CONTAINS THE COMPUTED VECTOR	DEOP	140
15:	C	DEOP	150
16:	C	DEOP	160
17:	DIMENSION FA(1),FB(1),FC(1),ROOT(1),VECT(1)	DEOP	170
18:	NT=N+NO+N1	DEOP	180
19:	IF(ID-3) 1,10,10	DEOP	190
20:	1 DO 20 J=1,NT	DEOP	200
21:	IF(J-1) 21,2,21	DEOP	210
22:	2 IF(ID-1) 5,4,5	DEOP	220
23:	4 VECT(I)=FB(I)/FA(I)/2.	DEOP	230
24:	GO TO 20	DEOP	240
25:	5 VECT(I)=FC(I)/FA(I)/3.	DEOP	250
26:	GO TO 20	DEOP	260
27:	21 Y=ROOT(I)-ROOT(J)	DEOP	270
28:	VECT(J)=FA(I)/FA(J)/Y	DEOP	280
29:	IF(ID-2) 20,22,20	DEOP	290
30:	22 VECT(J)=VECT(J)*(FB(I)/FA(I)-2./Y)	DEOP	300
31:	20 CONTINUE	DEOP	310
32:	GO TO 50	DEOP	320
33:	10 Y=0.	DEOP	330
34:	IF(ID-4) 31,30,31	DEOP	340
35:	31 DO 25 J=1,NT	DEOP	350

36:	X=ROOT(J)	DECP 360
37:	AX=X*(1.-X)	DECP 370
38:	IF(N0) 26,27,26	DECP 380
39: 27	AX=AX/X/X	DECP 390
40: 26	IF(N1) 28,29,23	DECP 400
41: 29	AX=AX/(1.-X)/(1.-X)	DECP 410
42: 28	VECT(J)=AX/FA(J)/FA(J)	DECP 420
43: 25	Y=Y+VECT(J)	DECP 430
44:	CONTD 50	DECP 440
45: 30	DO 35 J=1,NT	DECP 450
46:	X=ROOT(J)	DECP 460
47:	IF(N0) 36,37,36	DECP 470
48: 37	AX=1./X	DECP 480
49: 36	IF(N1) 38,39,38	DECP 490
50: 39	AX=1./(1.-X)	DECP 500
51: 38	VECT(J)=AX/FA(J)/FA(J)	DECP 510
52: 35	Y=Y+VECT(J)	DECP 520
53: 60	DO 61 J=1,NT	DECP 530
54: 61	VECT(J)=VECT(J)/Y	DECP 540
55: 50	RETURN	DECP 550
56:	END	DECP 560

```

1:      SUBROUTINE OUTP(X,Y,DERY,IHLF,NDIN,PRMT)      OUTP  10
2:      C      OUTP  20
3:      C      OUTP  30
4:      C      THIS SUBROUTINE GIVES THE OUTPUT OF THE MODEL      OUTP  40
5:      C      OUTP  50
6:      C      OUTP  60
7:      C      PRDEL      - THE INTERVAL AT WHICH THE RESULTS WILL BE PRINTED      OUTP  70
8:      C      T OR THETA - TIME BETWEEN THE POLLUTANT RELEASE(TIMIT) AND THE      OUTP  80
9:      C      INITIATION OF THE AVERAGING TIME      OUTP  90
10:     C      OMEGA      - END OF THE AVERAGING TIME      OUTP 100
11:     C      QX(I,J)    - FLUX ACROSS Y-Z PLANE AT X=JTH. POINT DUE TO ITH.      OUTP 110
12:     C      AND PRECEDING SOURCES      OUTP 120
13:     C      OUTP 130
14:     C      OUTP 140
15:     C      DIMENSION PRMT(5),Y(700),DERY(700),CZ0(700),CZ1(700),CZ2(700),      OUTP 150
16:     C      IC(15,15,15),QX(3,15),IHL(3,50)      OUTP 160
17:     C      COMMON /PLK1/ A1(15,15),A2(15,15),A3(15,15),R1(15,15),L2(15,15),      OUTP 170
18:     C      R3(15,15),R1(15),R3(15),R5(15),R4(15),R361(15),R362(15),APA1(15),      OUTP 180
19:     C      R361(15,15),J(700),U(15),V(15),XXX(3,15),XYY(15),XZZ(15),XMAX(3),      OUTP 190
20:     C      3YMAX,H,AK,TCH,P,KS(3),LS(3),CO(3),NX,NY,NZ,N1,N2,N3,KX,KY,KZ,      OUTP 200
21:     C      4W1(15),W2(15),W3(15),NSPCS,IFLG,MFLG,CC(3,15,15,15),PRDEL,PRMT3,      OUTP 210
22:     C      SINVRG      OUTP 220
23:     C      INTEGER VAR10,VAR11,VAR12,VAR13,VAR14,VAR15      OUTP 230
24:     C      IFLAG=IFLG      OUTP 240
25:     C      IF(MFLG.EQ.1) GO TO 15      OUTP 250
26:     C      IF(NSPCS.NE.1) GO TO 70      OUTP 260
27:     C      IF(X.EQ.0.0) IIII=0      OUTP 270
28:     C      IF(X.EQ.0.0) GO TO 71      OUTP 280
29:     C      AAI=FLOAT(IIII)      OUTP 290
30:     C      AAI1=AAI-X/PRDEL      OUTP 300
31:     C      IAI=IFIX(AAI1*100.)      OUTP 310
32:     C      IF(IAI.EQ.0) GO TO 71      OUTP 320
33:     C      GO TO 800      OUTP 330
34:     C      70 IF(X.EQ.0.0) II=0      OUTP 340
35:     C      IF(X.EQ.0.0) GO TO 71      OUTP 350

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36:	AI=FLOAT(II)	OUTPUT 360
37:	AI1=AI-X/PRMT(3)	OUTPUT 370
38:	I1=IFIX(AI1*100.)	OUTPUT 380
39:	IF(I1.EQ.0) GO TO 71	OUTPUT 390
40:	GO TO 800	OUTPUT 400
41:	71 CONTINUE	OUTPUT 410
42:	J=1	OUTPUT 420
43:	JJ=KX	OUTPUT 430
44:	DO 2 ID=1,NY	OUTPUT 440
45:	DO 1 LJ=J,JJ	OUTPUT 450
46:	CZ0(LJ)=0.	OUTPUT 460
47:	CZ2(LJ)=0.	OUTPUT 470
48:	DO 5 I=2,KZ	OUTPUT 480
49:	VAR10=LJ+KX*(I-2)	OUTPUT 490
50:	CZ2(LJ)=CZ2(LJ)+APA1(I)*Y(VAR10)*FLOAT(INVRS)	OUTPUT 500
51:	5 CZ0(LJ)=CZ0(LJ)+A3(1,I)*Y(VAR10)	OUTPUT 510
52:	CZ1(LJ)=(-A3(1,N3)*CZ2(LJ)-CZ0(LJ))/A3(1,1)	OUTPUT 520
53:	1 CONTINUE	OUTPUT 530
54:	J=ID*NZ*KX+1	OUTPUT 540
55:	JJ=J+KX-1	OUTPUT 550
56:	2 CONTINUE	OUTPUT 560
57:	IND=2	OUTPUT 570
58:	I1=1	OUTPUT 580
59:	I2=KX	OUTPUT 590
60:	DO 10 K=2,KY	OUTPUT 600
61:	J=2	OUTPUT 610
62:	DO 21 I=M1,M2	OUTPUT 620
63:	C(J,K,1)=CZ1(I)	OUTPUT 630
64:	21 J=J+1	OUTPUT 640
65:	M3=M1	OUTPUT 650
66:	M4=M2	OUTPUT 660
67:	DO 20 L=2,KZ	OUTPUT 670
68:	J=2	OUTPUT 680
69:	DO 31 I=M3,M4	OUTPUT 690
70:	C(J,K,L)=Y(I)	OUTPUT 700
71:	31 J=J+1	OUTPUT 710

72:	N3=M4+1	OUTP 720
73:	M4=IND*KX	OUTP 730
74:	IND=IND+1	OUTP 740
75:	20 CONTINUE	OUTP 750
76:	J=2	OUTP 760
77:	LN 22 I=M1,M2	OUTP 770
78:	C(J,K,N3)=CZ2(I)	OUTP 780
79:	22 J=J+1	OUTP 790
80:	M1=M3	OUTP 800
81:	M2=M4	OUTP 810
82:	10 CONTINUE	OUTP 820
83:	CALL ZERO(C)	OUTP 830
84:	IF(NSRCS.EQ.1) GO TO 65	OUTP 840
85:	IX=IFIX(X/(PRMT3-.01))	OUTP 850
86:	IIRK=(IFLG-1)*97+(IX+1)	OUTP 860
87:	WRITE(4'IIRK) ((C(N1,K,L),K=2,KY),L=1,N3)	OUTP 870
88:	II=II+1	OUTP 880
89:	IF(X.EQ.0.0) III=0	OUTP 890
90:	IF(X.EQ.0.0) GO TO 15	OUTP 900
91:	AII=FLOAT(III)	OUTP 910
92:	AIII=AII-X/PROFL	OUTP 920
93:	IIII=IFIX(AIII*100.)	OUTP 930
94:	IF(IIII.EQ.0) GO TO 65	OUTP 940
95:	GO TO 800	OUTP 950
96:	65 CONTINUE	OUTP 960
97:	III=III+1	OUTP 970
98:	IF(IFLG.EQ.1.AND.NSRCS.EQ.1) IIII=IIII+1	OUTP 980
99:	IIX=IFIX(X/(PROEL-.01))	OUTP 990
100:	IF(IFLG.EQ.NSRCS) GO TO 80	OUTP1000
101:	LN 90 J=2,N1	OUTP1010
102:	IIRK=J+(IFLG-1)*49*15+IIX*15	OUTP1020
103:	90 WRITE(2'IIRK) ((C(J,K,L),K=2,KY),L=1,N3)	OUTP1030
104:	IHL(IFLG,IIX+1)=IHLF	OUTP1040
105:	GO TO 800	OUTP1050
106:	80 CALL AVG(C,IIX,IFLAG)	OUTP1060
107:	IF(IIX.EQ.1.AND.NSRCS.EQ.1) GO TO 600	OUTP1070

108:	IF(IIX.EQ.1) GO TO 74	OUTP1080
109:	DO 67 J=2,N1	OUTP1090
110:	DO 67 K=2,KY	OUTP1100
111:	DO 67 L=1,N3	OUTP1110
112:	67 CC(IFLG,J,K,L)=C(J,K,L)	OUTP1120
113:	IF(X.FQ.0.0) GO TO 800	OUTP1130
114:	T=X-2.*PPDEL	OUTP1140
115:	IHL(IFLG,IIX+1)=IHLF	OUTP1150
116:	IF(NSRCS.FQ.1) GO TO 18	OUTP1160
117:	74 IIFLG=IFLG	OUTP1170
118:	78 IIFLG=IIFLG-1	OUTP1180
119:	IF(IIFLG.EQ.0) GO TO 18	OUTP1190
120:	DO 75 J=2,N1	OUTP1200
121:	IPLI=J+(IIFLG-1)*4+15+IIX*15	OUTP1210
122:	75 READ(2,IPLI) ((C(J,K,L),K=2,KY),L=1,N3)	OUTP1220
123:	CALL AVG(C,IIX,IIFLG)	OUTP1230
124:	IF(IIX.EQ.1.AND.IIFLG.EQ.1) GO TO 800	OUTP1240
125:	DO 76 J=2,N1	OUTP1250
126:	DO 76 K=2,KY	OUTP1260
127:	DO 76 L=1,N3	OUTP1270
128:	76 CC(IIFLG,J,K,L)=C(J,K,L)	OUTP1280
129:	GO TO 78	OUTP1290
130:	15 T=0.	OUTP1300
131:	IIX=0	OUTP1310
132:	DO 91 J=1,NSRCS	OUTP1320
133:	91 IHL(J,1)=0	OUTP1330
134:	IF(MFLG.EQ.1) GO TO 16	OUTP1340
135:	CALL AVG(C,IIX,IFLAG)	OUTP1350
136:	III=III+1	OUTP1360
137:	GO TO 800	OUTP1370
138:	18 CONTINUE	OUTP1380
139:	VAR11=KS(1)	OUTP1390
140:	VAR12=LS(1)	OUTP1400
141:	CC(1,1,VAR11,VAR12)=C0(1)	OUTP1410
142:	IF(NSRCS.EQ.1) GO TO 16	OUTP1420
143:	DO 17 I=2,NSRCS	OUTP1430

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144:      VAR13=I-1                                OUTPUT1440
145:      VAR14=KS(I)                                OUTPUT1450
146:      VAR15=LS(I)                                OUTPUT1460
147:      17 CC(VAR13,N1,VAR14,VAR15)=CC(VAR13,N1,VAR14,VAR15)+CO(I)    OUTPUT1470
148:      16 WRITE(6,131) T,X,((IHL(J,IIX+1),J=1,NSRCS)              OUTPUT1480
149:      WRITE(6,204)                                                OUTPUT1490
150:      WRITE(6,210) XXX(1,1),((XXX(J,I),I=2,N1),J=1,NSRCS)        OUTPUT1500
151:      WRITE(6,215)                                                OUTPUT1510
152:      WRITE(6,208)                                                OUTPUT1520
153:      L=N3+1                                                OUTPUT1530
154:      53 L=L-1                                                OUTPUT1540
155:      WRITE(6,205) XZZ(L)                                        OUTPUT1550
156:      DO 41 K=2,KY                                             OUTPUT1560
157:      WRITE(6,134) XYY(K),CC(1,1,K,L),((CC(I,J,K,L),J=2,N1),I=1,NSRCS) OUTPUT1570
158:      41 CONTINUE                                             OUTPUT1580
159:      IF(L.EQ.1) GO TO 40                                     OUTPUT1590
160:      GO TO 53                                                OUTPUT1600
161:      40 CONTINUE                                             OUTPUT1610
162:      DO 50 I=1,NSRCS                                         OUTPUT1620
163:      DO 50 J=1,N1                                             OUTPUT1630
164:      QX(I,J)=0.                                              OUTPUT1640
165:      DO 52 K=2,KY                                             OUTPUT1650
166:      DO 52 L=1,N3                                             OUTPUT1660
167:      52 QX(I,J)=QX(I,J)+CC(I,J,K,L)*U(L)*W2(K)*W3(L)          OUTPUT1670
168:      QX(I,J)=QX(I,J)/60000.*H*2.*YMAX                      OUTPUT1680
169:      50 CONTINUE                                             OUTPUT1690
170:      WRITE(6,220) QX(1,1),((QX(J,I),I=2,N1),J=1,NSRCS)        OUTPUT1700
171:      400 CONTINUE                                             OUTPUT1710
172:      C                                                        OUTPUT1720
173:      131 FORMAT(8(/),30X,'THETA =',F6.2,' MIN',/,30X,'OMEGA =',F6.2,' MIN', OUTPUT1730
174:      110X,'IHLF =',3I3)                                       OUTPUT1740
175:      134 FORMAT(1X,'Y=',F6.1,' M ',15F8.2)                  OUTPUT1750
176:      204 FORMAT(/,30X,'X DIRECTION (METERS)',/)              OUTPUT1760
177:      205 FORMAT(/,5X,'Z DIRECTION =',F10.1,' M',/)           OUTPUT1770
178:      208 FORMAT(35X,'*****')                                OUTPUT1780
179:      210 FORMAT(11X,F8.1,1X,14F8.1)                          OUTPUT1790

```



```
180: 215 FORMAT(//,38X,'CONCENTRATION(MG/CCU.M)')
181: 220 FORMAT(4(/),1X,'QX(GR/SEC)=' ,15F9.2)
182: RETURN
183: END
```

```
OUTP1800
OUTP1810
OUTP1820
OUTP1830
```

1:	SUBROUTINE ZERO(C)	ZERO	10
2:	C	ZERO	20
3:	C	ZERO	30
4:	C THIS SUBROUTINE CLEANS THE OUTPUT OF THE MODEL	ZERO	40
5:	C	ZERO	50
6:	C	ZERO	60
7:	DIMENSION C(15,15,15)	ZERO	70
8:	COMMON /ILK1/ A1(15,15),A2(15,15),A3(15,15),P1(15,15),P2(15,15),	ZERO	80
9:	P3(15,15),R1(15),P3(15),P5(15),R5(15),R361(15),R362(15),APA1(15),	ZERO	90
10:	2P36I(15,15),Q(700),U(15),V(15),XXX(3,15),XYY(15),XZZ(15),XMAX(3),	ZERO	100
11:	3YMAX,H,AK,TCH,P,KS(3),LS(3),CO(3),NX,NY,NZ,N1,N2,N3,KX,KY,KZ,	ZERO	110
12:	4w1(15),w2(15),w3(15),NSRCS,IFLG,IFLG,CC(3,15,15,15),PMDEL,PRAT3,	ZERO	120
13:	5INVRS	ZERO	130
14:	J=2	ZERO	140
15:	55 K=KS(IFLG)	ZERO	150
16:	L=LS(IFLG)	ZERO	160
17:	IF(C(J,K,L).LE.0.) GO TO 10	ZERO	170
18:	12 L=L+1	ZERO	180
19:	IF(L.GT.N3) GO TO 14	ZERO	190
20:	IF(C(J,K,L).LE.0.) GO TO 20	ZERO	200
21:	GO TO 12	ZERO	210
22:	14 L=LS(IFLG)	ZERO	220
23:	15 L=L-1	ZERO	230
24:	IF(L.LT.1) GO TO 30	ZERO	240
25:	IF(C(J,K,L).LE.0.) GO TO 25	ZERO	250
26:	GO TO 15	ZERO	260
27:	20 DO 21 I=L,N3	ZERO	270
28:	21 C(J,K,I)=0.	ZERO	280
29:	GO TO 14	ZERO	290
30:	25 C(J,K,L)=0.	ZERO	300
31:	L=L-1	ZERO	310
32:	IF(L.EQ.0) GO TO 30	ZERO	320
33:	GO TO 25	ZERO	330
34:	30 L=LS(IFLG)	ZERO	340
35:	K=KS(IFLG)	ZERO	350

```

36:      33 L=LS(IFLG)
37:      K=K+1
38:      IYD=1
39:      IF(K.EQ.N2) GO TO 32
40:      52 IF(C(J,K,L).LE.0.) GO TO 35
41:      GO TO 37
42:      35 GO 36 I=1,N3
43:      36 C(J,K,I)=0.
44:      IF(IYD.EQ.1) GO TO 85
45:      GO TO 86
46:      85 DO 80 I=K,KY
47:      90 C(J,I,L)=0.
48:      GO TO 87
49:      86 KIND=K
50:      93 C(J,KIND,L)=0.
51:      IF(KIND.EQ.1) GO TO 87
52:      KIND=KIND-1
53:      GO TO 88
54:      87 CONTINUE
55:      IF(IYD.EQ.1) GO TO 33
56:      GO TO 51
57:      37 L=L+1
58:      IF(L.GT.N3) GO TO 38
59:      IF(C(J,K,L).LE.0.) GO TO 39
60:      GO TO 37
61:      39 GO 40 I=L,N3
62:      40 C(J,K,I)=0.
63:      38 L=LS(IFLG)
64:      L=L-1
65:      IF(L.GE.1) GO TO 63
66:      IF(IYD.EQ.1) GO TO 33
67:      IF(IYD.EQ.2) GO TO 51
68:      63 IF(C(J,K,L).LE.0.) GO TO 42
69:      GO TO 68
70:      42 C(J,K,L)=0.
71:      L=L-1

```

```

ZERO 360
ZERO 370
ZERO 380
ZERO 390
ZERO 400
ZERO 410
ZERO 420
ZERO 430
ZERO 440
ZERO 450
ZERO 460
ZERO 470
ZERO 480
ZERO 490
ZERO 500
ZERO 510
ZERO 520
ZERO 530
ZERO 540
ZERO 550
ZERO 560
ZERO 570
ZERO 580
ZERO 590
ZERO 600
ZERO 610
ZERO 620
ZERO 630
ZERO 640
ZERO 650
ZERO 660
ZERO 670
ZERO 680
ZERO 690
ZERO 700
ZERO 710

```

72:	IF(L.EQ.1) GO TO 42	ZERO 720
73:	IF(IYD.EQ.1) GO TO 33	ZERO 730
74:	IF(IYD.EQ.2) GO TO 51	ZERO 740
75:	32 L=LS(IFLG)	ZERO 750
76:	K=KS(IFLG)	ZERO 760
77:	51 L=LS(IFLG)	ZERO 770
78:	K=K-1	ZERO 780
79:	IYD=2	ZERO 790
80:	IF(K.EQ.1) GO TO 50	ZERO 800
81:	GO TO 52	ZERO 810
82:	50 J=J+1	ZERO 820
83:	IF(J.GT.N1) GO TO 60	ZERO 830
84:	GO TO 55	ZERO 840
85:	10 DO 58 I=J,N1	ZERO 850
86:	DO 58 K=2,KY	ZERO 860
87:	DO 58 L=1,N3	ZERO 870
88:	58 C(I,K,L)=0.	ZERO 880
89:	60 CONTINUE	ZERO 890
90:	RETURN	ZERO 900
91:	END	ZERO 910

1:	SUBROUTINE AVG(C,II,IFLAG)	AVG	10
2:	C	AVG	20
3:	C	AVG	30
4:	C THIS SUBROUTINE COMPUTES THE AVERAGE CONCENTRATIONS (AVERAGING	AVG	40
5:	C TIME = 2*PRDEL)	AVG	50
6:	C	AVG	60
7:	C	AVG	70
8:	DIMENSION C(15,15,15),D(15,15,15)	AVG	80
9:	COMMON /PLK1/ A1(15,15),A2(15,15),A3(15,15),P1(15,15),P2(15,15),	AVG	90
10:	P3(15,15),P4(15,15),R3(15,15),R5(15,15),R6(15,15),P361(15,15),R362(15,15),APA1(15,15),	AVG	100
11:	P364(15,15),O(700),U(15,15),V(15,15),XXX(3,15),XYY(15,15),XZ7(15,15),XMAX(3,15),	AVG	110
12:	3YMAX,H,AK,TCH,P,KS(3,15),LS(3,15),CO(3,15),IX,IY,I7,N1,N2,N3,KX,KY,KZ,	AVG	120
13:	4U1(15,15),W2(15,15),W3(15,15),MSRCS,IFLG,MFLG,CC(15,15,15,15),PRDEL,PRMT3,	AVG	130
14:	5INVR5	AVG	140
15:	IF(II.GT.2) GO TO 90	AVG	150
16:	M=II+1	AVG	160
17:	DO 10 J=2,N1	AVG	170
18:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVG	180
19:	10 WRITE(3,IPLK) ((C(J,K,L),K=2,KY),L=1,N3)	AVG	190
20:	IF(II.EQ.2) GO TO 80	AVG	200
21:	RETURN	AVG	210
22:	10 M=2	AVG	220
23:	DO 15 J=2,N1	AVG	230
24:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVG	240
25:	15 READ(3,IPLK) ((D(J,K,L),K=2,KY),L=1,N3)	AVG	250
26:	M=1	AVG	260
27:	DO 20 J=2,N1	AVG	270
28:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVG	280
29:	20 WRITE(3,IPLK) ((D(J,K,L),K=2,KY),L=1,N3)	AVG	290
30:	M=3	AVG	300
31:	DO 35 J=2,N1	AVG	310
32:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVG	320
33:	35 READ(3,IPLK) ((D(J,K,L),K=2,KY),L=1,N3)	AVG	330
34:	M=2	AVG	340
35:	DO 45 J=2,N1	AVG	350

36:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AV ,	360
37:	45 WRITE(3,IPLK) ((D(J,K,L),K=2,KY),L=1,N3)	AV ,	370
38:	M=3	AVC	380
39:	DO 50 J=2,N1	AVC	390
40:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVC	400
41:	55 WRITE(3,IPLK) ((C(J,K,L),K=2,KY),L=1,N3)	AVC	410
42:	80 CONTINUE	AVC	420
43:	M=1	AVC	430
44:	DO 70 J=2,N1	AVC	440
45:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVC	450
46:	70 READ(3,IPLK) ((C(J,K,L),K=2,KY),L=1,N3)	AVC	460
47:	M=2	AVC	470
48:	DO 71 J=2,N1	AVC	480
49:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVC	490
50:	71 READ(3,IPLK) ((D(J,K,L),K=2,KY),L=1,N3)	AVC	500
51:	DO 72 J=2,N1	AVC	510
52:	DO 72 K=2,KY	AVC	520
53:	DO 72 L=1,N3	AVC	530
54:	72 C(J,K,L)=C(J,K,L)+D(J,K,L)	AVC	540
55:	M=3	AVC	550
56:	DO 73 J=2,N1	AVC	560
57:	IPLK=J+(IFLAG-1)*15+(M-1)*45	AVC	570
58:	73 READ(3,IPLK) ((D(J,K,L),K=2,KY),L=1,N3)	AVC	580
59:	DO 74 J=2,N1	AVC	590
60:	DO 74 K=2,KY	AVC	600
61:	DO 74 L=1,N3	AVC	610
62:	74 C(J,K,L)=(C(J,K,L)+D(J,K,L))/3.	AVC	620
63:	RETURN	AVC	630
64:	END	AVC	640

```

1:      SUPROUTINE RKGS(PRMT,Y,DERY,NDIM,IHLF,FCT,OUTP,AUX)      RKGS 10
2:      C                                                         RKGS 20
3:      C                                                         RKGS 30
4:      C THIS SU ROUTINE SOLVES A SYSTEM OF FIRST ORDER ORDINARY DIFFERENTIAL RKGS 40
5:      C EQUATIONS WITH GIVEN INITIAL CONDITIONS                RKGS 50
6:      C                                                         RKGS 60
7:      C                                                         RKGS 70
8:      C      PRMT      - AN INPUT OUTPUT VECTOR WITH DIMENSION GREATER OR RKGS 80
9:      C                  EQUAL TO 5                                RKGS 90
10:     C      PRMT(1)    - LOWER BOUND OF THE INTERVAL            RKGS 100
11:     C      PRMT(2)    - UPPER BOUND OF THE INTERVAL           RKGS 110
12:     C      PRMT(3)    - INITIAL INCREMENT OF THE INDEPENDENT VARIABLE RKGS 120
13:     C      PRMT(4)    - UPPER ERROR BOUND                     RKGS 130
14:     C      PRMT(5)    - NO INPUT PARAMETER. IT IS 0 UNLESS THE USER WANTS TO RKGS 140
15:     C                  TERMINATE RKGS AT ANY OUTPUT POINT     RKGS 150
16:     C      DERY       - INPUT VECTOR OF ERROR WEIGHTS. LATERON IS THE VECTOR RKGS 160
17:     C                  OF DERIVATIVES                          RKGS 170
18:     C      NDIM       - THE NUMBER OF EQUATIONS IN THE SYSTEM RKGS 180
19:     C      IHLF       - THE NUMBER OF BISECTIONS OF THE INITIAL INCREMENT RKGS 190
20:     C      AUX       - AN AUXILIARY STORAGE ARRAY (8 ROWS AND NDIM COLUMNS) RKGS 200
21:     C                                                         RKGS 210
22:     C                                                         RKGS 220
23:     C      DIMENSION Y(1),DERY(1),AUX(8,1),A(4),F(4),C(4),PRMT(1) RKGS 230
24:     C      DO 1 I=1,NDIM                                       RKGS 240
25:     C 1 AUX(8,I)=.06666667*DERY(I)                             RKGS 250
26:     C      X=PRMT(1)                                           RKGS 260
27:     C      XFND=PRMT(2)                                         RKGS 270
28:     C      H=PRMT(3)                                           RKGS 280
29:     C      PRMT(5)=0.                                           RKGS 290
30:     C      CALL FCT(X,Y,DERY)                                   RKGS 300
31:     C                                                         RKGS 310
32:     C      ERROR TEST                                         RKGS 320
33:     C                                                         RKGS 330
34:     C      IF(H*(XFND-X))38,37,2                                RKGS 340
35:     C                                                         RKGS 350

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36:	C	PREPARATIONS FOR RUNGE-KUTTA METHOD	RKGS	360
37:	C		RKGS	370
38:	2	A(1)=.5	RKGS	380
39:		A(2)=.2928932	RKGS	390
40:		A(3)=1.707107	RKGS	400
41:		A(4)=.1666667	RKGS	410
42:		B(1)=2.	RKGS	420
43:		B(2)=1.	RKGS	430
44:		B(3)=1.	RKGS	440
45:		B(4)=2.	RKGS	450
46:		C(1)=.5	RKGS	460
47:		C(2)=.2928932	RKGS	470
48:		C(3)=1.707107	RKGS	480
49:		C(4)=.5	RKGS	490
50:	C		RKGS	500
51:	C	PREPARATIONS OF FIRST RUNGE-KUTTA STEP	RKGS	510
52:	C		RKGS	520
53:		DO 3 I=1,NDIM	RKGS	530
54:		AUX(1,I)=Y(I)	RKGS	540
55:		AUX(2,I)=DERY(I)	RKGS	550
56:		AUX(3,I)=0.	RKGS	560
57:	3	AUX(6,I)=0.	RKGS	570
58:		IFEC=0	RKGS	580
59:		H=H+H	RKGS	590
60:		IHLF=-1	RKGS	600
61:		ISTEP=0	RKGS	610
62:		IEND=0	RKGS	620
63:	C		RKGS	630
64:	C	START OF A RUNGE-KUTTA STEP	RKGS	640
65:	C		RKGS	650
66:	4	IF((X+H-XEND)*H) 7,6,5	RKGS	660
67:	5	H=XEND-X	RKGS	670
68:	6	IEND=1	RKGS	680
69:	C		RKGS	690
70:	C	RECORDING OF INITIAL VALUES OF THIS STEP	RKGS	700
71:	C		RKGS	710

72:	7 CALL OUTP(X,Y,DERY,IRFC,NDIM,PRMT)	RKGS 720
73:	IF(PRMT(5))40,8,40	RKGS 730
74:	8 ITEST=0	RKGS 740
75:	9 ISTEP=ISTEP+1	RKGS 750
76:	C	RKGS 760
77:	C START OF INNERMOST RUNGE-KUTTA LOOP	RKGS 770
78:	C	RKGS 780
79:	J=1	RKGS 790
80:	10 AJ=A(J)	RKGS 800
81:	BJ=B(J)	RKGS 810
82:	CJ=C(J)	RKGS 820
83:	DO 11 I=1,NDIM	RKGS 830
84:	R1=H*DERY(I)	RKGS 840
85:	R2=AJ*(R1-PJ*AUX(J,I))	RKGS 850
86:	Y(I)=Y(I)+R2	RKGS 860
87:	R2=R2+R2+R2	RKGS 870
88:	11 AUX(6,I)=AUX(6,I)+R2-CJ*R1	RKGS 880
89:	IF(J-4)12,15,15	RKGS 890
90:	12 J=J+1	RKGS 900
91:	IF(J-3)13,14,13	RKGS 910
92:	13 X=X+.5*H	RKGS 920
93:	14 CALL FCT(X,Y,DERY)	RKGS 930
94:	GO TO 10	RKGS 940
95:	C	RKGS 950
96:	C TEST OF ACCURACY	RKGS 960
97:	C	RKGS 970
98:	15 IF(ITEST)16,16,20	RKGS 980
99:	C	RKGS 990
100:	C IN CASE ITEST=0 THERE IS NO POSSIBILITY FOR TESTING OF ACCURACY	RKGS1000
101:	C	RKGS1010
102:	16 DO 17 I=1,NDIM	RKGS1020
103:	17 AUX(4,I)=Y(I)	RKGS1030
104:	ITEST=1	RKGS1040
105:	ISTEP=ISTEP+ISTEP-2	RKGS1050
106:	18 IHLF=IHLF+1	RKGS1060
107:	X=X-H	RKGS1070

108:	H=.5*H	RKGS1080
109:	DO 19 I=1,NDIM	RKGS1090
110:	Y(I)=AUX(1,I)	RKGS1100
111:	DERY(I)=AUX(2,I)	RKGS1110
112:	19 AUX(5,I)=AUX(3,I)	RKGS1120
113:	GOTO 9	RKGS1130
114:	C	RKGS1140
115:	C IN CASE ITEST=1 TESTING OF ACCURACY IS POSSIBLE	RKGS1150
116:	C	RKGS1160
117:	20 IMOD=ISTEP/2	RKGS1170
118:	IF(ISTEP-IMOD-IMOD)21,23,21	RKGS1180
119:	21 CALL FCT(X,Y,DERY)	RKGS1190
120:	DO 22 I=1,NDIM	RKGS1200
121:	AUX(5,I)=Y(I)	RKGS1210
122:	22 AUX(7,I)=DERY(I)	RKGS1220
123:	GOTO 9	RKGS1230
124:	C	RKGS1240
125:	C COMPUTATION OF TEST VALUE DELT	RKGS1250
126:	C	RKGS1260
127:	23 DELT=0.	RKGS1270
128:	DO 24 I=1,NDIM	RKGS1280
129:	24 DELT=DELT+AUX(8,I)*ABS(AUX(4,I)-Y(I))	RKGS1290
130:	IF(DELT-PRMT(4))28,28,25	RKGS1300
131:	C	RKGS1310
132:	C ERROR IS TOO GREAT	RKGS1320
133:	C	RKGS1330
134:	25 IF(IHLF-10)26,36,36	RKGS1340
135:	26 DO 27 I=1,NDIM	RKGS1350
136:	27 AUX(4,I)=AUX(5,I)	RKGS1360
137:	ISTEP=ISTEP+ISTEP-4	RKGS1370
138:	X=X-H	RKGS1380
139:	IEND=0	RKGS1390
140:	GOTO 18	RKGS1400
141:	C	RKGS1410
142:	C RESULT VALUES ARE GOOD	RKGS1420
143:	C	RKGS1430

144:	28 CALL FCT(X,Y,DERY)	RKGS1440
145:	GO 29 I=1,NDIM	RKGS1450
146:	AUX(1,I)=Y(I)	RKGS1460
147:	AUX(2,I)=DERY(I)	RKGS1470
148:	AUX(3,I)=AUX(6,I)	RKGS1480
149:	Y(I)=AUX(5,I)	RKGS1490
150:	29 DERY(I)=AUX(7,I)	RKGS1500
151:	CALL OUTP(X-H,Y,DERY,IHLF,NDIM,PRMT)	RKGS1510
152:	IF(PRMT(5))40,30,40	RKGS1520
153:	30 GO 31 I=1,NDIM	RKGS1530
154:	Y(I)=AUX(1,I)	RKGS1540
155:	31 DERY(I)=AUX(2,I)	RKGS1550
156:	IPFC=IHLF	RKGS1560
157:	IF(IEND)32,32,39	RKGS1570
158:	C	RKGS1580
159:	C INCREMENT GETS DOUBLED	RKGS1590
160:	C	RKGS1600
161:	32 IHLF=IHLF-1	RKGS1610
162:	ISTEP=ISTEP/2	RKGS1620
163:	H=H+H	RKGS1630
164:	IF(IHLF)4,33,33	RKGS1640
165:	33 IMOD=ISTEP/2	RKGS1650
166:	IF(ISTEP-IMOD-IMOD)4,34,4	RKGS1660
167:	34 IF(DELT-.02*PRMT(4))35,35,4	RKGS1670
168:	35 IHLF=IHLF-1	RKGS1680
169:	ISTEP=ISTEP/2	RKGS1690
170:	H=H+H	RKGS1700
171:	GOTO 4	RKGS1710
172:	C	RKGS1720
173:	C RETURNS TO CALLING PROGRAM	RKGS1730
174:	C	RKGS1740
175:	36 IHLF=11	RKGS1750
176:	CALL FCT(X,Y,DERY)	RKGS1760
177:	GOTO 39	RKGS1770
178:	37 IHLF=12	RKGS1780
179:	GOTO 39	RKGS1790

```
180:      38 IHLF=13
181:      39 CALL OUTP(X,Y,DEFY,IHLF,NDIM,PRMT)
182:      40 RETURN
183:      END
```

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RKCS1800
RKCS1810
RKCS1820
RKCS1830
```

APPENDIX B

INPUT DATA REQUIRED

As examples, the input information for the hypothetical cases 8 and 10 are given next.

INPUT DATA (Case #8)

TINIT = 0.0 ENCS = 90.0 MIN PRMT(3) = 2.5C MIN PRMT(4) = 1.CCCCC
 NUMBER OF SOURCES = 1
 PROEL = 5.00 MIN
 NX = 6 NY = 7 NZ = 7
 YMAX = 700.0 M H = 505.00 M
 KS = 5 LS = 4 CO = 35.45 MG/CU.M XMAX = 10000.0 M
 STABILITY CLASS = 4 INVR5 = 1 ALPHA = 2.00 AK = C.58E-C4 1/MIN
 UST = 300.00 M/MIN LGR = 30.00 M/MIN AM = 0.250 TCH = 15.0 MIN P = 0.05

INPUT DATA (Case #10)

TINIT = 0.0 ENCS = 90.0 MIN PRMT(3) = 2.50 MIN PRMT(4) = 1.CCCCC
 NUMBER OF SOURCES = 2
 PROEL = 5.00 MIN
 NX = 6 NY = 7 NZ = 7
 YMAX = 700.0 M H = 505.00 M
 KS = 5 LS = 4 CO = 35.45 MG/CU.M XMAX = 10000.0 M
 KS = 4 LS = 5 CO = 21.27 MG/CU.M XMAX = 8000.0 M
 STABILITY CLASS = 4 INVR5 = 1 ALPHA = 2.00 AK = C.58E-C4 1/MIN
 UST = 300.00 M/MIN LGR = 30.00 M/MIN AM = 0.250 TCH = 15.0 MIN P = 0.0

APPENDIX C

NOMENCLATURE

a	Constant in equation (4.8)
a_i	Parameters defined by equation (4.2)
a_{ij}	Parameters defined by equation (4.41)
$\bar{A}$	Matrix defined by equation (4.19)
AM	Represents the exponent m
b	Constant in equation (4.29)
$\bar{B}$	Matrix defined by equation (4.20)
c	Constant in equation (4.29)
c_j	Coefficients in equation (4.3)
C_i	Instantaneous concentration of species i , mg/m^3
C_B	Background concentration
$C_O(i)$	Concentration at i^{th} source
d_i	Coefficients defined by equation (4.11)
d_{ij}	Coefficients defined by equation (4.42)
D_i	Molecular diffusivity of species i , m^2/min
D'	Eddy diffusivity tensor used in equation (3.1)
e_i	Constants defined by equation (4.43)
f_j	Constants defined by equation (4.50)
G_i	Constant given by equation (4.9)

G_i^*	Constant in equation (4.33)
H	Maximum height above terrain (in some cases refers to the elevation of the inversion base)
INVR	Constant used in equation (4.105)
ISTB	Stability class (1 very unstable, 6 very stable)
(JS,KS,LS)	(x,y,z) coordinate position of a point source
k	Reaction rate constant, min^{-1}
k_o	Von Karman's constant
K	Turbulent diffusivity, m^2/min
ℓ	Height defined by equation (3.11)
L	Effective emission height, m
m	Exponent in equation (4.65)
N	Number of interior collocation points
N_j	j^{th} independent Gaussian white noise
NSRCS	Number of sources
p	Exponent in equation (3.10)
P	Constant in equation (4.67)
P_o	First orthogonal polynomial
P_i	i^{th} orthogonal polynomial
P_j	Power spectral density of the j^{th} white noise
PRMT(3)	Initial step size of integration
PRMT(4)	Upper error bound in "RKGS"
Q	Source emission rate, $\text{mg}/\text{m}^3 \text{min}$
Q(i)	Strength of i^{th} continuous point source, kg/s
$\bar{Q}$	Matrix used in orthogonal collocation theory
Q_x	Mass rate through y-z plane at x = constant, kg/s

$Q(x,t/x^*,t^*)$	Transition probability density function
$\bar{R}$	Matrix used in orthogonal collocation theory
R_i	Rate of generation of species i
s	Number of species
$S(x,t)$	Spatial-temporal distribution of particle sources
t	Time, min
$\bar{T}$	Matrix used in orthogonal collocation theory
TCH	Parameter in equation (4.67)
u	Velocity in x-direction, m/min
u	Variable in equation (4.31)
u_j	j^{th} component of fluid velocity, m/min
u^*	Friction velocity
UGR	Mean wind velocity in the x-direction at ground level
UST	Geostrophic wind speed, m/min
v	Velocity in y-direction, m/min
v^*	Pseudo-velocity defined by equation (3.1)
w	Velocity in z-direction, m/min
$w(x)$	Weighting function
W_j	Quadrature weights
x	Cartesian coordinate in mean wind direction
x	Refers to independent variable in orthogonal collocation theory
x_j	Collocation points
x_{max}	Maximum distance in the x-direction

y	Cartesian coordinate in horizontal direction
y	Refers to dependent variable in orthogonal collocation theory
$y_{\max}$	Maximum distance in the y -direction
z	Cartesian coordinate in vertical direction
z_0	Characteristic surface roughness length
z_1	Reference height

Greek Symbols

α	Constant in equation (4.63)
α	Exponent in equation (4.5)
∇	Gradient vector
∇^2	Laplacian
β	Exponent in equation (4.5)
Γ	Gamma function
δ	Test value used in "RKGS"
δ_{ij}	Kronecker delta function
Δ	Knee height, m
ζ	Function that represents K_z
η	Function that represents v
θ	Time between the pollutant release and the initiation of the averaging time, min
ξ	Function that represents K_y
σ	Standard deviation
$\phi(x,y)$	Function of the independent variables x and y , given by equation (4.41)

ψ	Function that represents u
Ω	End of the averaging time, min

Superscripts

'	Denotes the fluctuating component when used in a concentration or velocity variable
—	Denotes the mean value when used on a velocity variable
*	Refers to shifted polynomials
=	Refers to a matrix

Subscripts

i	i^{th} species
i	Index in collocation equations
i	Index used in orthogonal collocation theory
j	j^{th} direction in Cartesian coordinates
j	Index used in orthogonal collocation theory
j	Represents the x-direction in collocation equations
k	Represents the y-direction in collocation equations
l	Represents the z-direction in collocation equations
n	Index used in orthogonal collocation theory
s	Denotes ground level
x	Refers to x coordinate direction
y	Refers to y coordinate direction
z	Refers to z coordinate direction
~	Denotes a vector quantity

Brackets

< > Denotes ensemble averages